

# Experimental and Simulations Related to Microcellular Injection Molding

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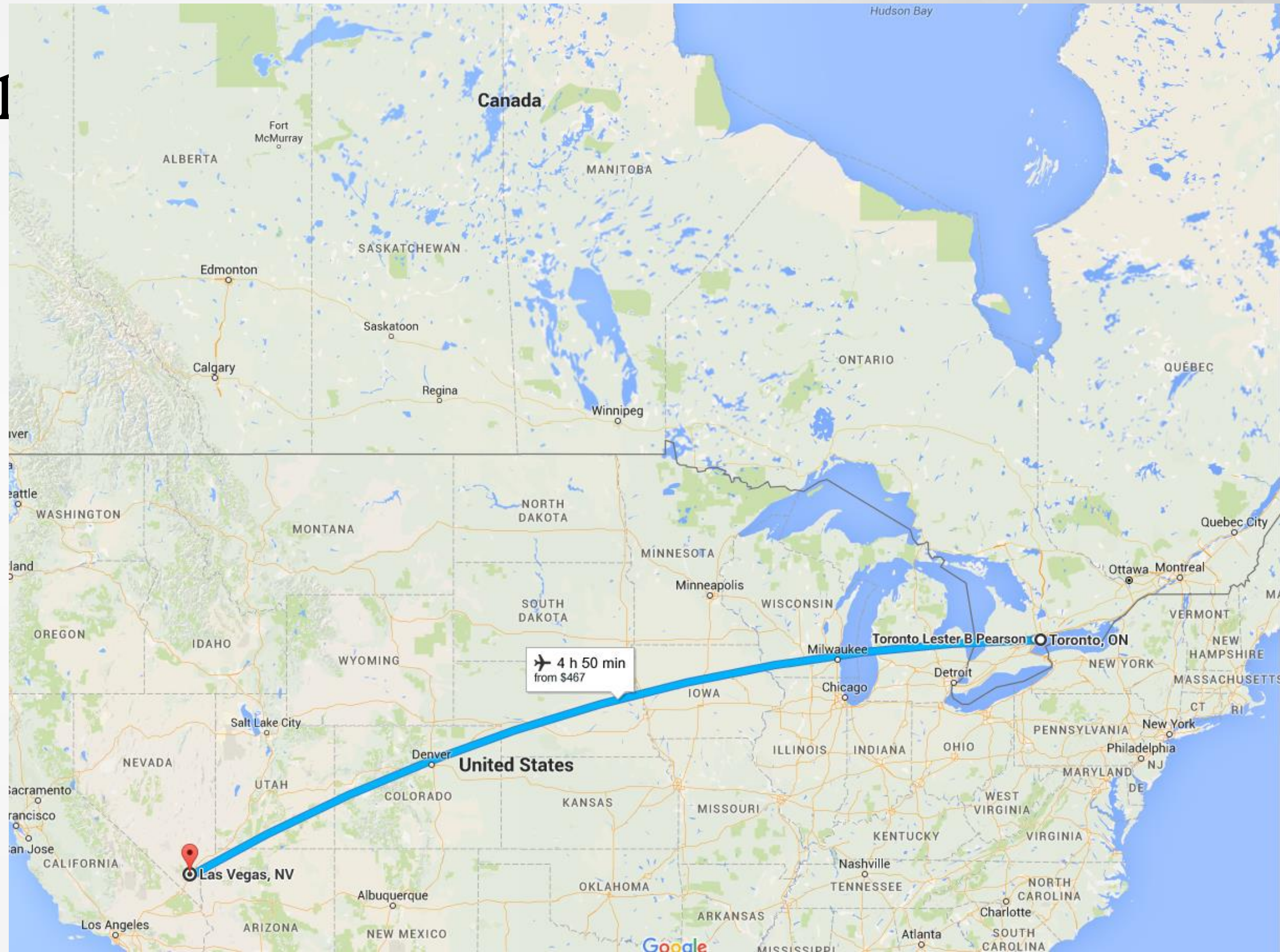
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Microcel

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## Background:

BASc: Industrial Metallurgy & Manufacturing Engineering

MASc: Materials Science and Engineering

MASc: Physical and Rheological Properties of Polymers;  
Rheology of Blends

PhD: – Investigation of the Mechanism(s) of Cell Nucleation  
and Growth in Foam Injection Molding;  
– Microcellular Foam Injection Molding;  
– Functional Polymers.



# Experimental and Simulations Related to Microcellular Injection Molding

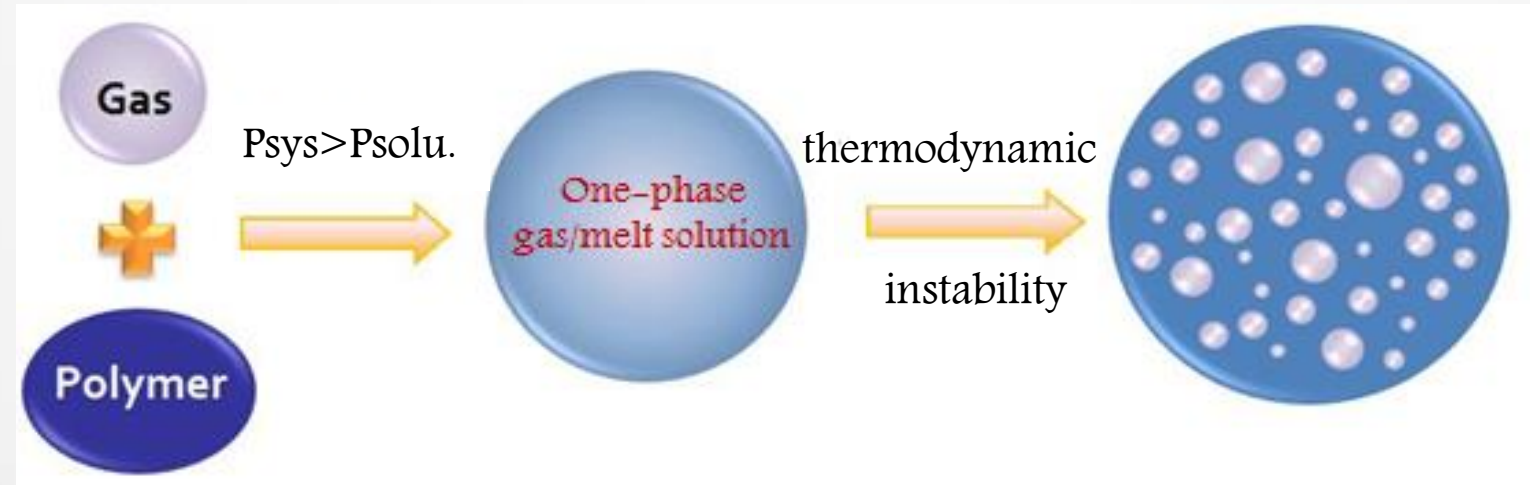
## Agenda:

- Visualization Equipment and Mold Design
- Mechanisms of Cell Nucleation and Growth in Low- and High-pressure Foam Injection Molding (FIM)
- Foam Injection Molding using Gas-Counter Pressure (FIM+GCP)
- Foam Injection Molding with High Expansion (FIM+MO)
- Application of Nucleating Agents (added or inherit)
- Simulation of Microcellular Injection Molding Process

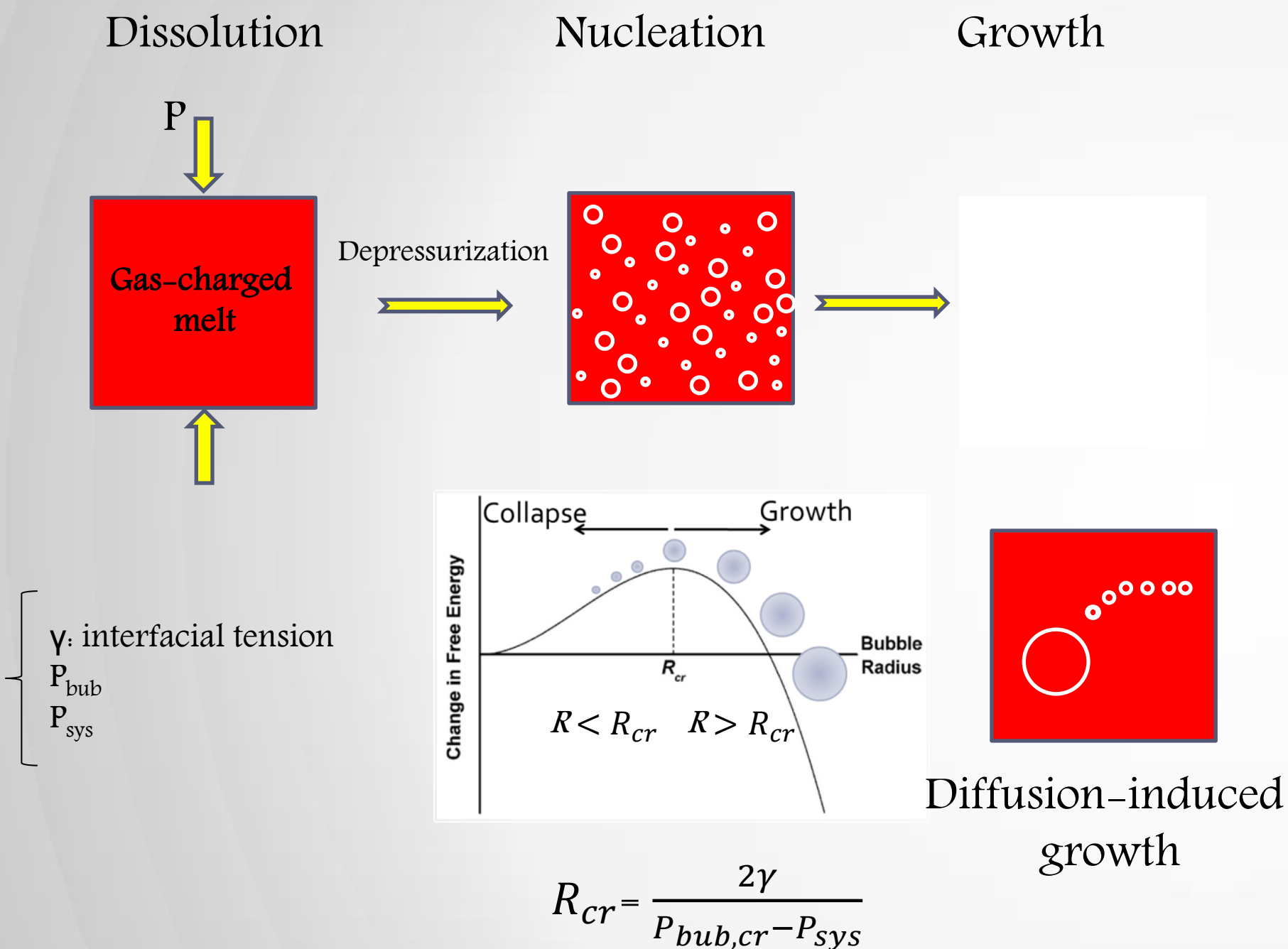
# Introduction

# Plastic Foams

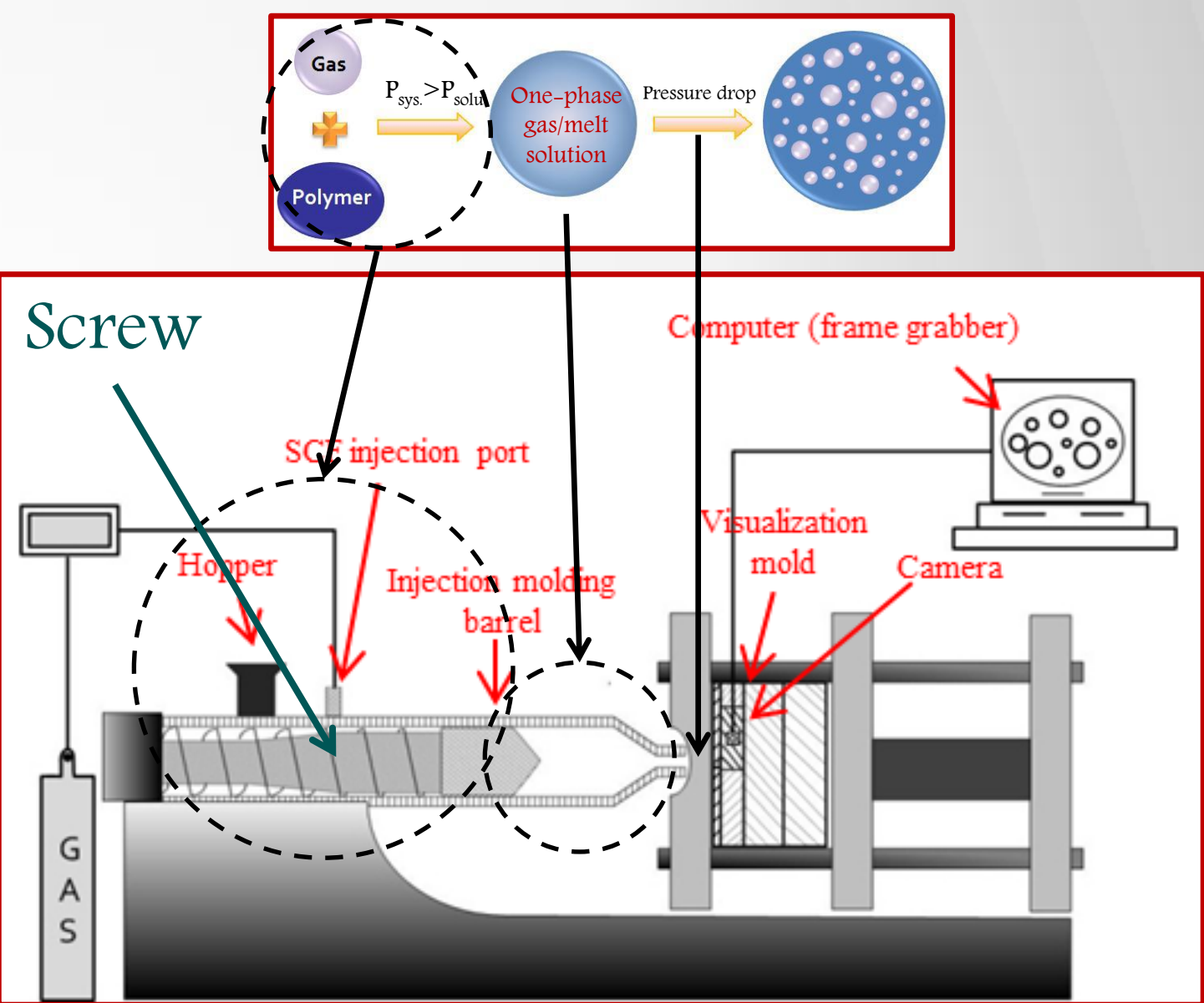
1. Dissolution of a blowing agent ( $\text{CO}_2$ ,  $\text{N}_2$ ) in the polymer melt to make a one-phase, homogeneous melt/gas mixture;
2. Cell nucleation *via* thermodynamic instability
3. Cell growth



# Nucleation and growth



# Foam Injection Molding (FIM)





# Foam Injection Molding (FIM)

## Broad spectrum of applications

- almost no residual stresses;
- high geometric accuracy;
- sound insulation properties;

material/energy  
saving.

➤ higher toughness, impact strength, and fatigue life (micro-cellular)

➤ improved heat insulation(nano-cellular)





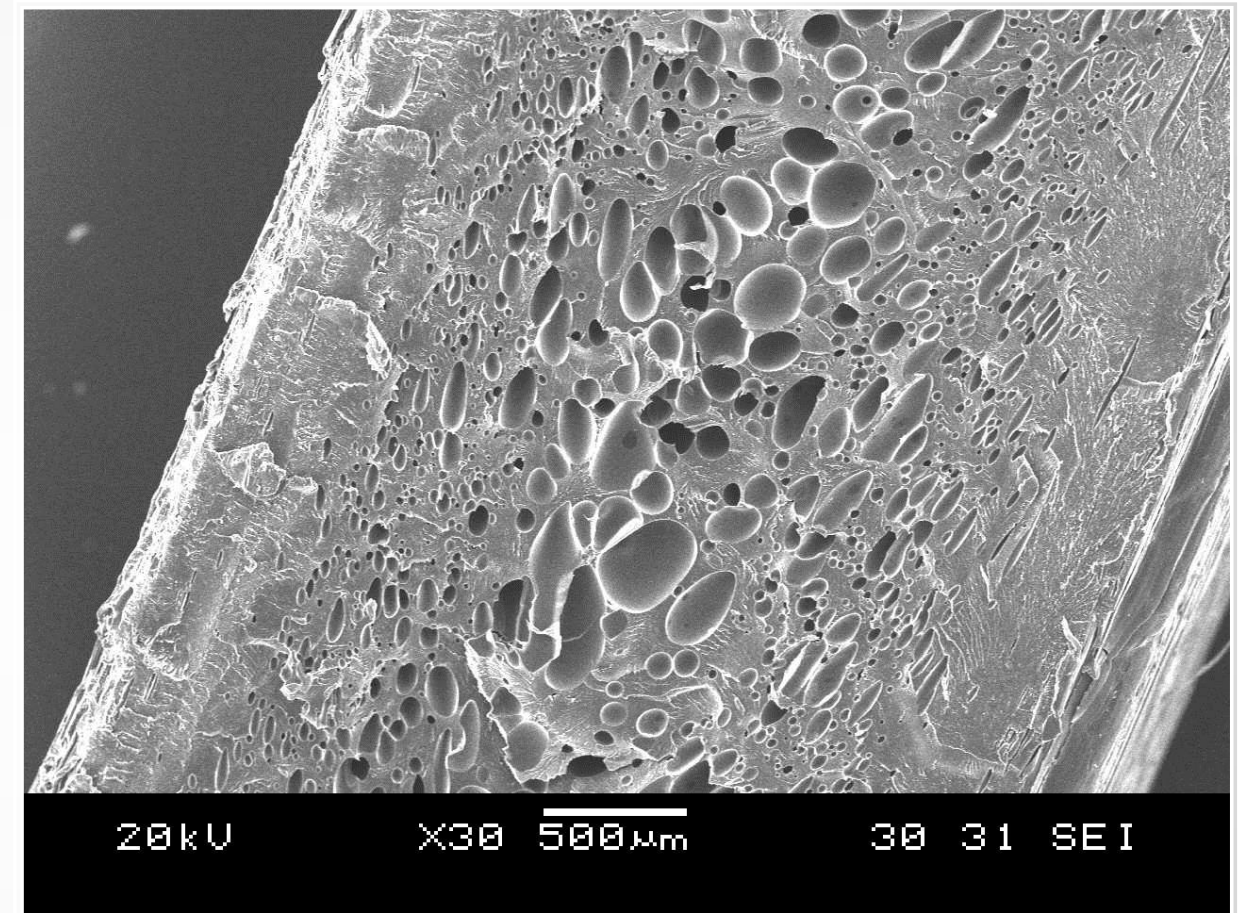
# Challenges

➤ Control the morphology to obtain desirable properties

- high cell density
- uniform distribution

**NOT easy in FIM !**

**Un-known  
Mechanisms !**



# What we are trying to achieve?

Identify the underlying mechanisms (nucleation/growth) in various FIM technologies in order to:

## 1. Experiment

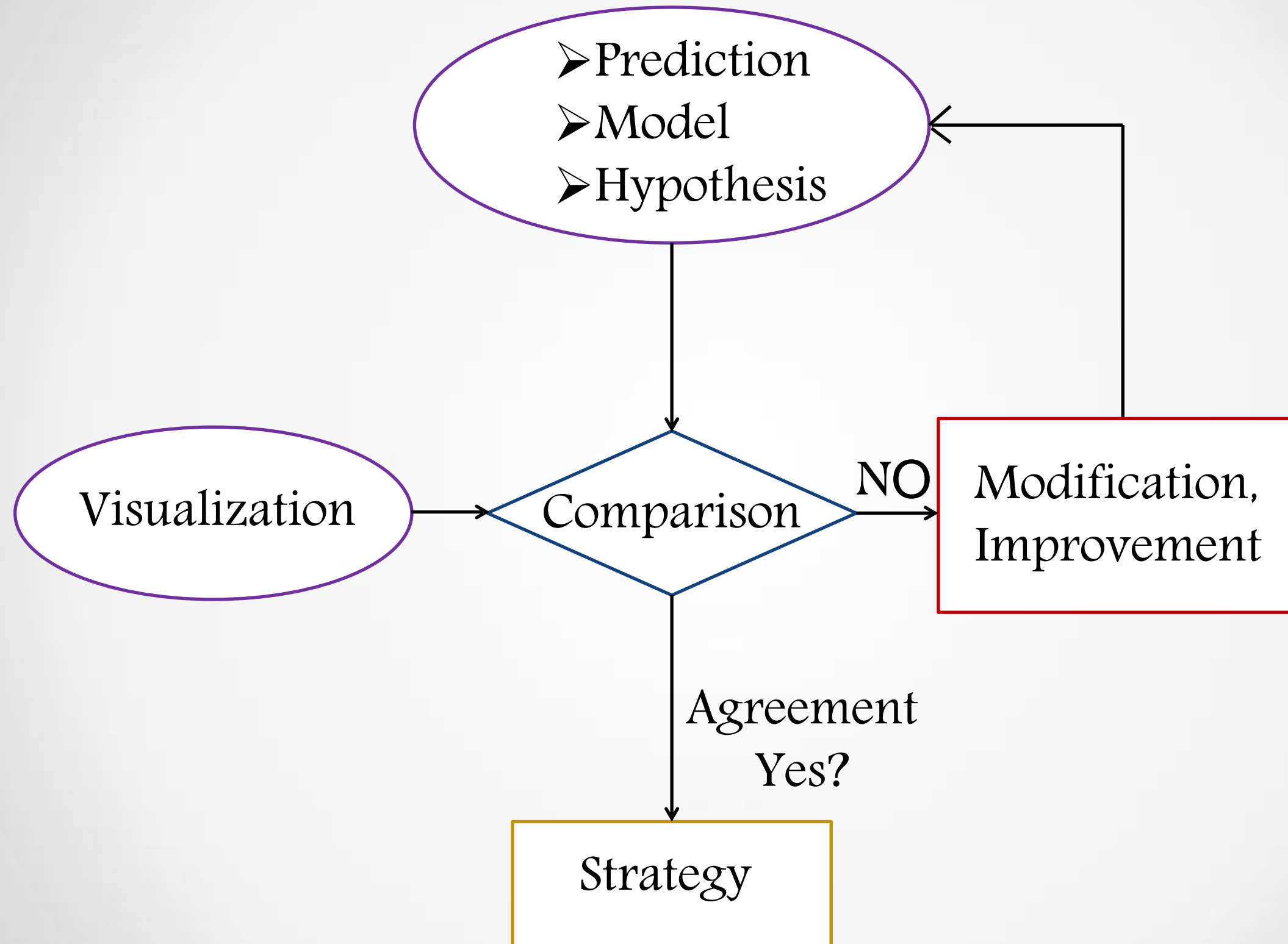
- ✓ Set proper processing parameters to perform CORRECT experiment
- ✓ To come up with DOE which yields the expected cellular structure (and so desired properties)

## 2. Simulation (Modeling)

- ✓ Contributing parameters/responsible mechanisms to be included/considered
- ✓ Actual (reliable) data to validate the model



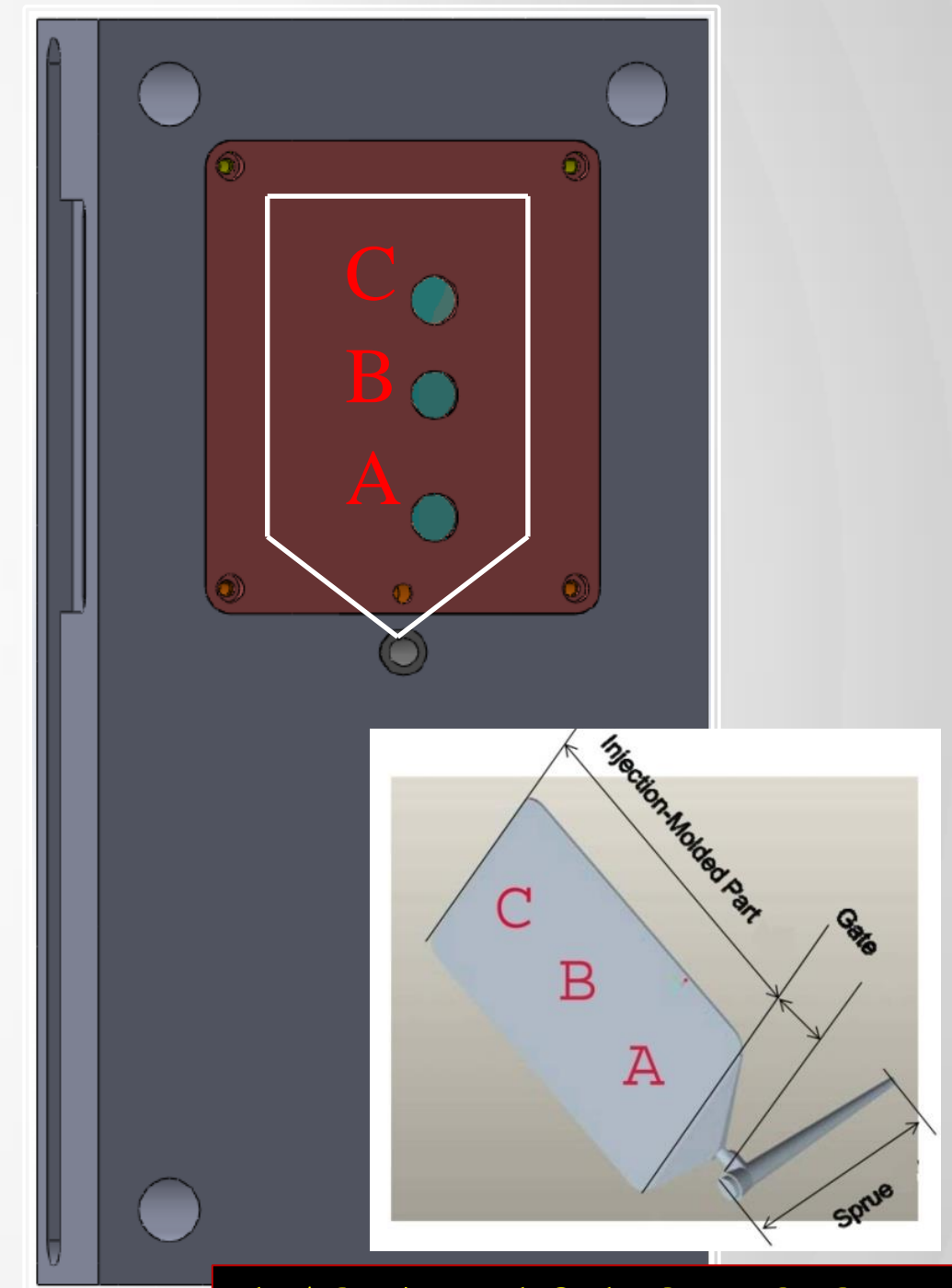
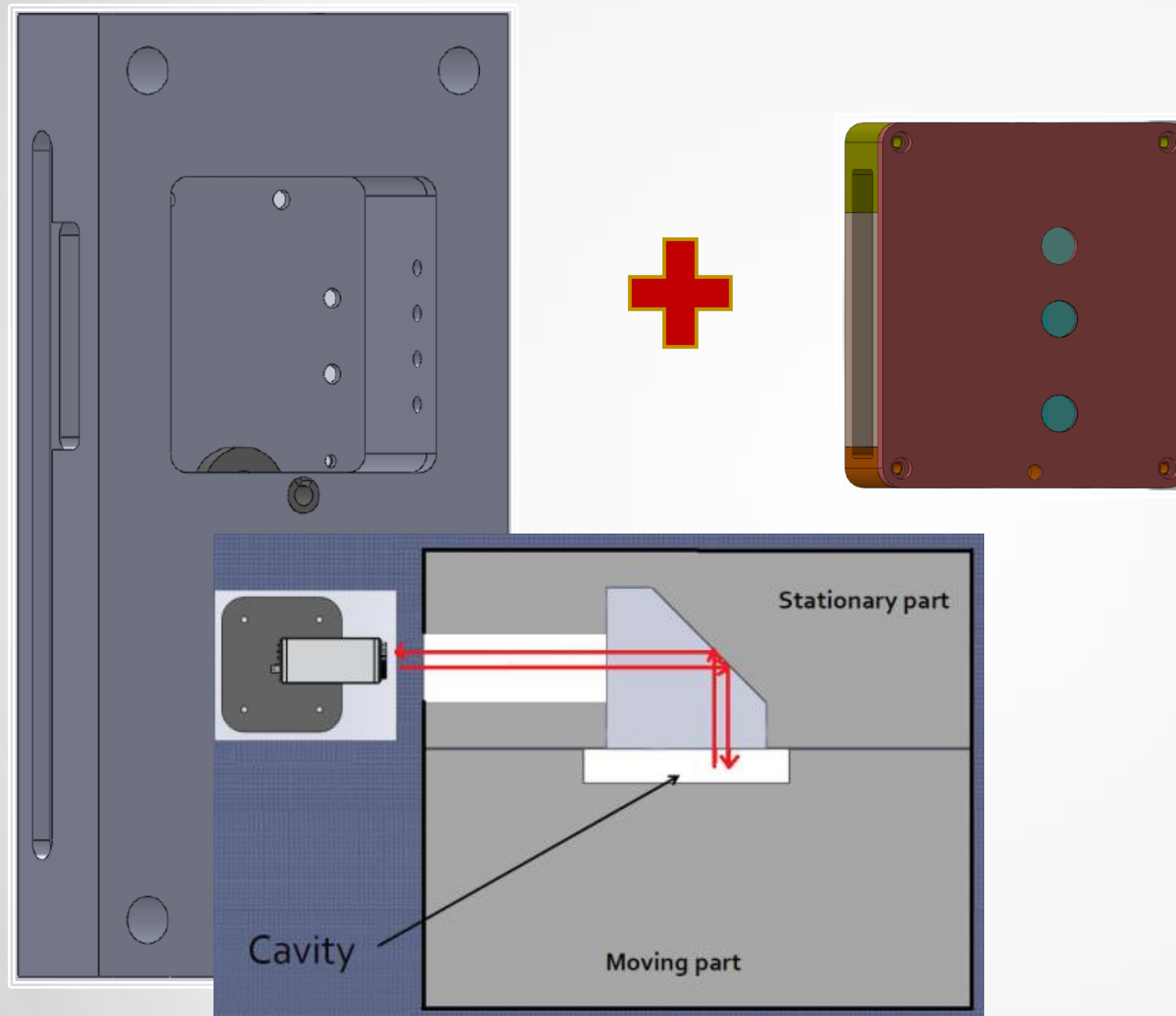
# Our Research Approach



# Visualization Mold Design and Experiment Equipment



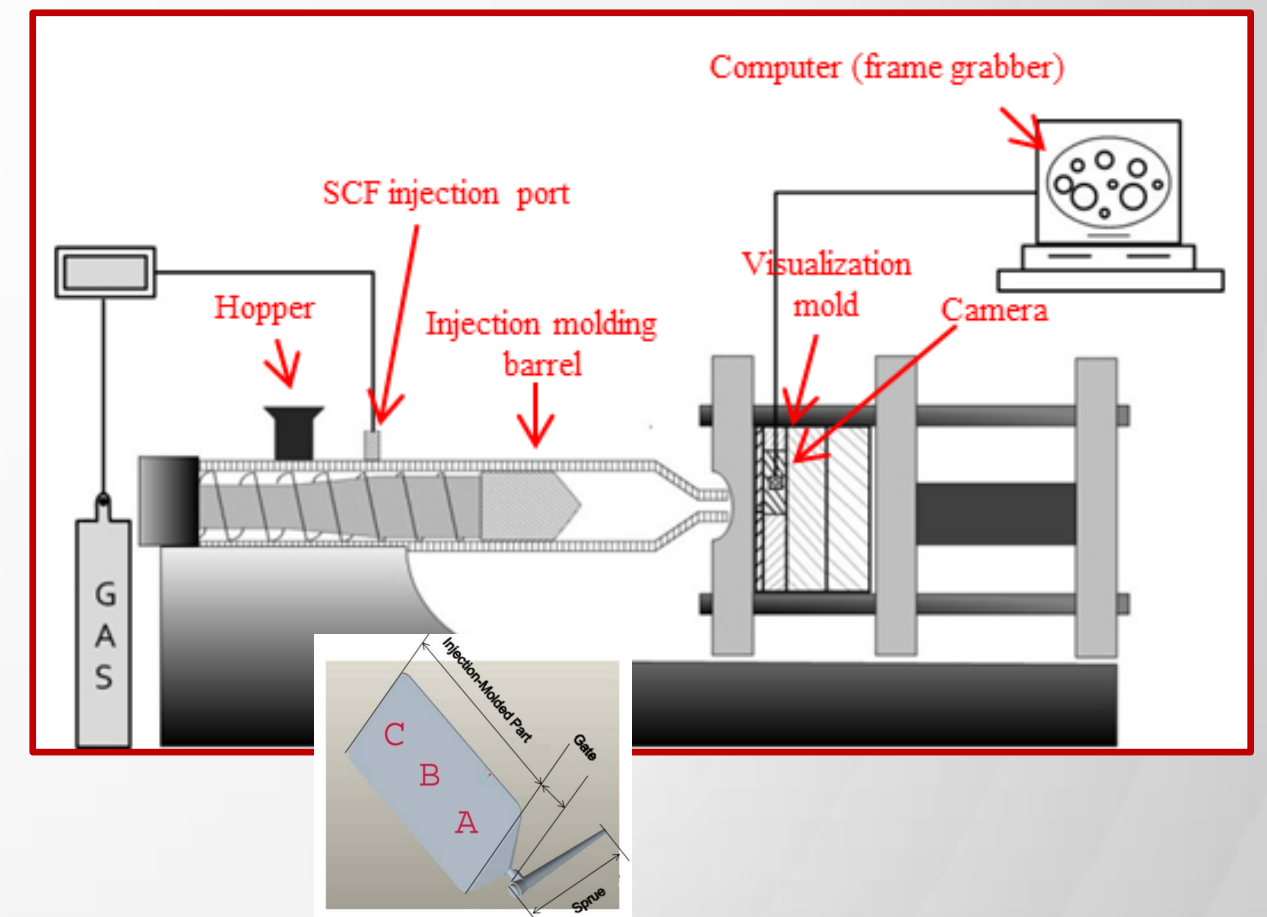
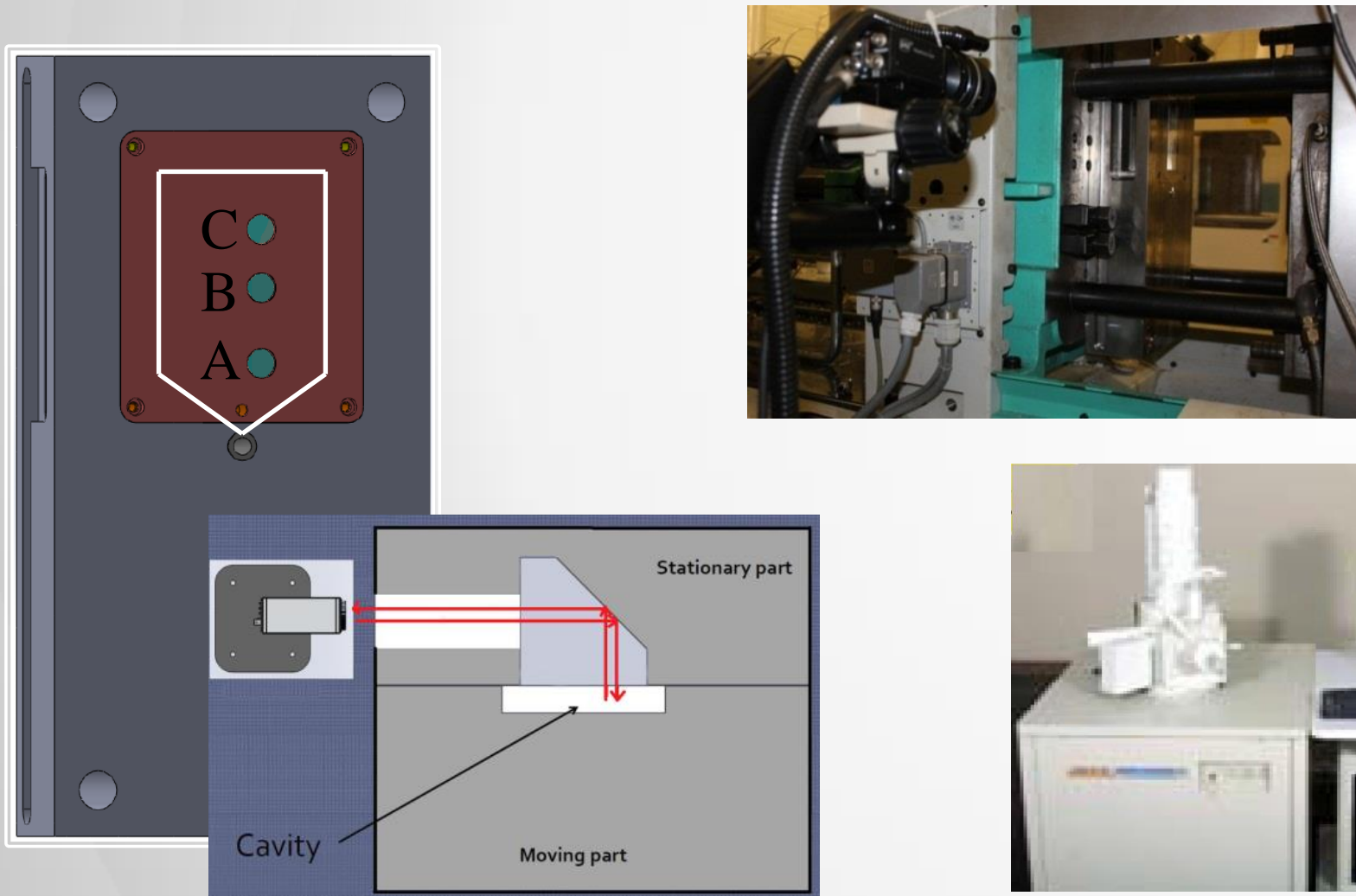
# Mold Design



$152.4 \times 101.6 \times 3.2 \text{ mm}$

# Equipment

- 50-ton Arburg ALLROUNDER (equipped with MuCell)
- Visualization Mold
- Camera: CV M10 camera from JAI equipped with a magnifying lens from Navitar

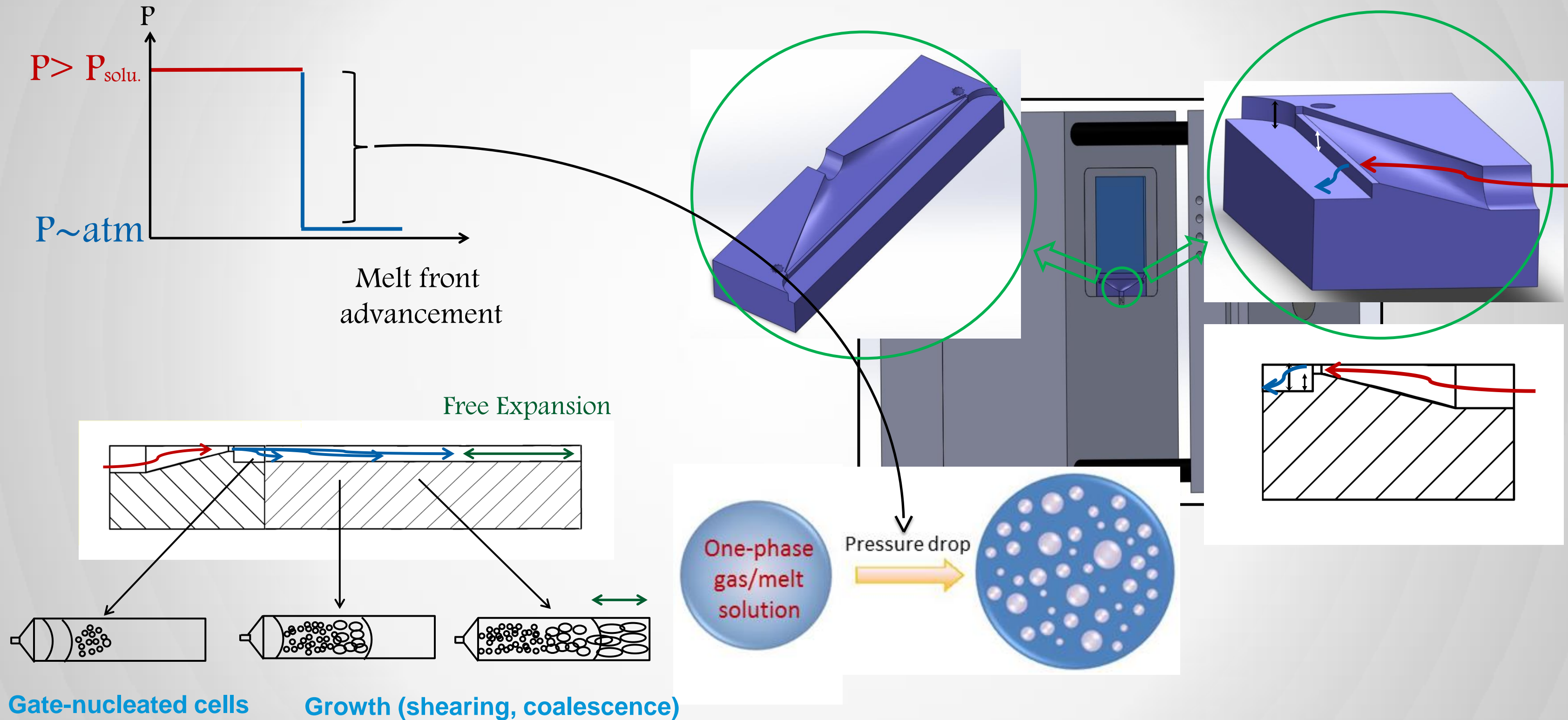


135 × 111 × 3.2 mm



# Low-pressure FIM

# Pressure Drop over the Gate (Low-Pressure FIM)

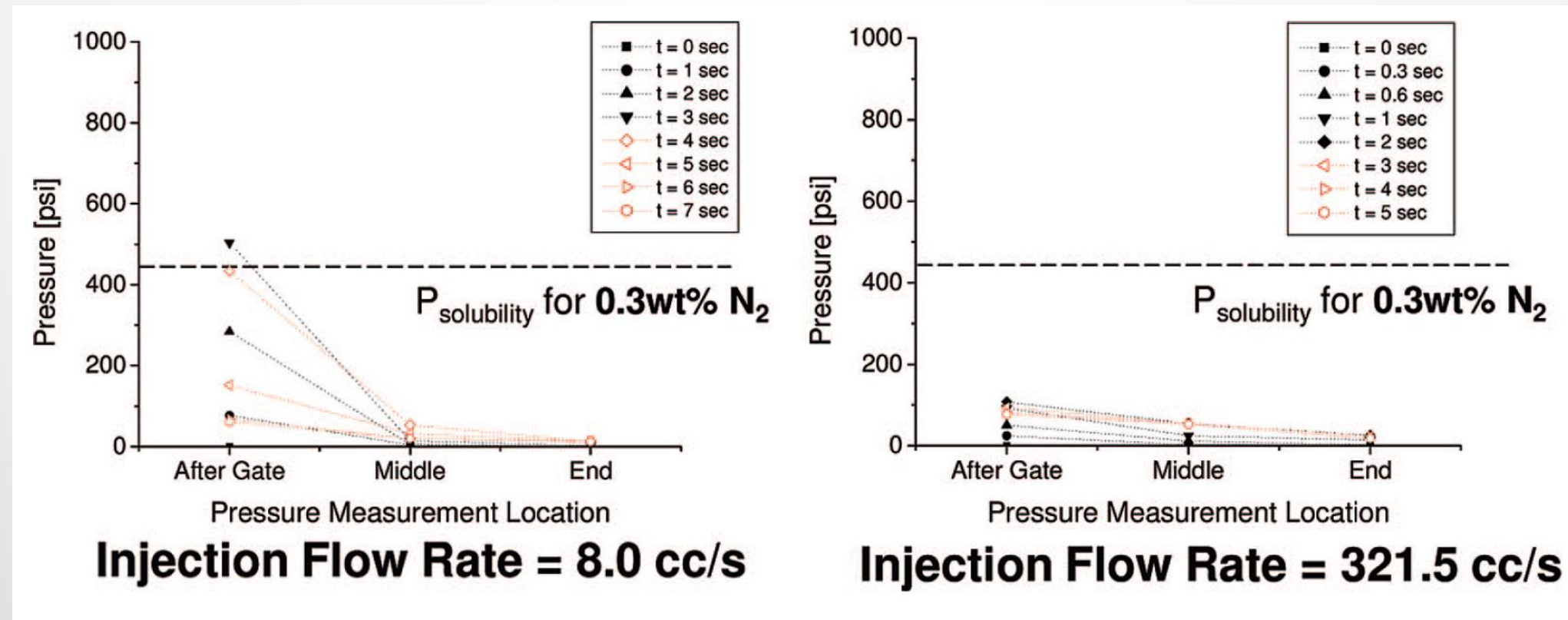
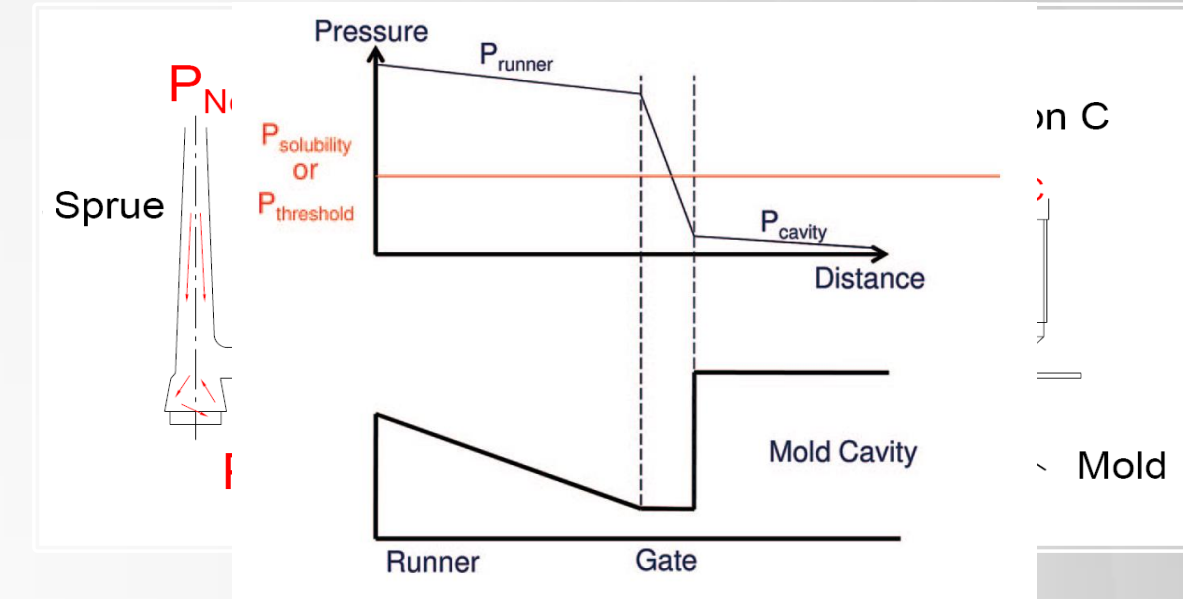




# Strategies to improve the microcellular structure

## 1. Injection Speed

- a– higher melt/gas mixture temperature → lower cavity pressure
- b– higher pressure drop rate
- c– faster travel of gate–nucleated cells → less growth/coalescence



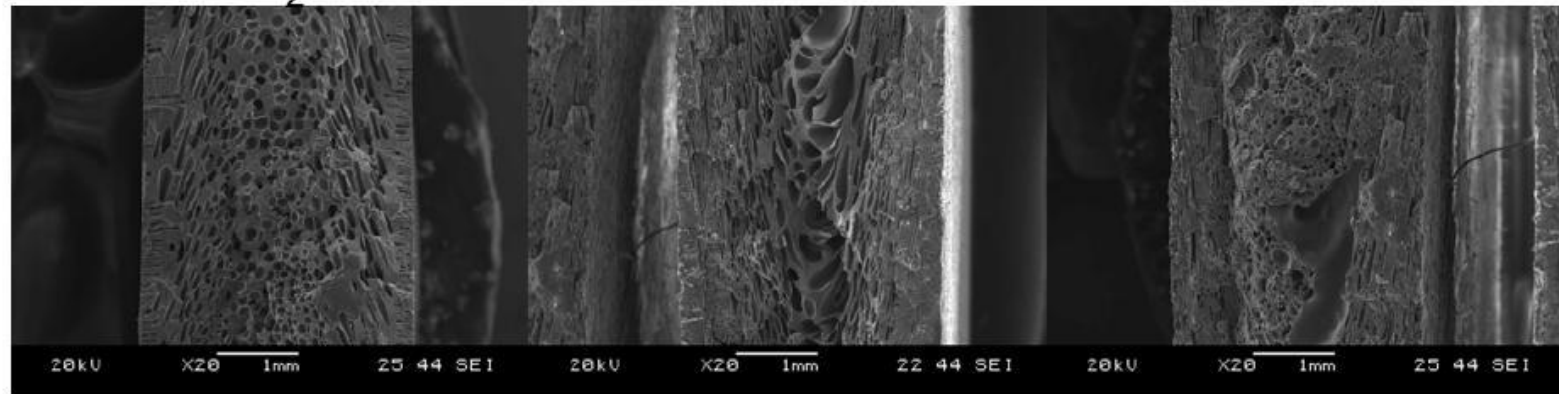
Lee, J. W., Wang, J., Yoon, J. D., & Park, C. B. (2008). Industrial & Engineering Chemistry Research, 47(23), 9457-9464

# Strategies to improve the microcellular structure

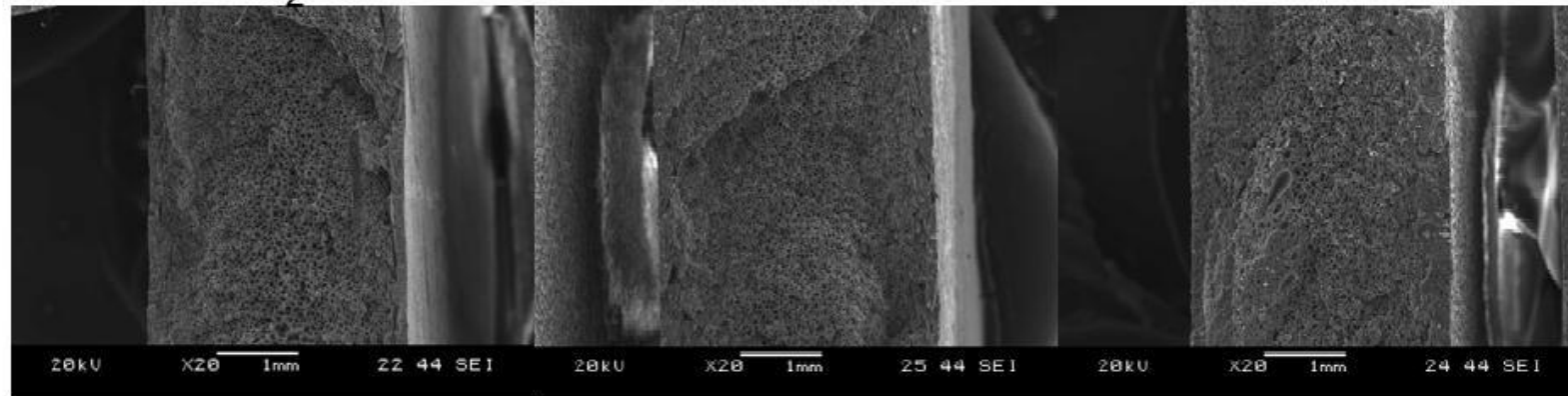
2. Shot size

3. % of dissolved gas

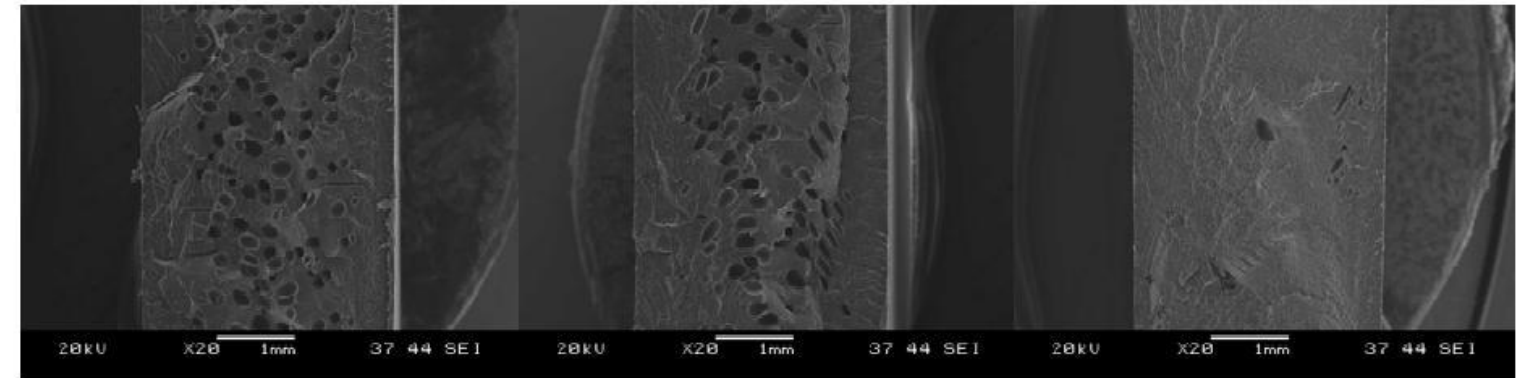
0.3 wt% N<sub>2</sub>



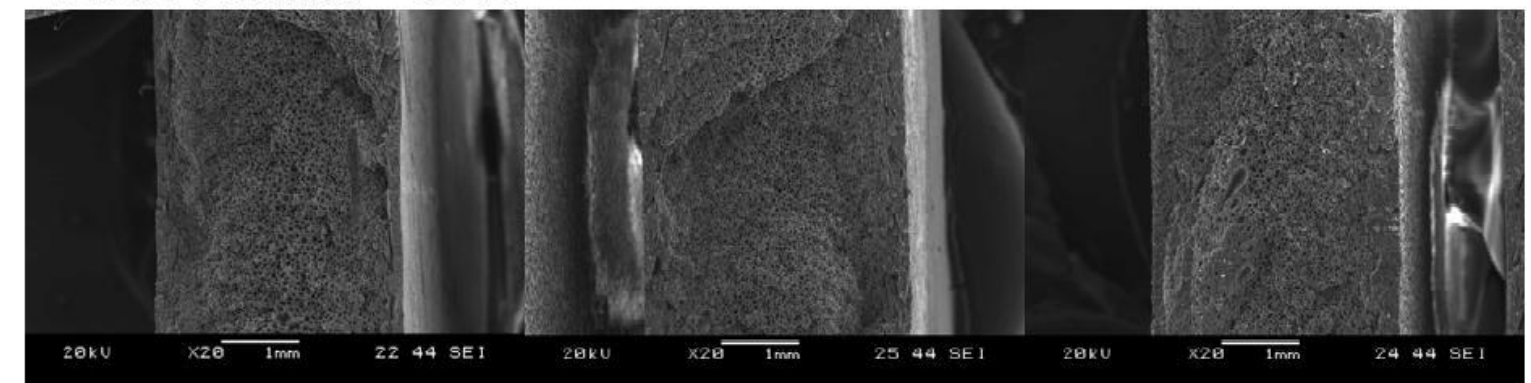
0.5 wt% N<sub>2</sub>



Void Fraction = 10%



Void Fraction = 30%



Location A

Location B

Location C

0.5 wt% N<sub>2</sub>, injection speed=400 mm/s, @200 °C

<sup>1</sup> Lee J. W. S., PhD Thesis, Chapter 5, Department of Mechanical and Industrial Engineering University of Toronto (2009)

# High-pressure Foam Injection Molding

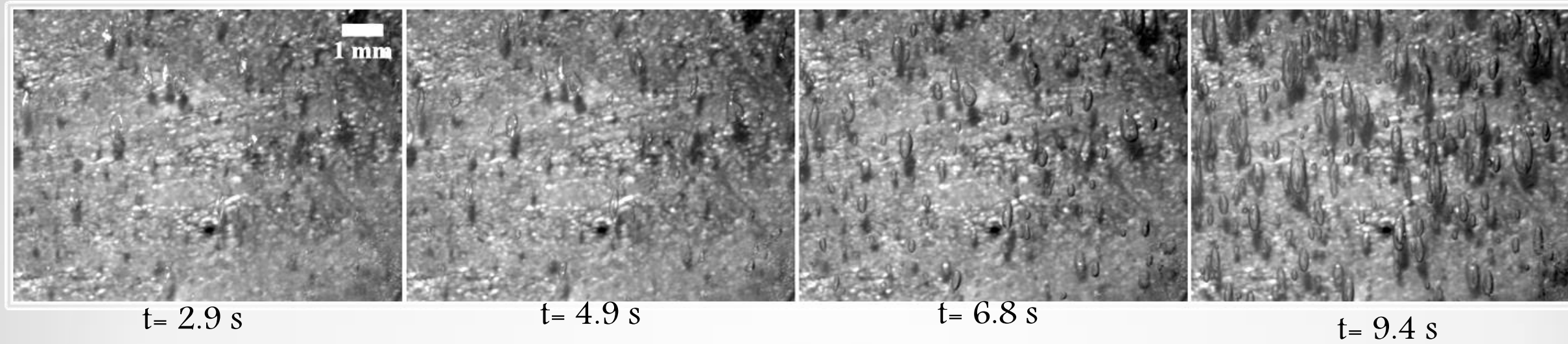
Materials:

- PS675 from AmericasStyrenics (MFI: 7.5 gr/10min);
- CO<sub>2</sub>: Linde Gas Canada;

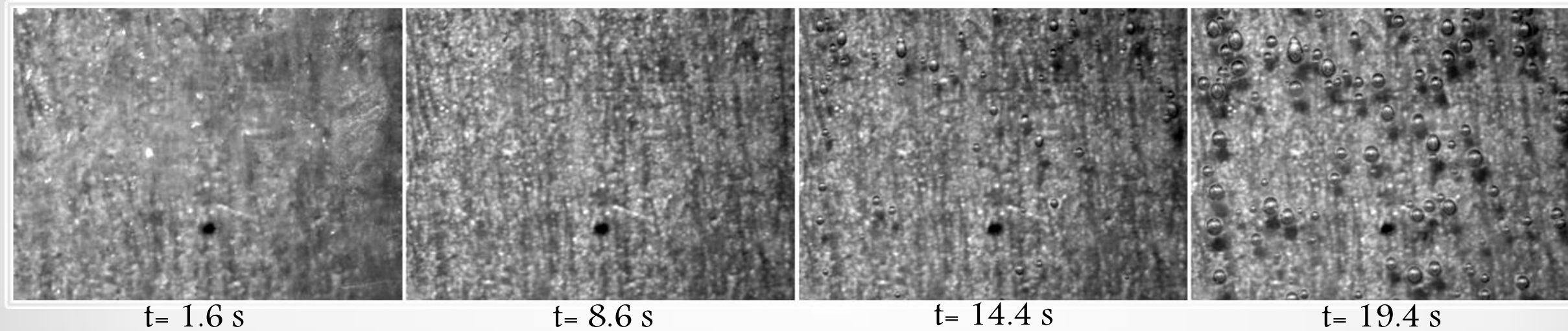


# Low- and High-pressure FIM

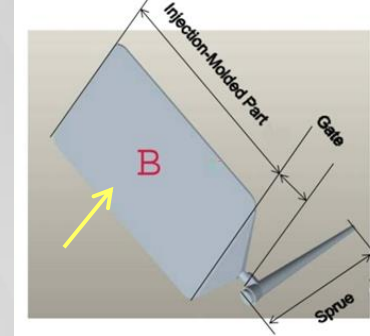
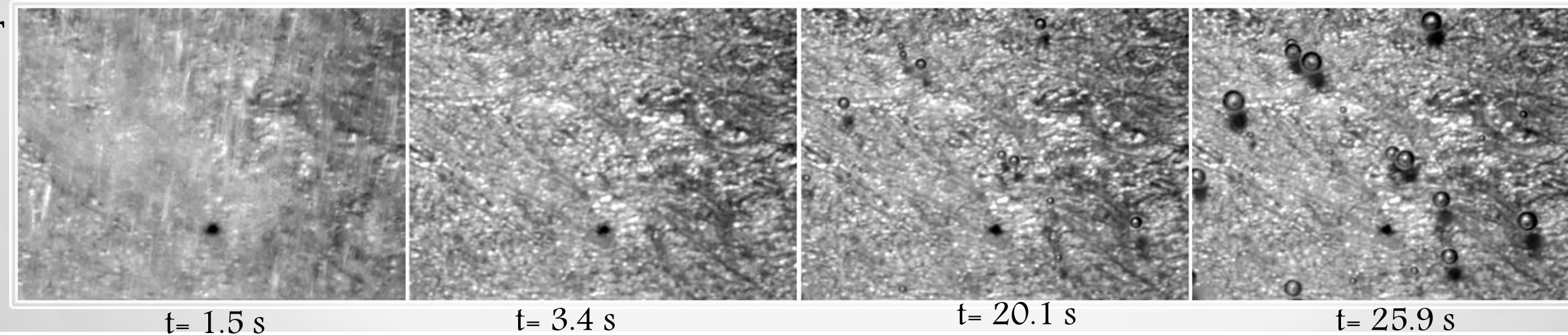
Pack P= 25 bar



Pack P= 80 bar



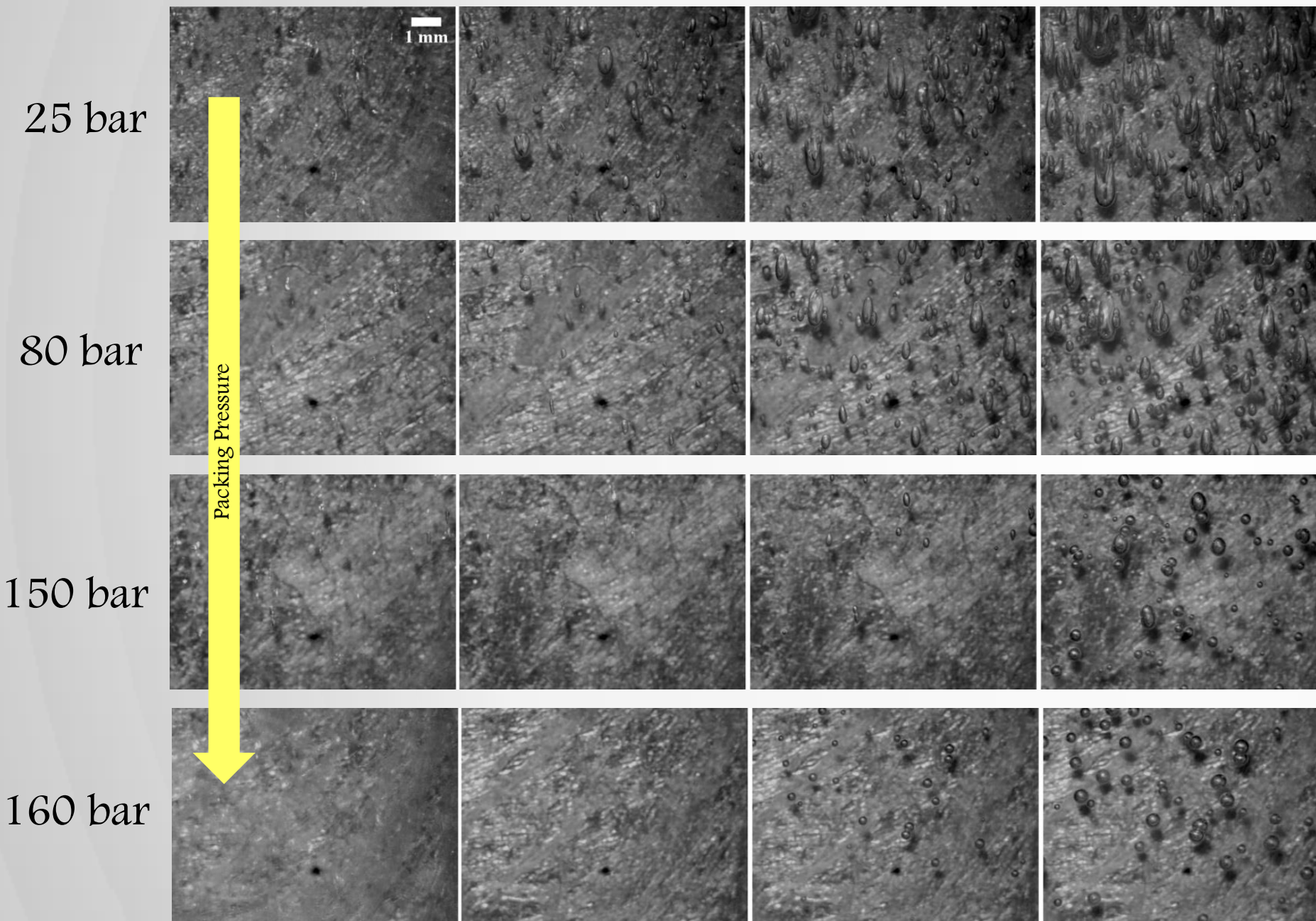
Pack P= 150 bar



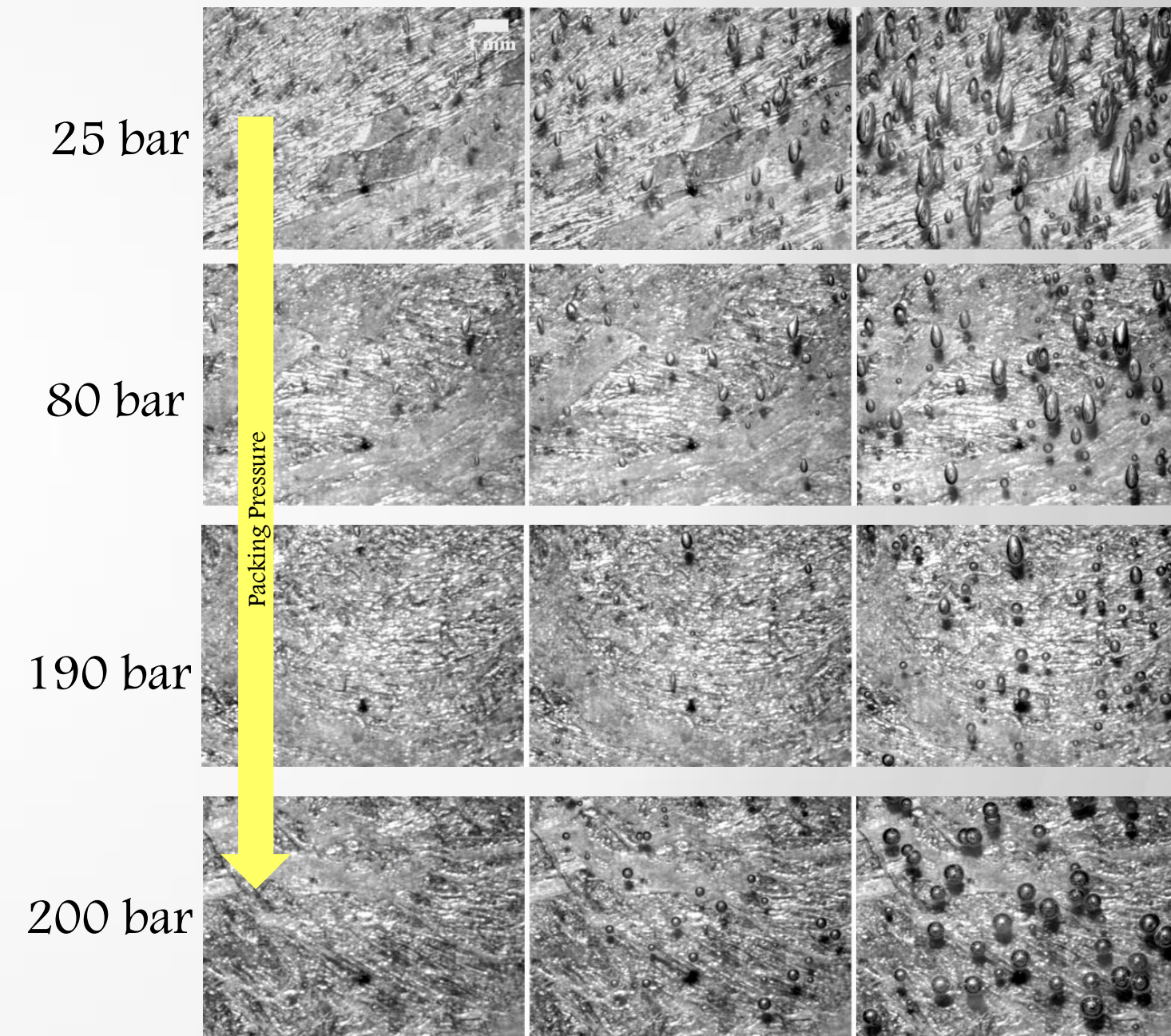
we are looking  
at this spot



# Effect of Processing Parameters on Nucleation Mechanism in High-Pressure FIM



Injection speed 80 cm<sup>3</sup>/s



High-resistant gate



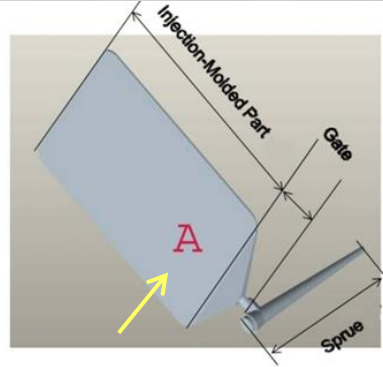
# Mechanism of Bubble Formation using Gas-Counter Pressure

Materials:

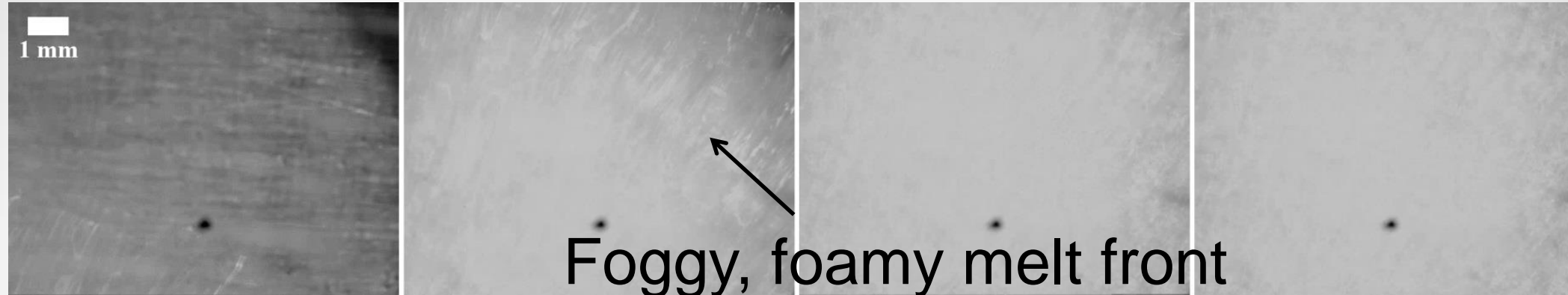
- PS (MC3650) from AmericasStyrenics (MFI: 13.0 gr/10min);
- CO<sub>2</sub> & N<sub>2</sub>: Linde Gas Canada;



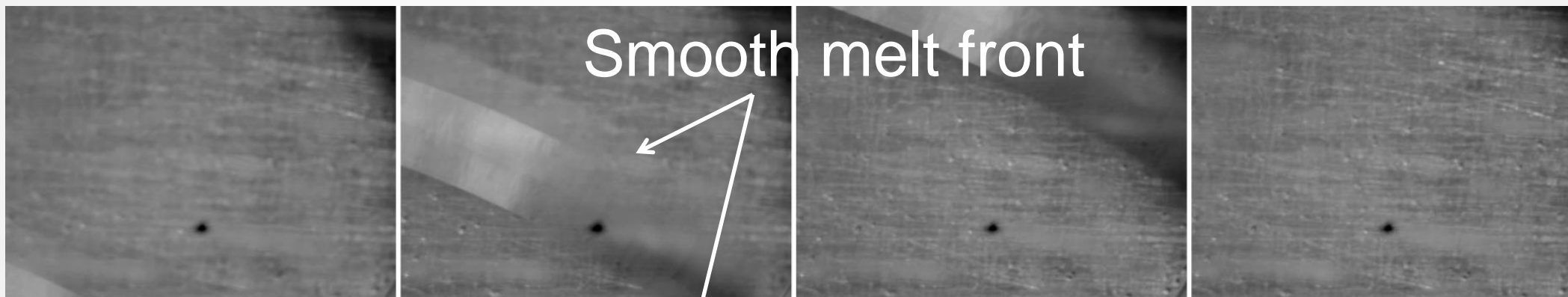
# Full-shot FIM + GCP



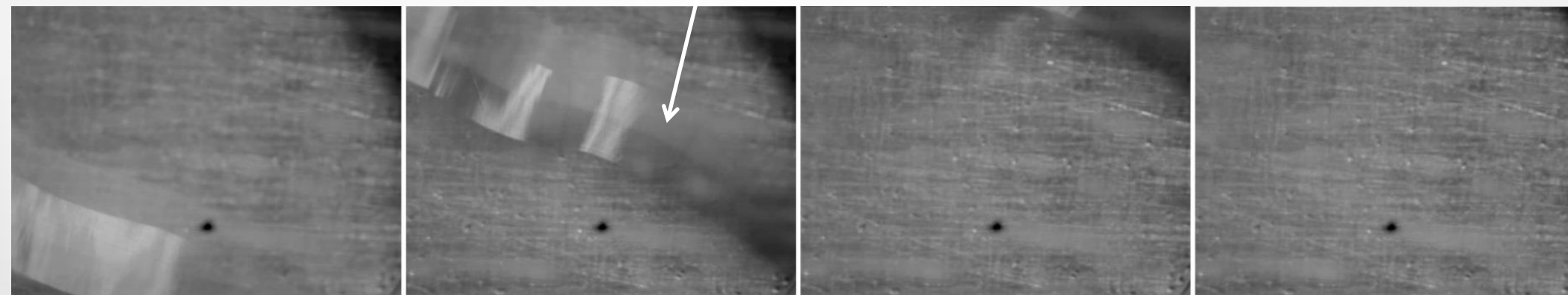
NO GCP



GCP=  
200 psi

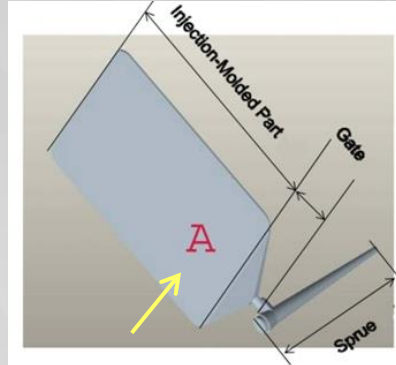


GCP=  
400 psi

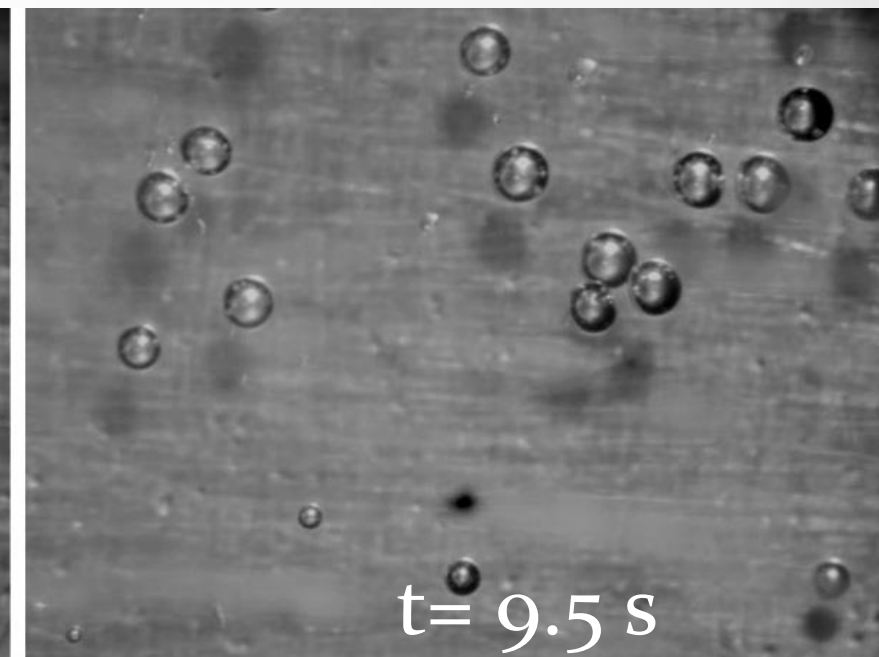
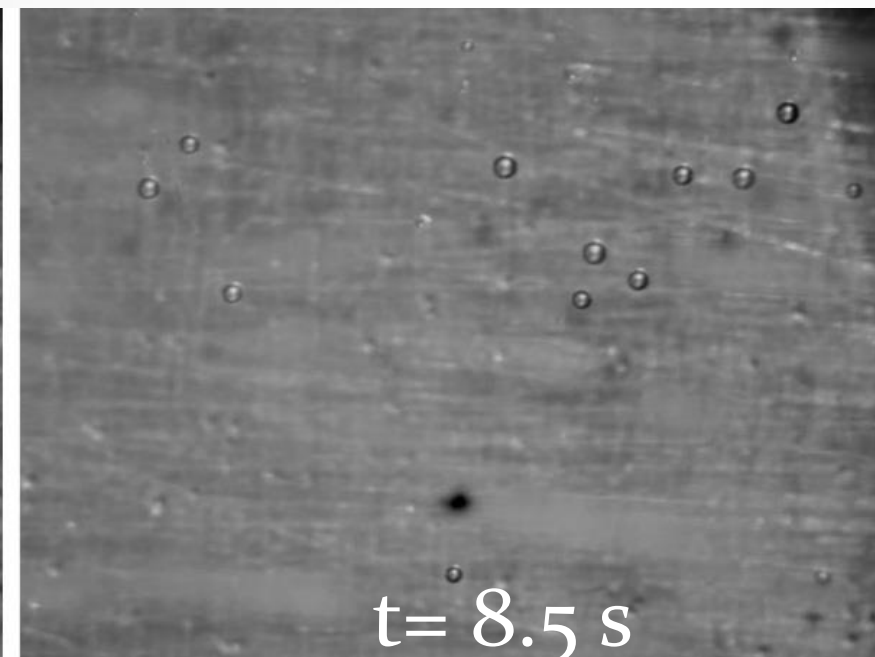
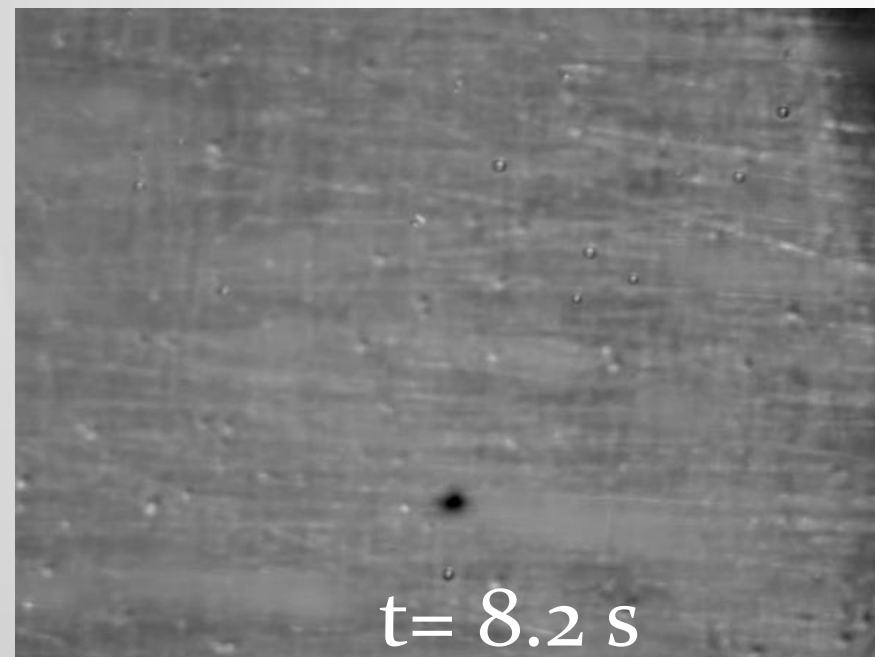
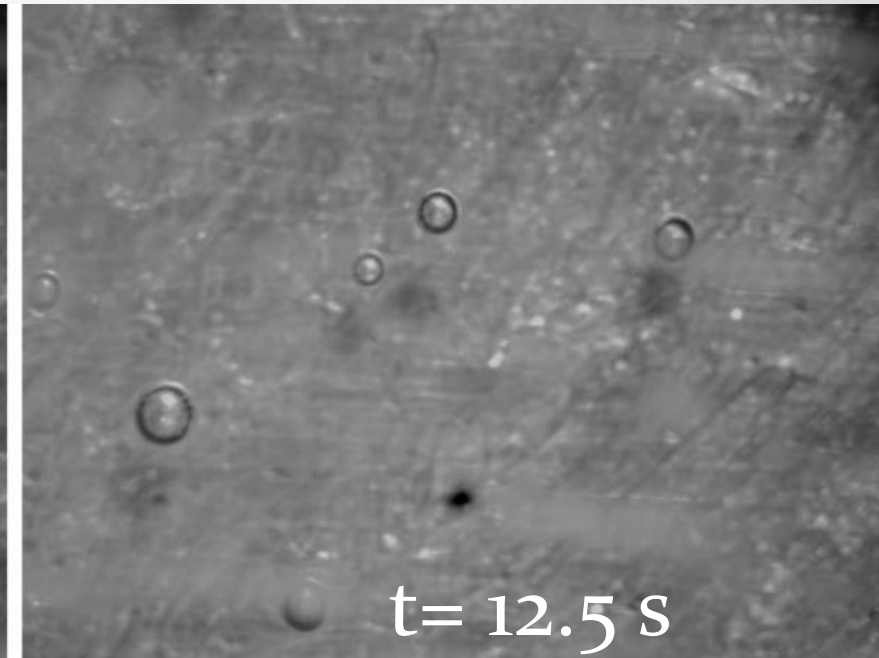
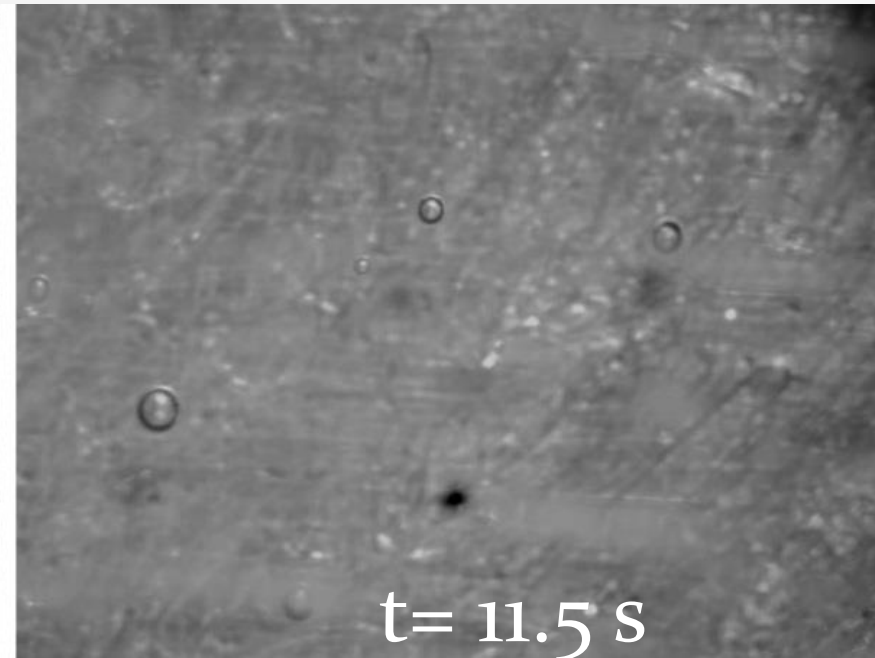
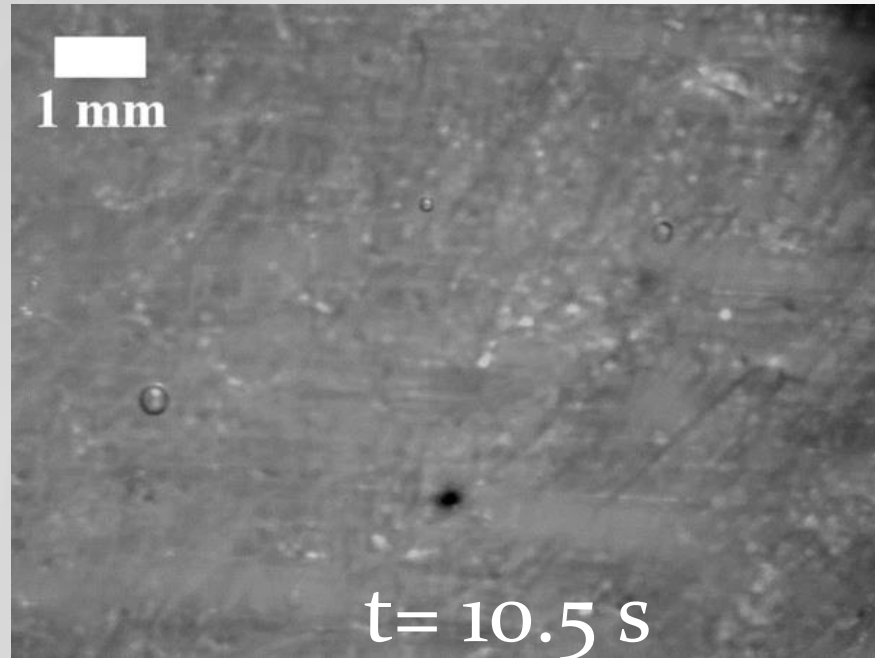


PS/CO<sub>2</sub> (1 % CO<sub>2</sub>; Speed: 35 cc/s; T<sub>melt</sub>: 230 °C)

# Full-shot FIM + GCP



we are looking at this spot



PS/CO<sub>2</sub> (1 % CO<sub>2</sub>; Speed: 35 cc/s;  $T_{\text{melt}}$ : 230 °C)

# High-Pressure Foam Injection Molding with High Expansion

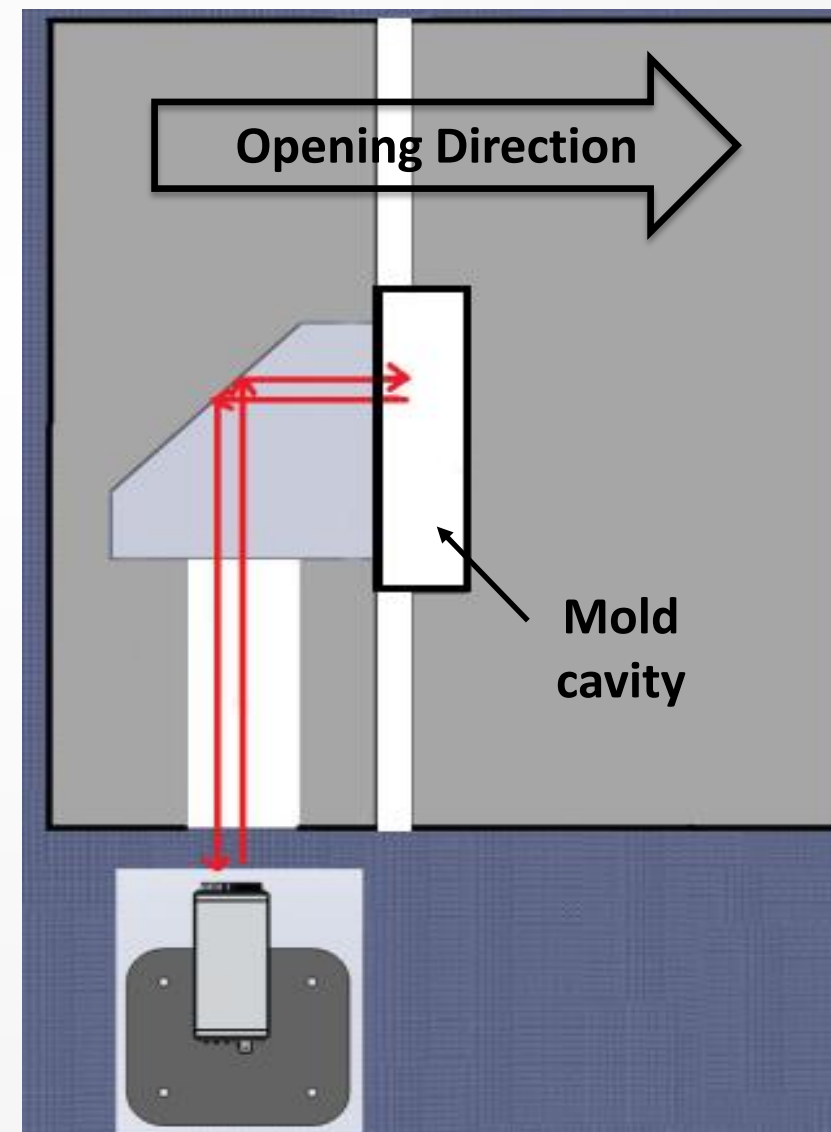
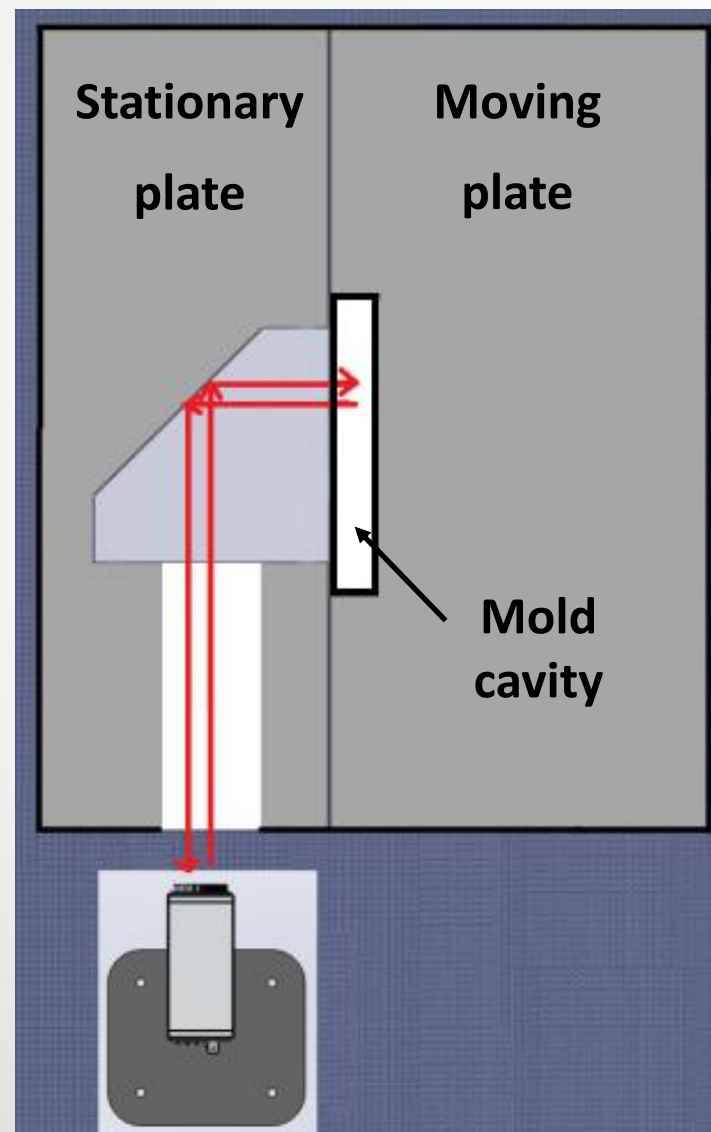
Materials:

- PS675 from AmericasStyrenics (MFI: 7.5 gr/10min);
- CO<sub>2</sub>: Linde Gas Canada;



# High-Pressure Foam Injection Molding with High Expansion

- To increase the void fraction (i.e., the expansion ratio)

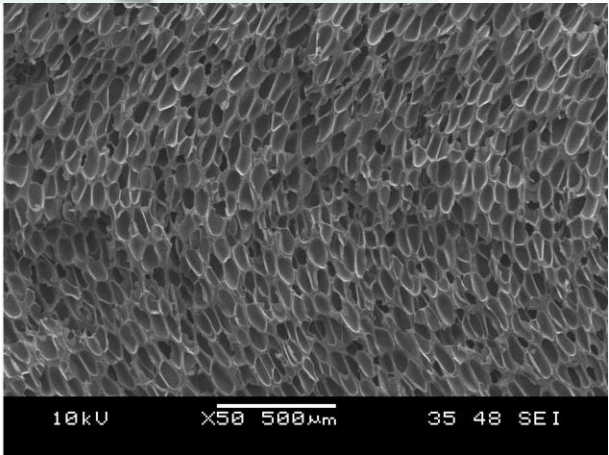
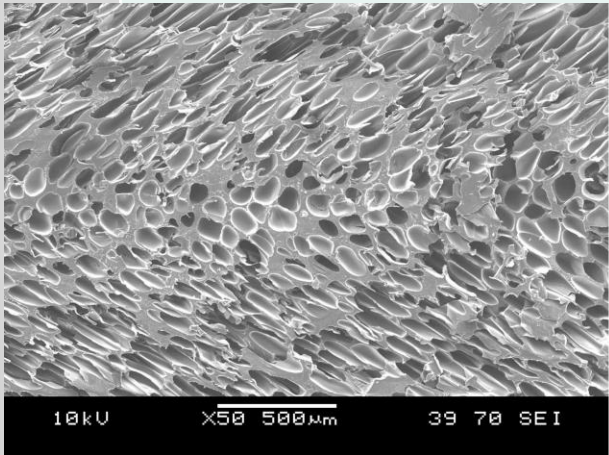


#AU2015

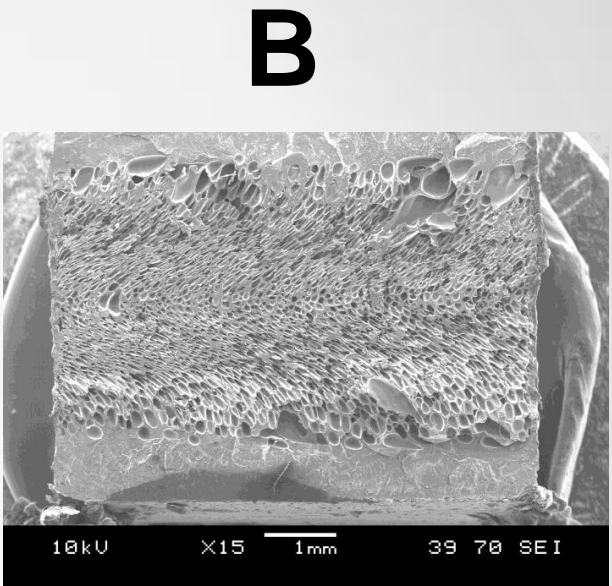
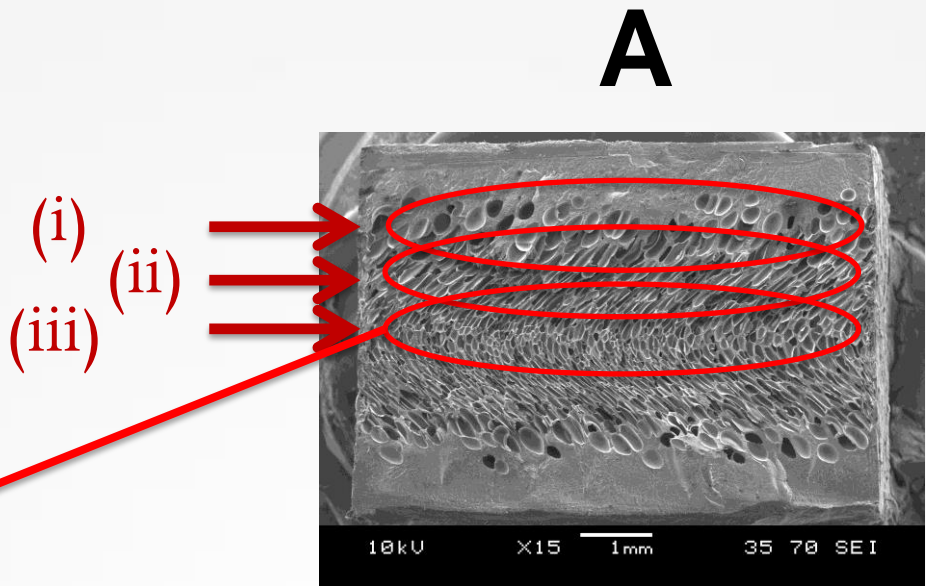


# Experiment

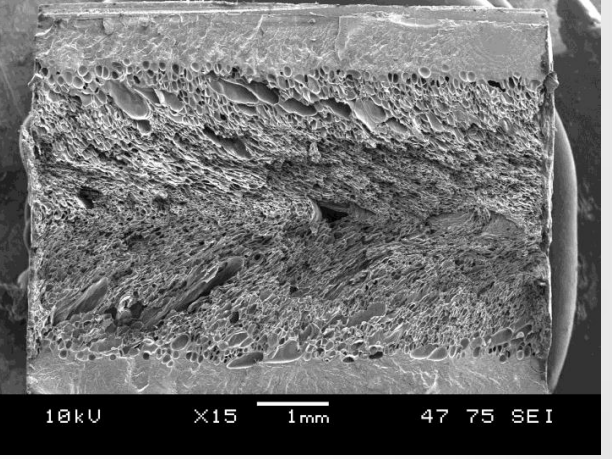
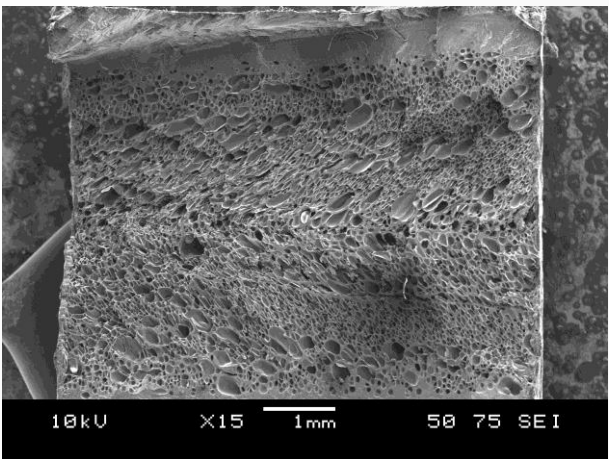
Processing parameter	Value
Shot Size	62 cm <sup>3</sup>
Gas concentration	5% wt



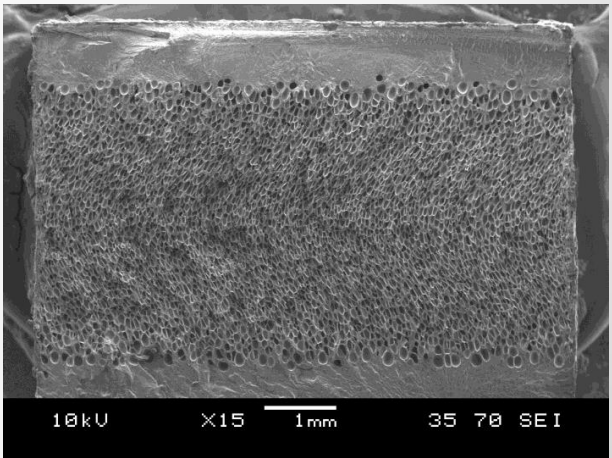
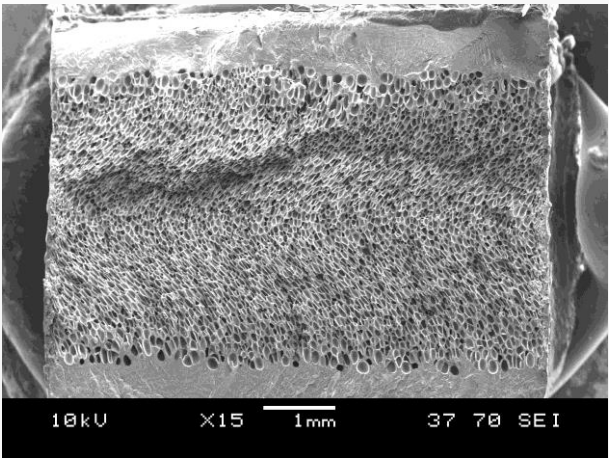
MO Speed	50 mm/s
MO Distance	2 mm
Cooling Time	30 s



6 MPa

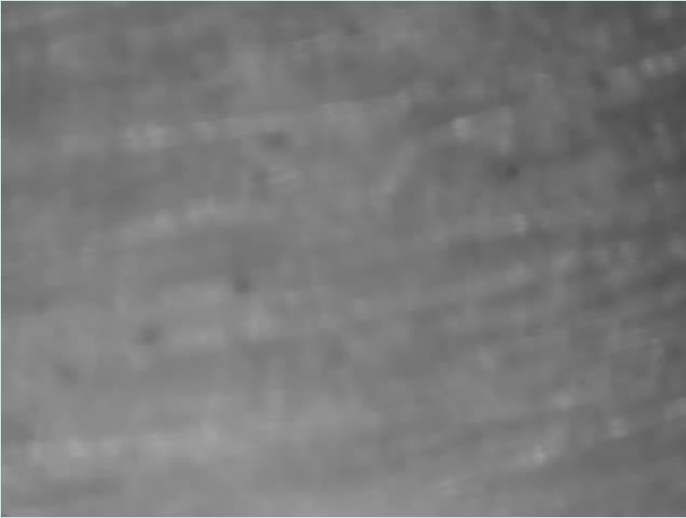
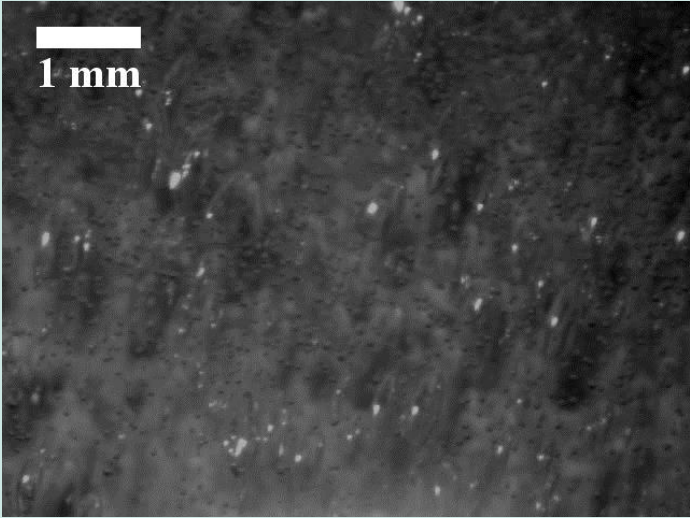
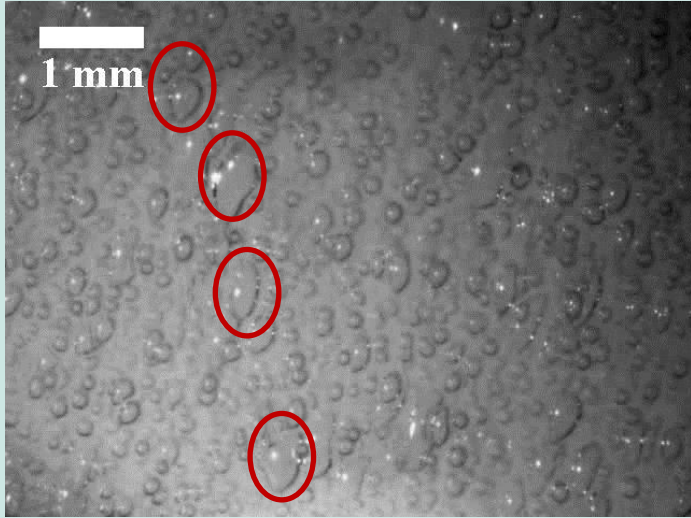
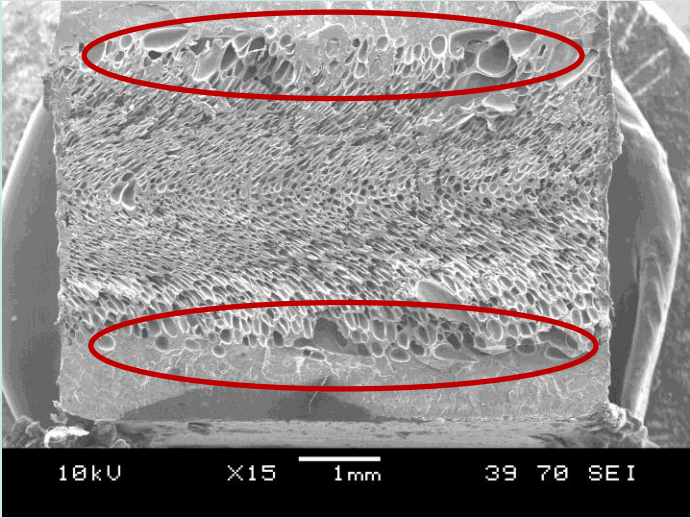

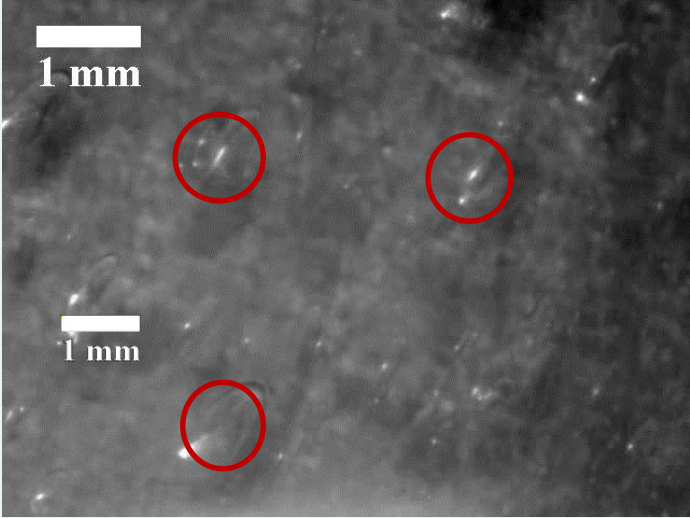
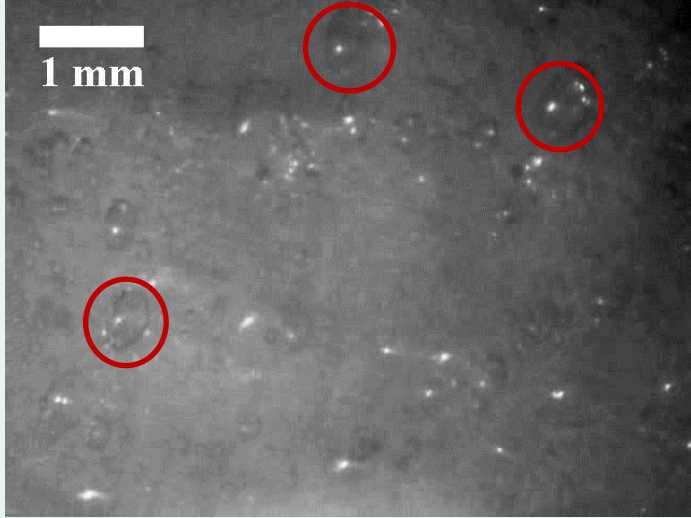
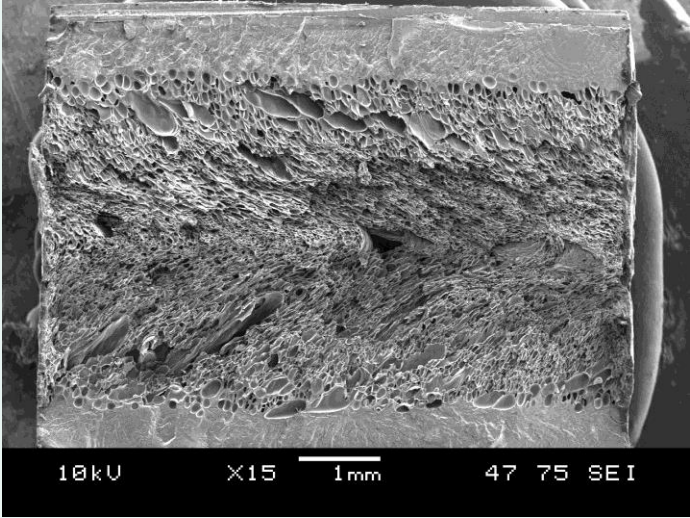



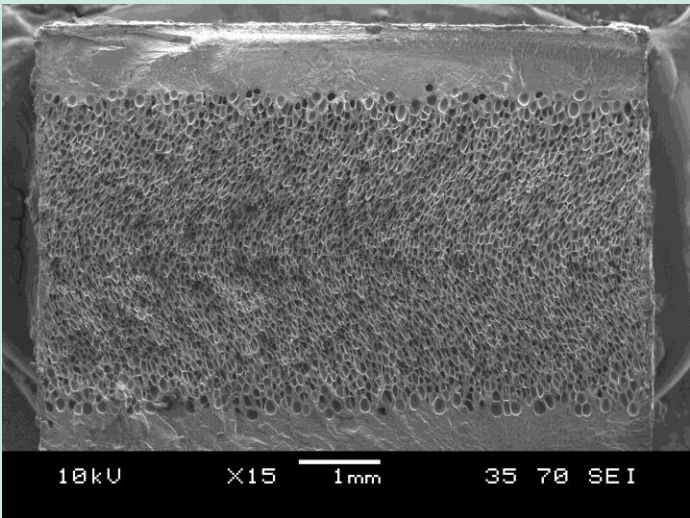


14 MPa



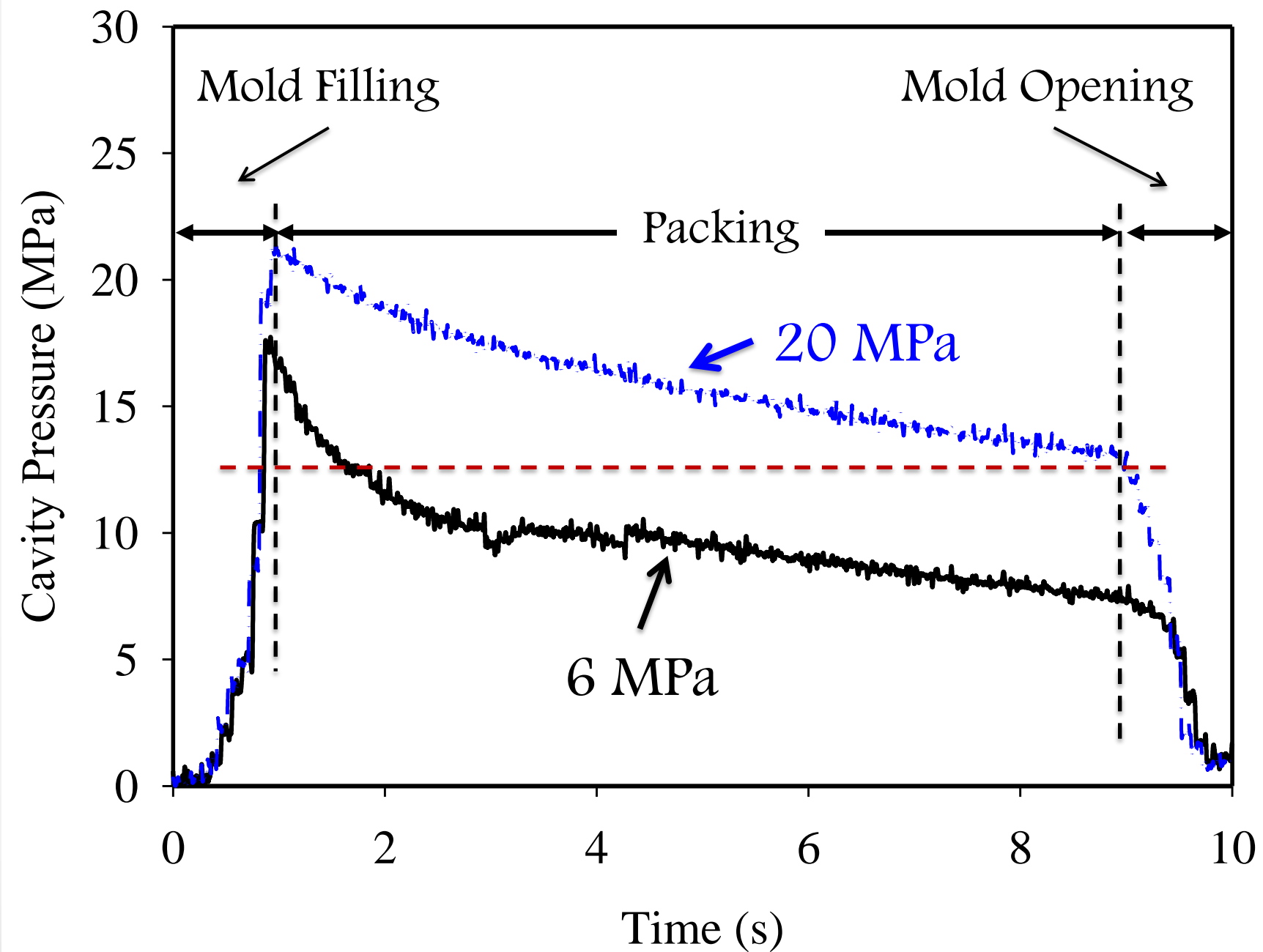
20 MPa



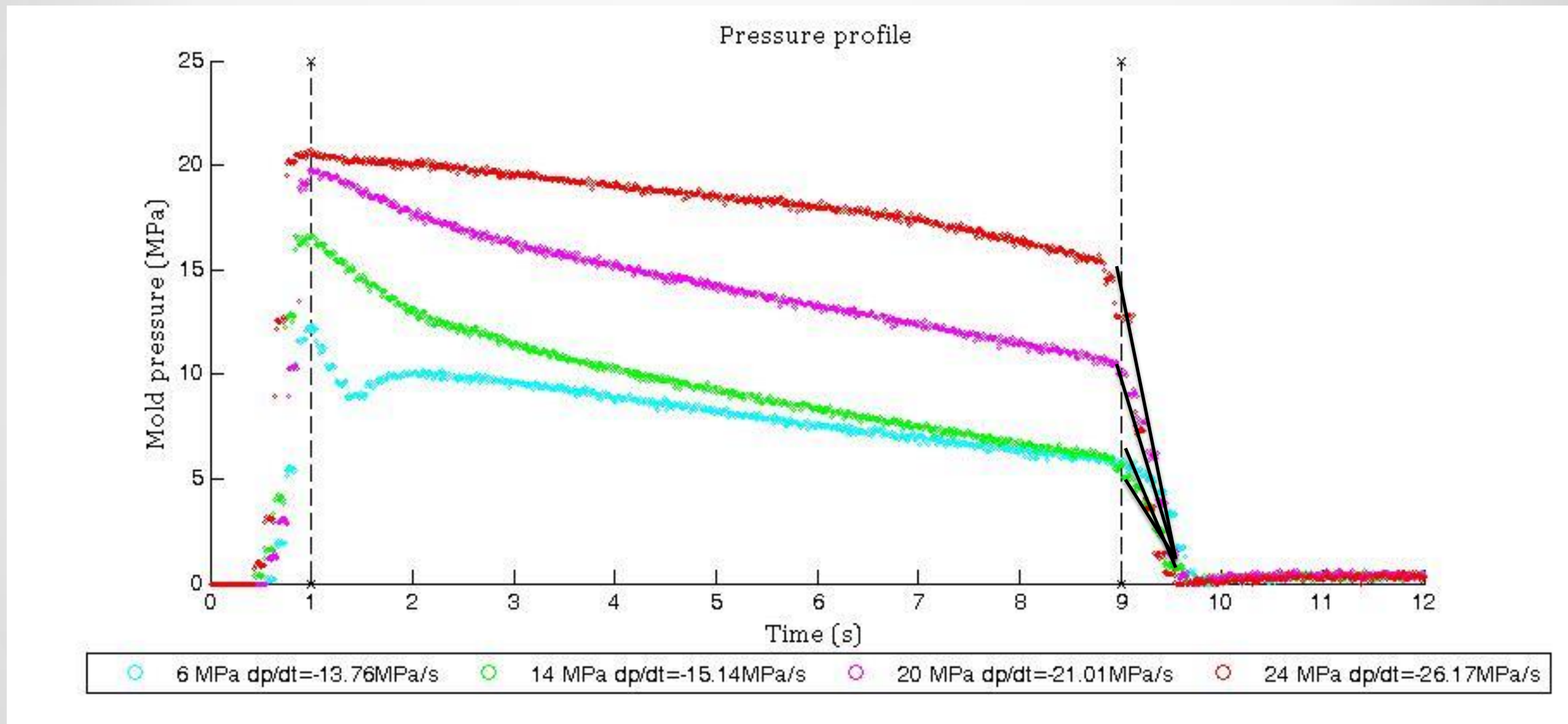
Packing Pressure	Video at Location B	Before MO (10.15s)	After MO (11.45s)	SEM at Location B
<u>6</u> MPa				
14 MPa				
20 MPa				



# Cavity Pressure Profiles



# Pressure Drop rate



# High-Pressure Foam Injection Molding with High Expansion

- High expansion
- Pressure-drop on the entire part → improved structural uniformity
- By removing all gate-nucleated bubbles (with application of proper packing pressure)
  - more gas supply for new nucleation (increased nucleation driving force)
  - no elongated bubble → improved homogeneity
  - proper packing pressure → higher pressure drop rate after opening → higher final cell density

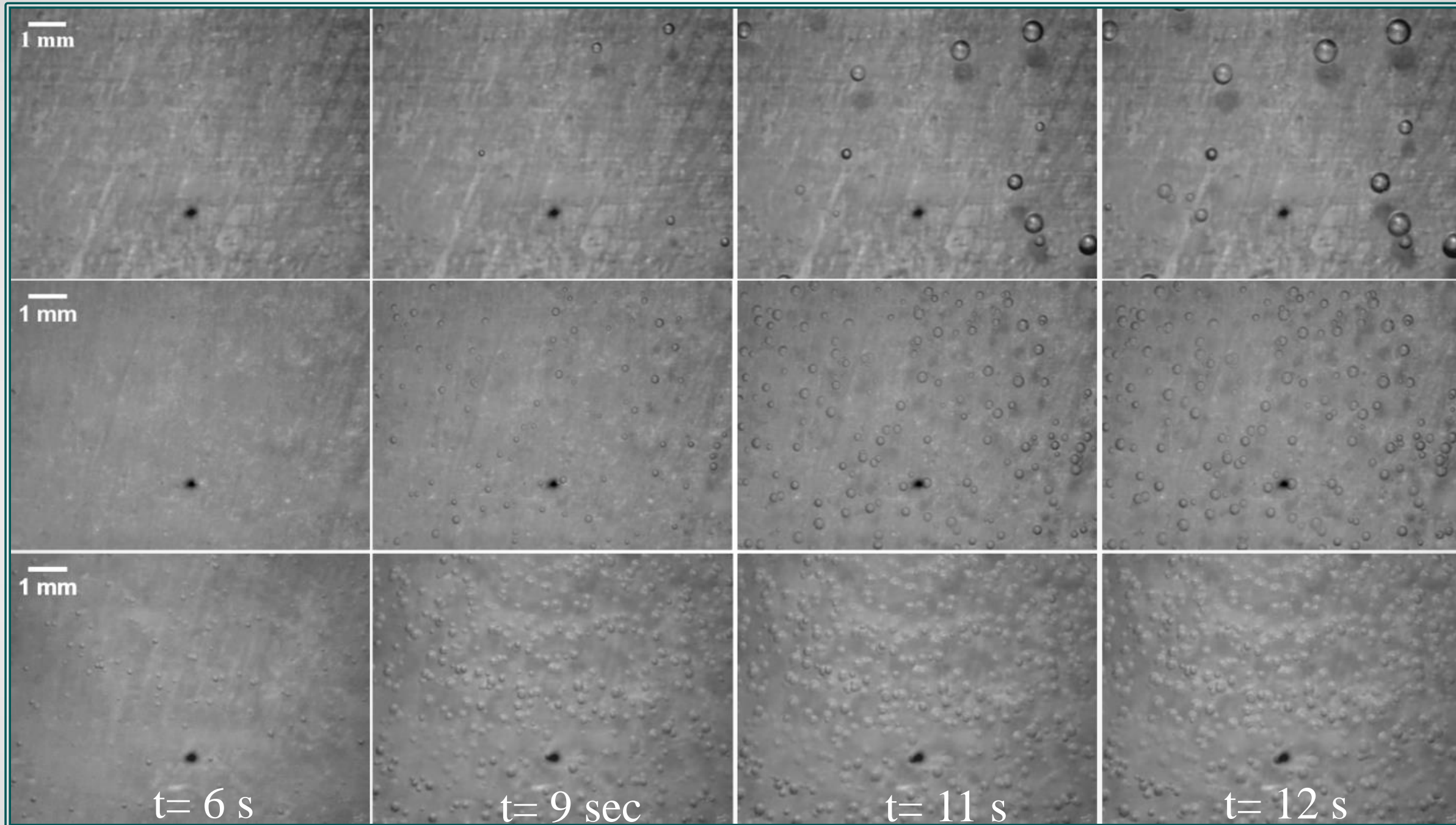


# Effect of Nucleating Agent (Talc) & Effect of Crystals

- PS675 from AmericasStyrenics (MFI: 7.5 gr/10min);
- PP DM55Pharm, Borealis (MFI: 2.8 gr/10min, Homopolymer);
- CO<sub>2</sub>: Linde Gas Canada

# High-Pressure Foam Injection Molding using Talc

PS

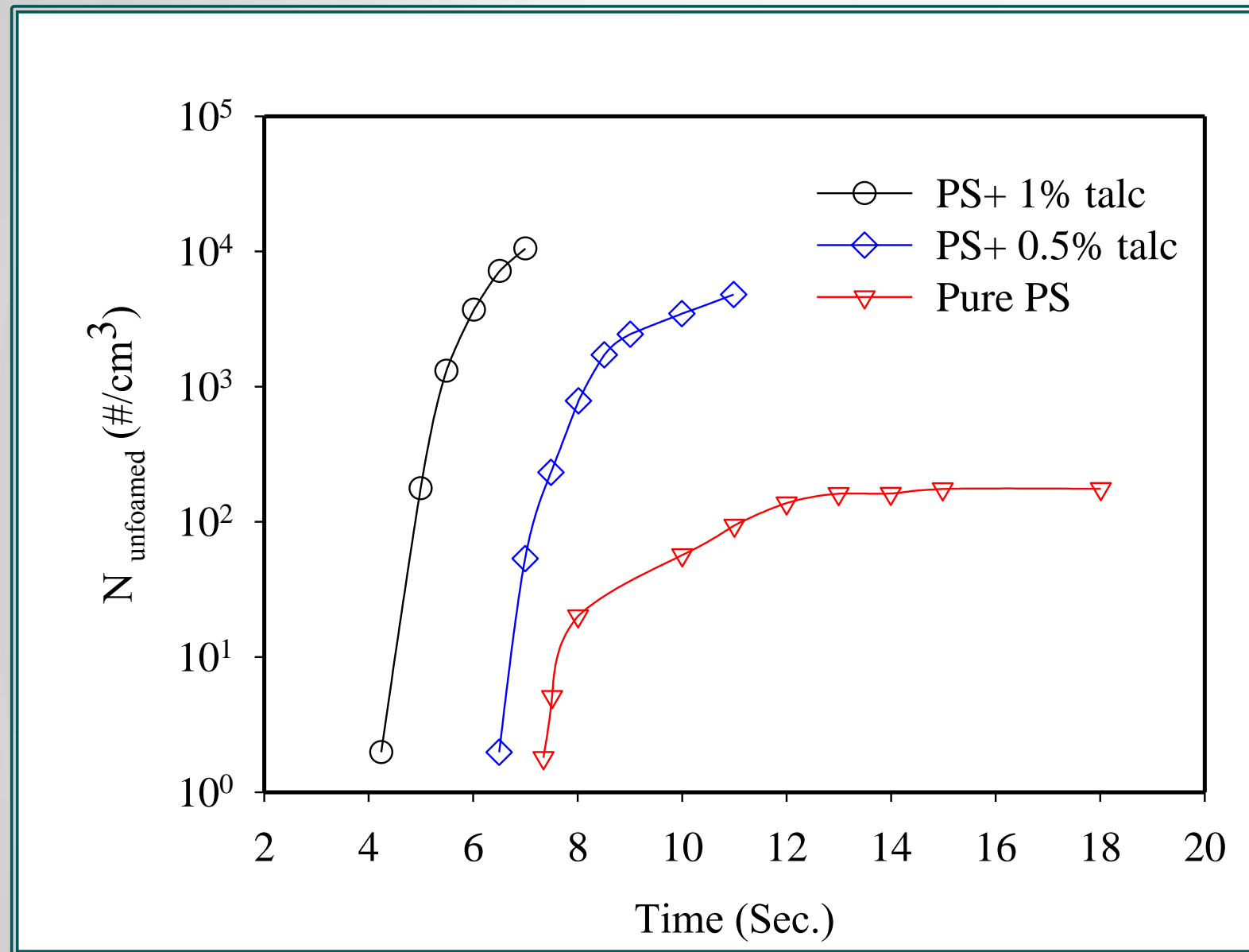


PS +  
0.5% talc

PS +  
1% talc

PS/CO<sub>2</sub> (1% CO<sub>2</sub>; Speed: 80 cc/s; T<sub>melt</sub>: 230 °C)

# High-Pressure Foam Injection Molding using Talc



$$W_{hom} = \frac{16 \gamma^3}{3 (P_{bub,cr} - (P_{sys} + \Delta P_{local}))^2}$$

$$W_{het} = W_{hom} F(\theta_c, \beta)$$

$$F(\theta_c, \beta) \leq 1$$

$$F(\theta_c, \beta) = \frac{1}{4} \left[ 2 - 2 \sin(\theta_c - \beta) + \frac{\cos \theta_c \cos^2(\theta_c - \beta)}{\sin \beta} \right]$$



# Importance of Nucleating Agents (Talc, Crystal)

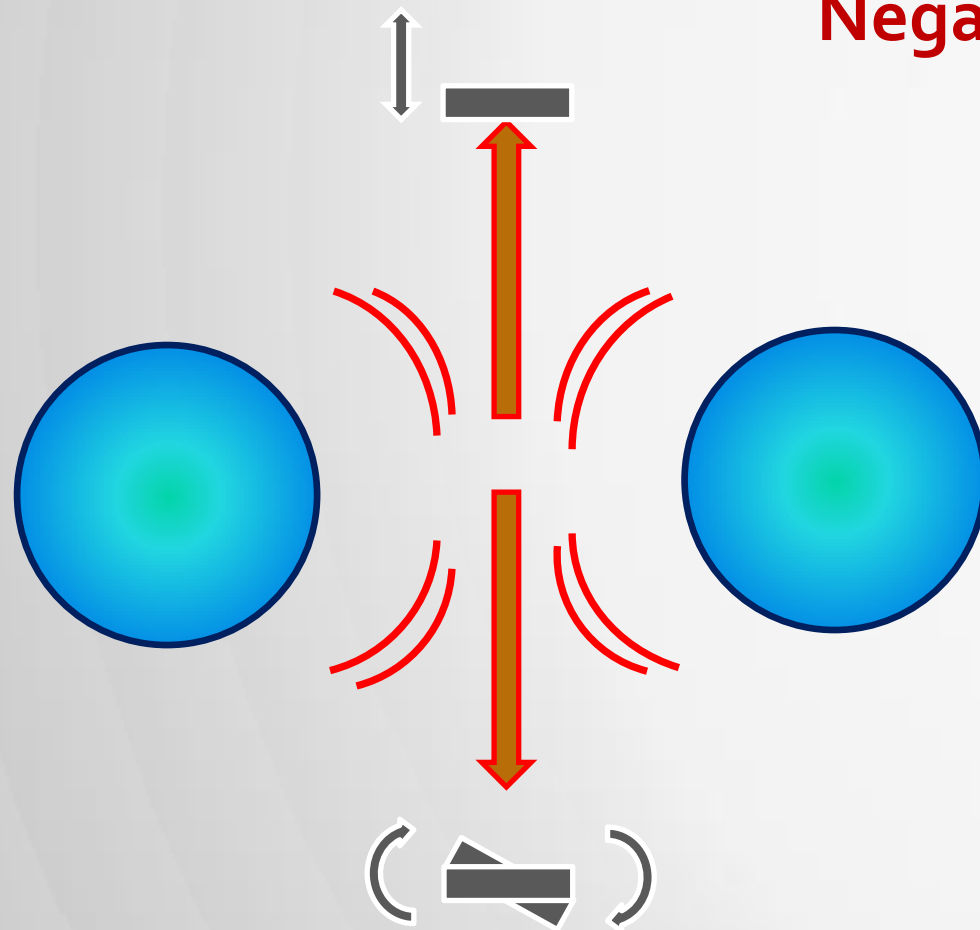
- Heterogeneous nucleation

$$w_{het} = w_{hom} F(\theta_c, \beta); F(\theta_c, \beta) \leq 1$$

- Pressure fluctuations about the exclusion

Bubble expansion → tangential stretching on the bubble wall → flow field in the surroundings

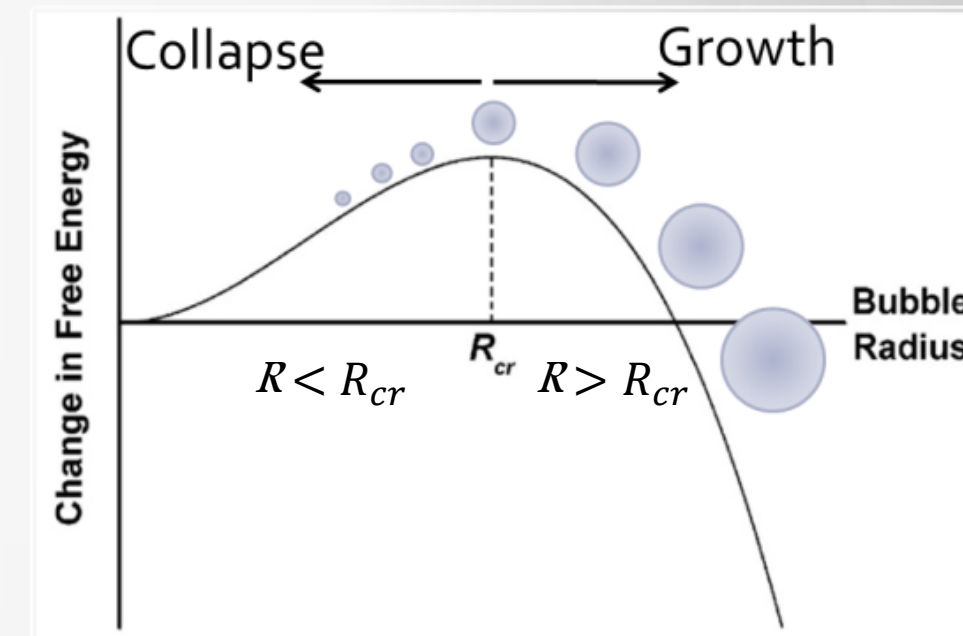
**Negative local pressure fluctuations (tensile)**



$$R_{cr} = \frac{2\gamma}{P_{bub,cr} - (P_{sys} + \Delta P_{local})}$$

Level of supersaturation ↑

Formation of baby bubbles



$$R_{cr} = \frac{2\gamma}{P_{bub,cr} - P_{sys}}$$

# Summary

**Low-pressure FIM:** Gate-nucleated cells; high void fraction; poor structural uniformity and fair cell density

**High-pressure FIM:** Shrinkage-induced cells; improved structural uniformity; low void fraction and cell density

**FIM+GCP:** Nucleation upon GCP release; fast cell nucleation; improved surface quality;

**High-pressure FIM+MO:** Cell nucleation during MO, high cell density, highly uniform;



# Summary

**In-situ Visualization:** Strong tool/characterization method to

- identify unknown phenomena/mechanisms
- generate reliable experimental data

## Modeling and Simulation



# Simulation of Microcellular Injection Molding Process



# Simulation of Microcellular Injection Molding Process

- **Topics**

- **Introduction**
- Core-back microcellular injection molding
- Microcellular injection molding using chemical blowing agent
- Effects of gas counter pressure

# Flow Analysis for Microcellular Injection Molding

- **Mass Continuity equation**

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0$$

- **Momentum equation**

$$\rho \frac{D\mathbf{v}}{Dt} = -\nabla p + \nabla \cdot \boldsymbol{\tau} + \rho \mathbf{g}$$

- **Energy equation**

$$\rho C_p \frac{DT}{Dt} = \nabla \cdot (k \nabla T) + \eta \dot{\gamma}^2 + \beta T \frac{Dp}{Dt}$$



# Bubble Growth Modeling

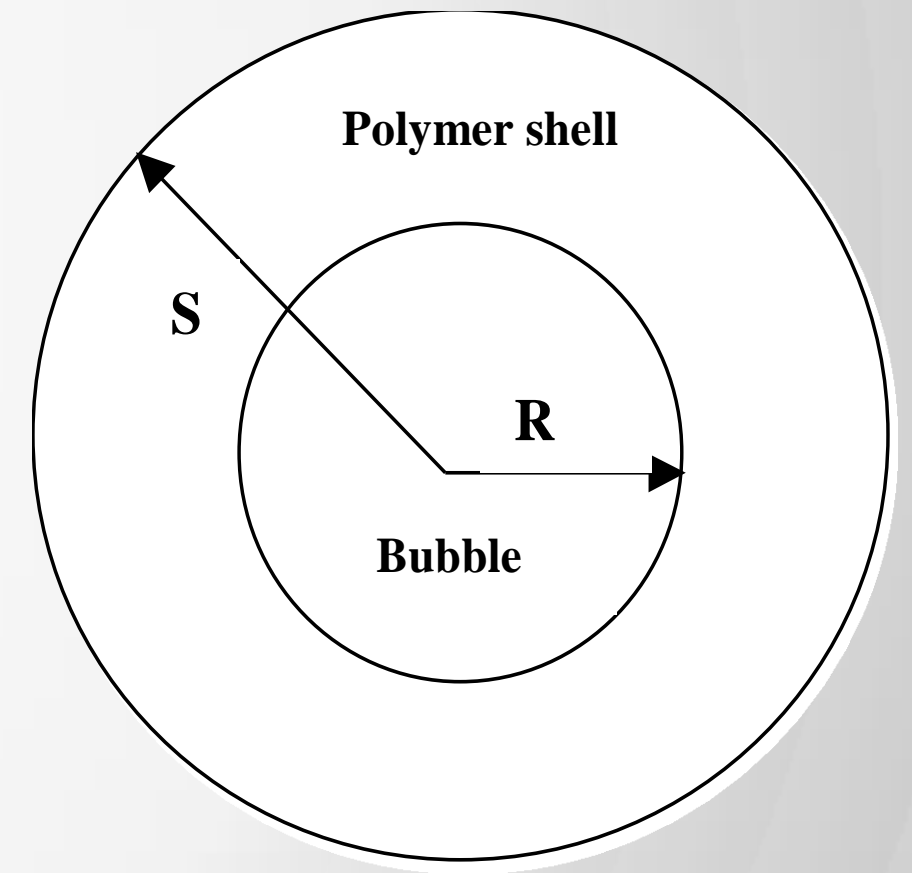
- Expansion of cell due to
  - Hydrodynamic growth due to surrounding fluid

$$4\eta\dot{R} / R = (P_g - P) - 2\sigma / R$$

- Diffusion of gas from envelope into bubble

$$\frac{d}{dt} \left( \frac{p_g R^3}{R_g T} \right) = \frac{6\rho^2 D \kappa_h R_g T (p_{g0} - p_g)^2 R^4}{p_g R^3 - p_{g0} R_0^3}$$

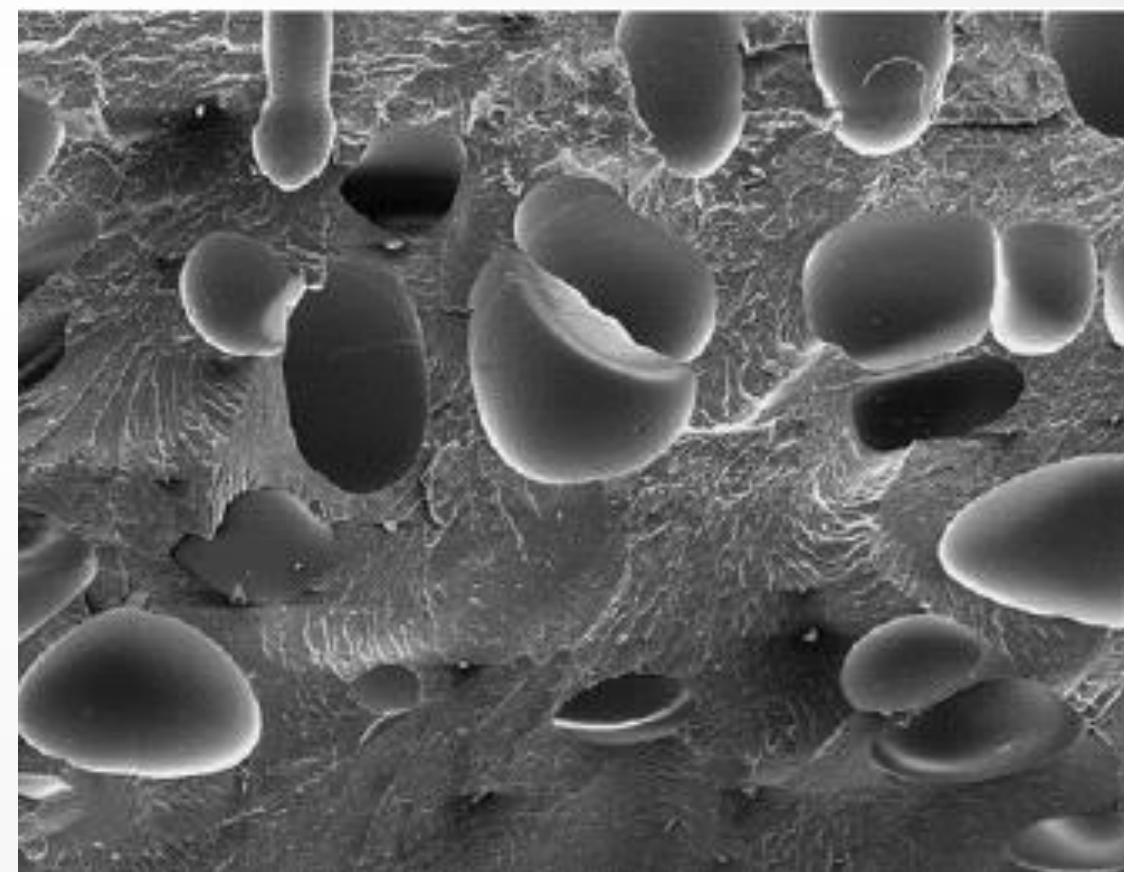
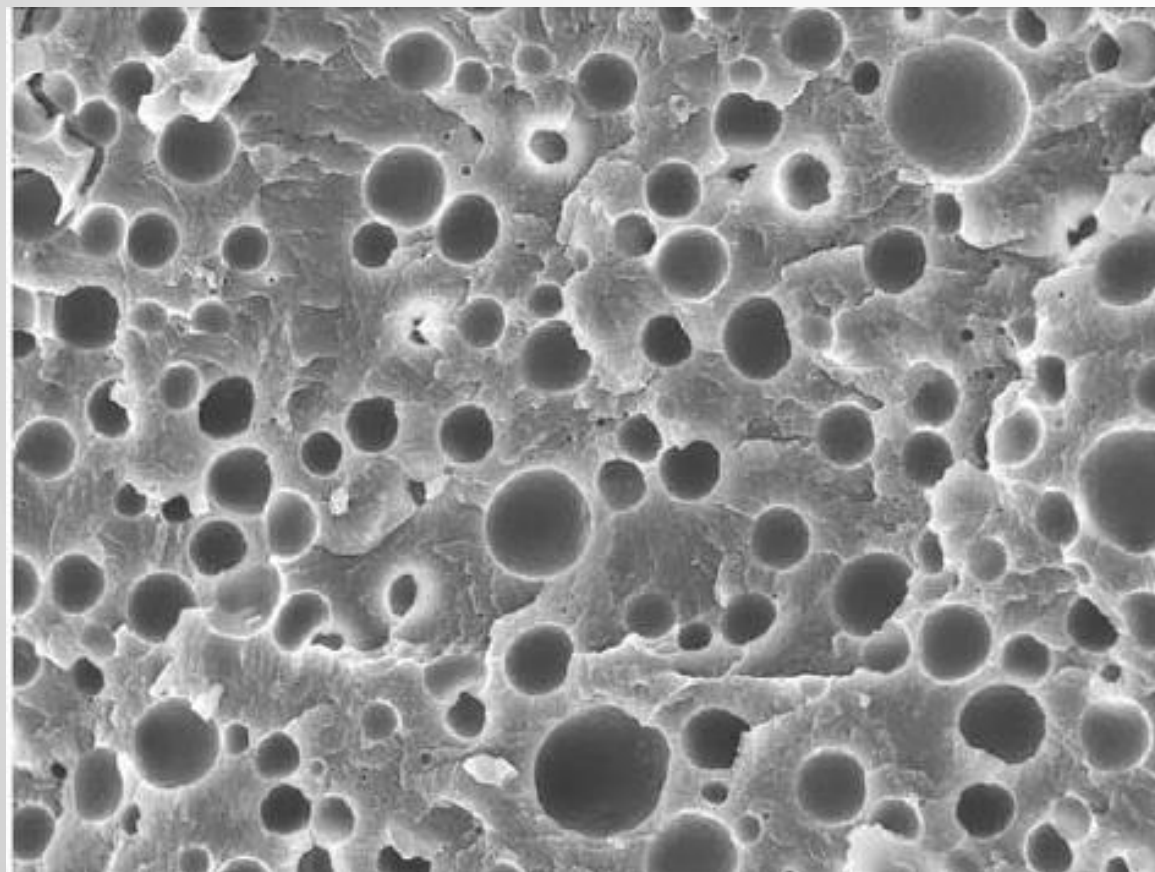
$P_g$  (pressure inside bubble),  $P$  (the melt pressure)  
 $\sigma$  (surface tension),  $R_g$  (Universal gas constant)  
 $R$  (radius of the bubble),  $R_0$  (initial radius of bubble)



(Amon and Denson (Polym. Eng. Sci 1984))

# Bubble Nucleation Model

- Predict the bubble number density distribution in parts produced by microcellular injection molding
- Calculate the effects of effect of **process conditions** and **material properties** on bubble nucleation



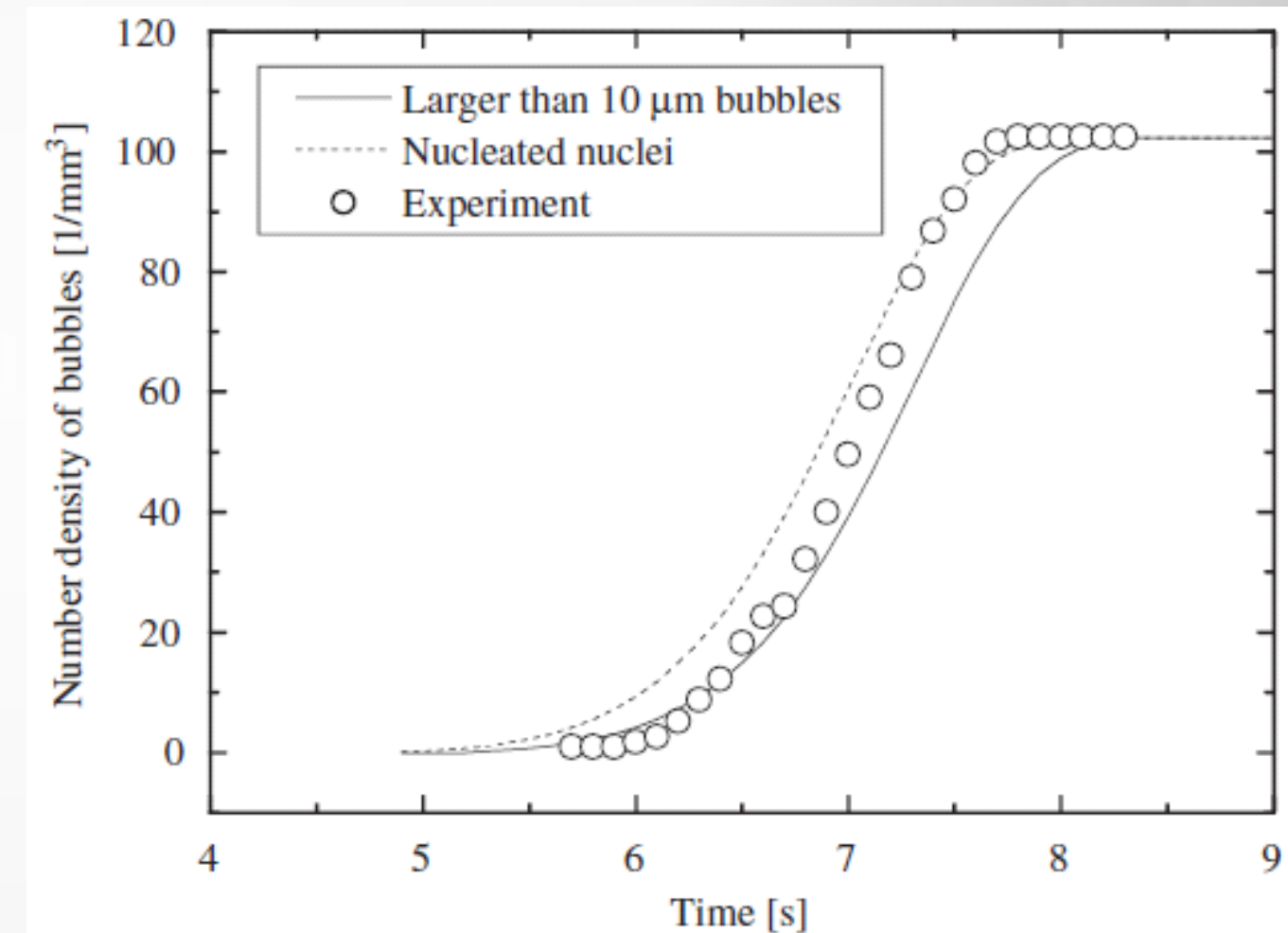
(Yuan & Turng (Polymer, 2005); Lee et al. (Polymer, 2011))

# Fitted Nucleation Model

- **Fit the nucleation model to the actual nucleation density measurement data from the molding experiment**

$$J = F_1 N \left[ \frac{2\sigma}{\pi m B} \right]^{\frac{1}{2}} \exp \left[ \frac{-16 F_2 \pi \sigma^3}{3 k T [P_v - P_l]^2} \right]$$

- $F_1, F_2$ : Determined from fitting



(K. Taki, Chem. Eng. Sci., 2008)



# Material Data Model

- Accurate material data is needed for accurate nucleation calculation
- Surface tension

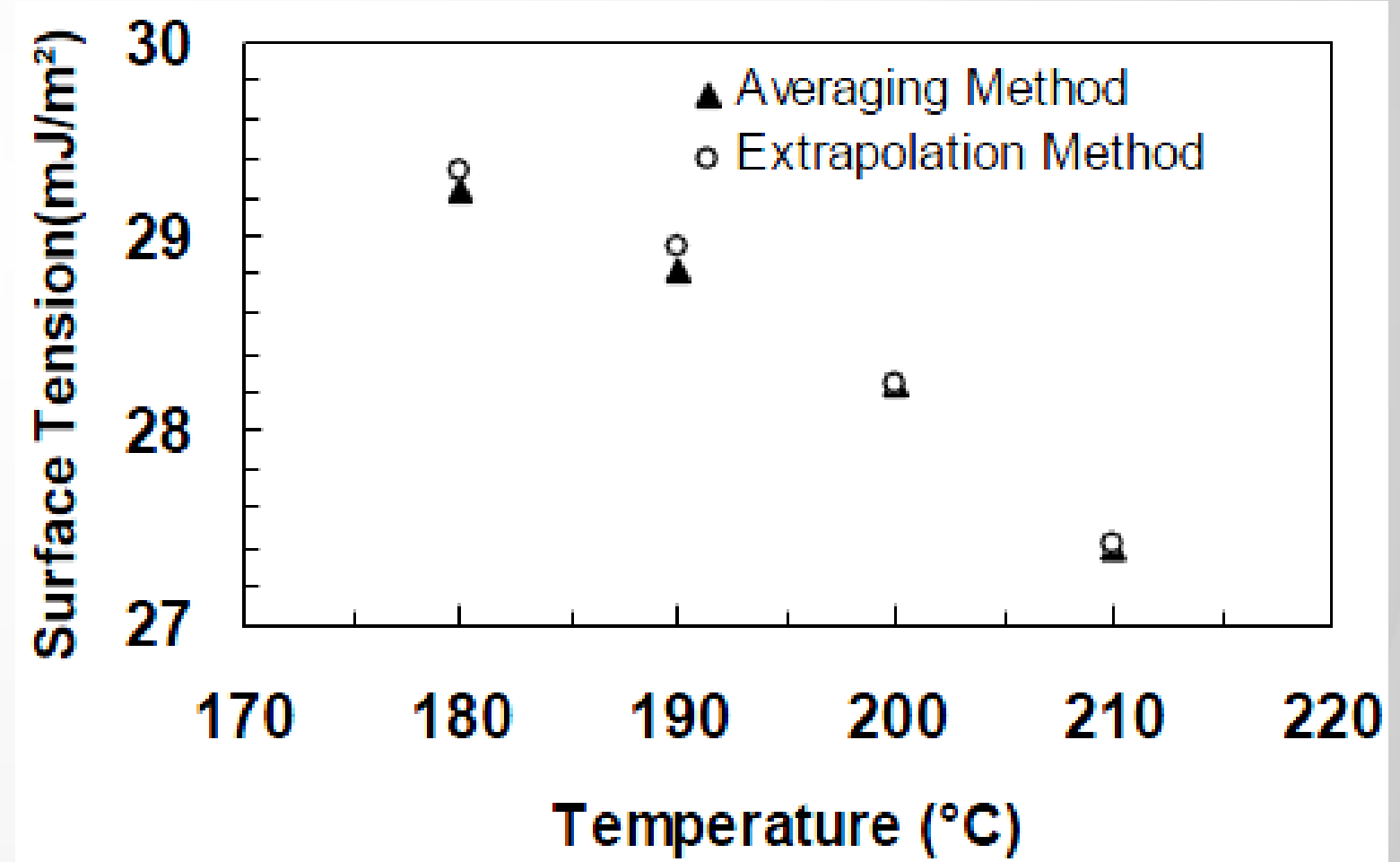
$$\sigma = \sigma_0 \left(1 - \frac{T}{T_c}\right)^{11/9} \quad \text{or} \quad \sigma = \sigma_0 \left(\frac{\rho}{\rho_0}\right)^4$$

- Solubility

$$\kappa_h = \kappa_{h0} \exp\left(\frac{\kappa_{h1}}{T^2}\right)$$

- Diffusivity

$$D = D_0 \exp\left(\frac{D_1}{T}\right)$$



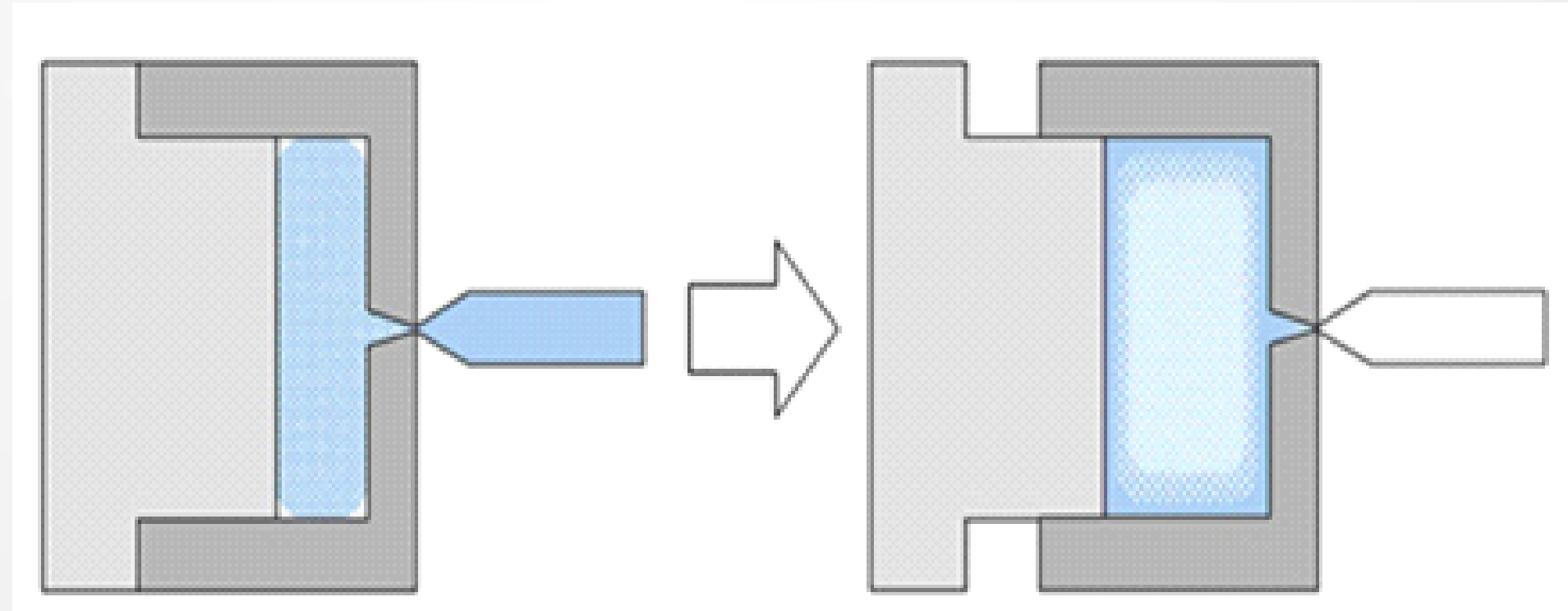
# Simulation of Microcellular Injection Molding Process

## ■ Topics

- Introduction
- **Core-back microcellular injection molding**
- Microcellular injection molding using chemical blowing agent
- Effects of gas counter pressure

# Core-back for Microcellular Injection Molding

- Complete filling & packing before mold opening
- Mold opening: Bubble nucleation and growth with mold opening
- Advantages
  - Better surface quality
  - Higher part **expansion ratio**






# Core-back (Partial Mold Opening) for Microcellular Injection Molding

- Check “Include Core-back” option to run core-back analysis
- Specify distance, speed profile and direction of mold opening

Process Settings Wizard - Fill+Pack Settings - Page 1 of 3



Mold surface temperature: 23.9 C  
Melt temperature: 237.8 C

Filling control  
Injection time of 1.81 s [0:]

Velocity/pressure switch-over (Microcellular)  
By %volume filled at 99 % [50:100]

Pack/holding control  
%Filling pressure vs time Edit profile...

☒ Include Core-back (Microcellular) Edit data...

Cooling time  
Specified of 3 s [0:]

☒ Fiber orientation analysis if fiber material  
☐ Birefringence analysis if material data includes optical properties

Advanced options...  
Fiber parameters...

Core-back data

Core-back open distance: 2.55 mm [0.1:10]

Core-back opening speed vs distance (opening is along z-axis)

	Distance mm [0:10]	Core-back opening speed mm/s [1:50]
1	0	2
2	3	2
3		

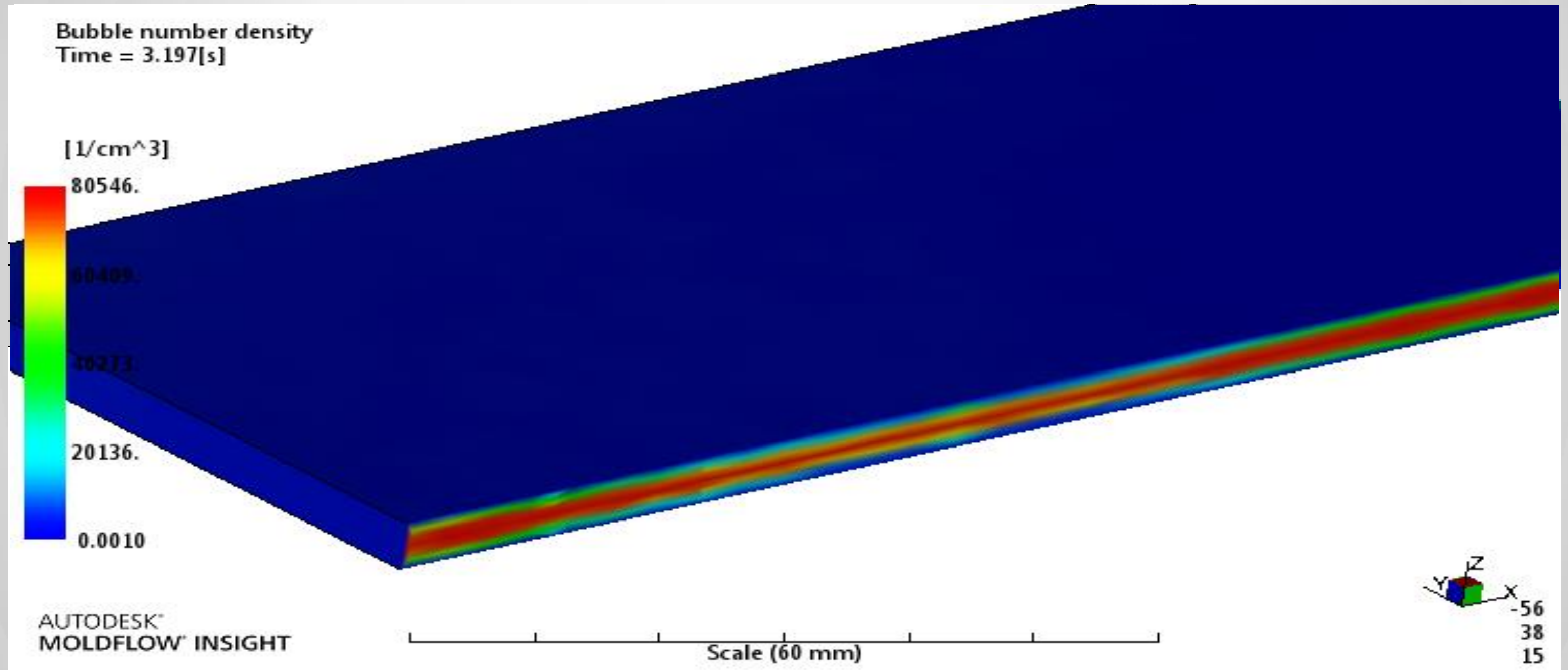
Core-back opening direction: -Z

OK Cancel Help

# Core-back (Partial Mold Opening) for Microcellular Injection Molding

- **Available for analysis sequences that include “Fill+Pack”**
  - Not available for “Fill” only
- **Core-back occurs at the end of the packing phase**
- **Model the elements to be opened using “Compression (3D)” element**
- **Negative values for press displacement or press speed -> Mold opening**

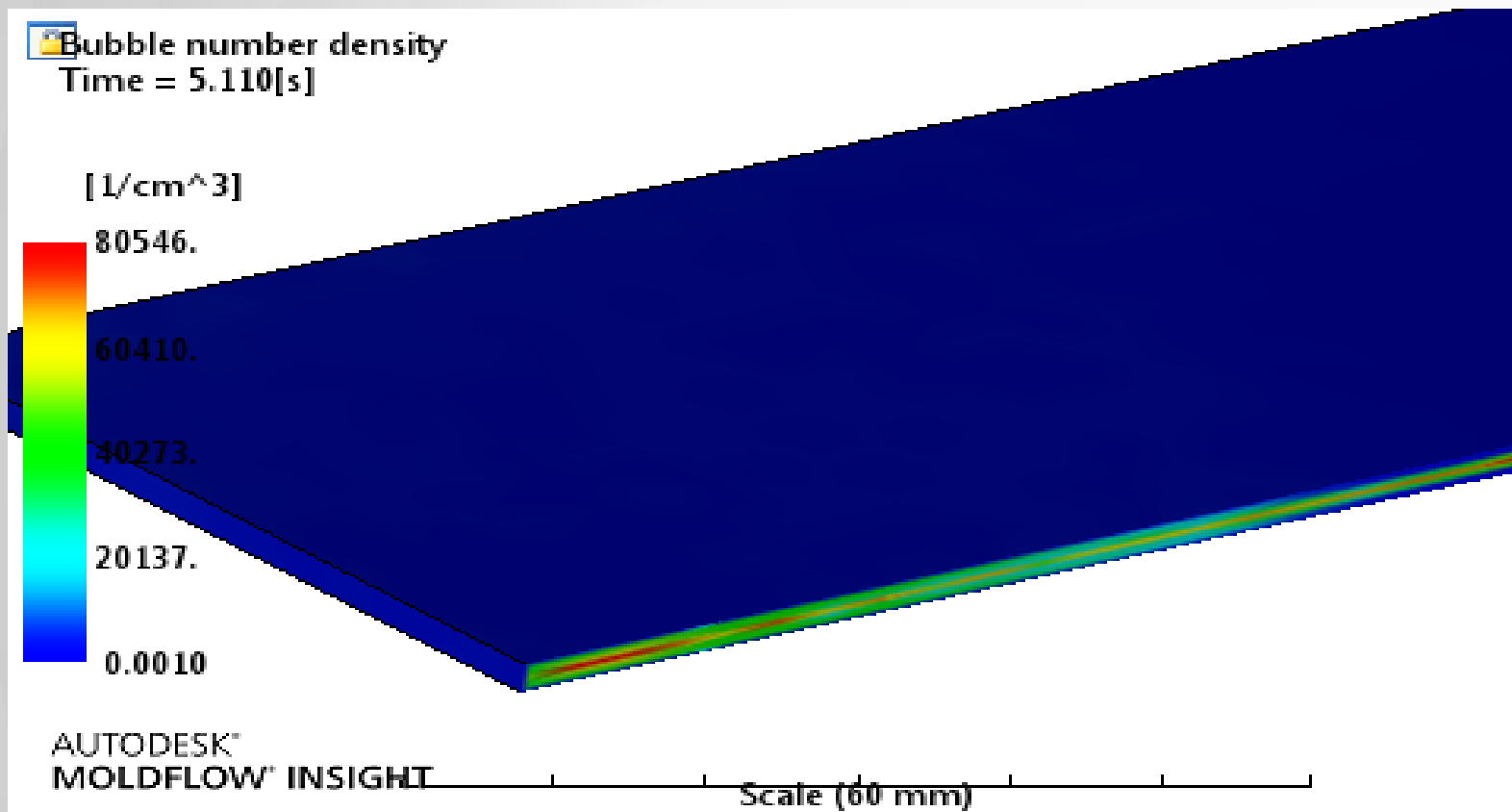
# Case 1: Bubble Number Density Result



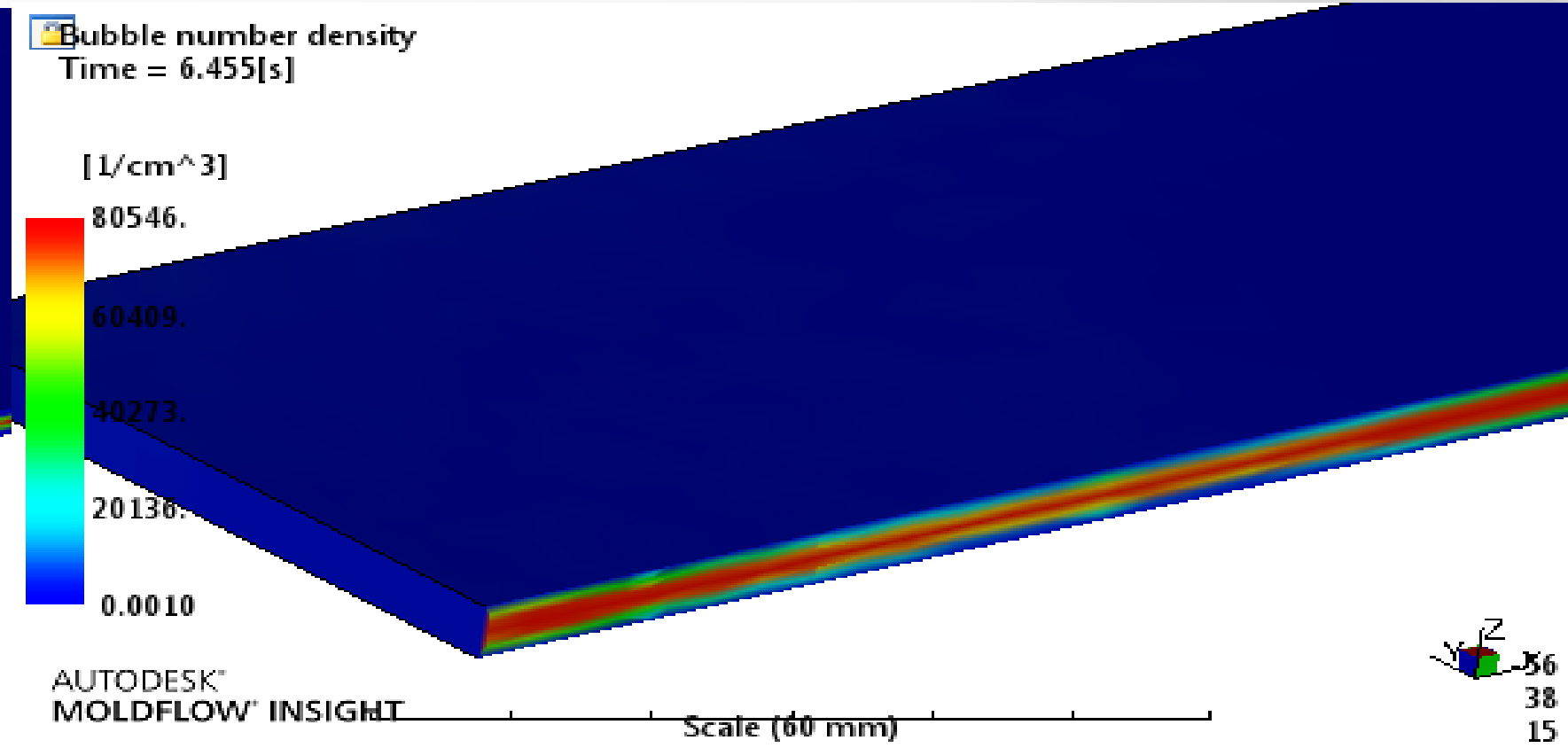


# More Bubbles with Core-Back

## No Core-Back



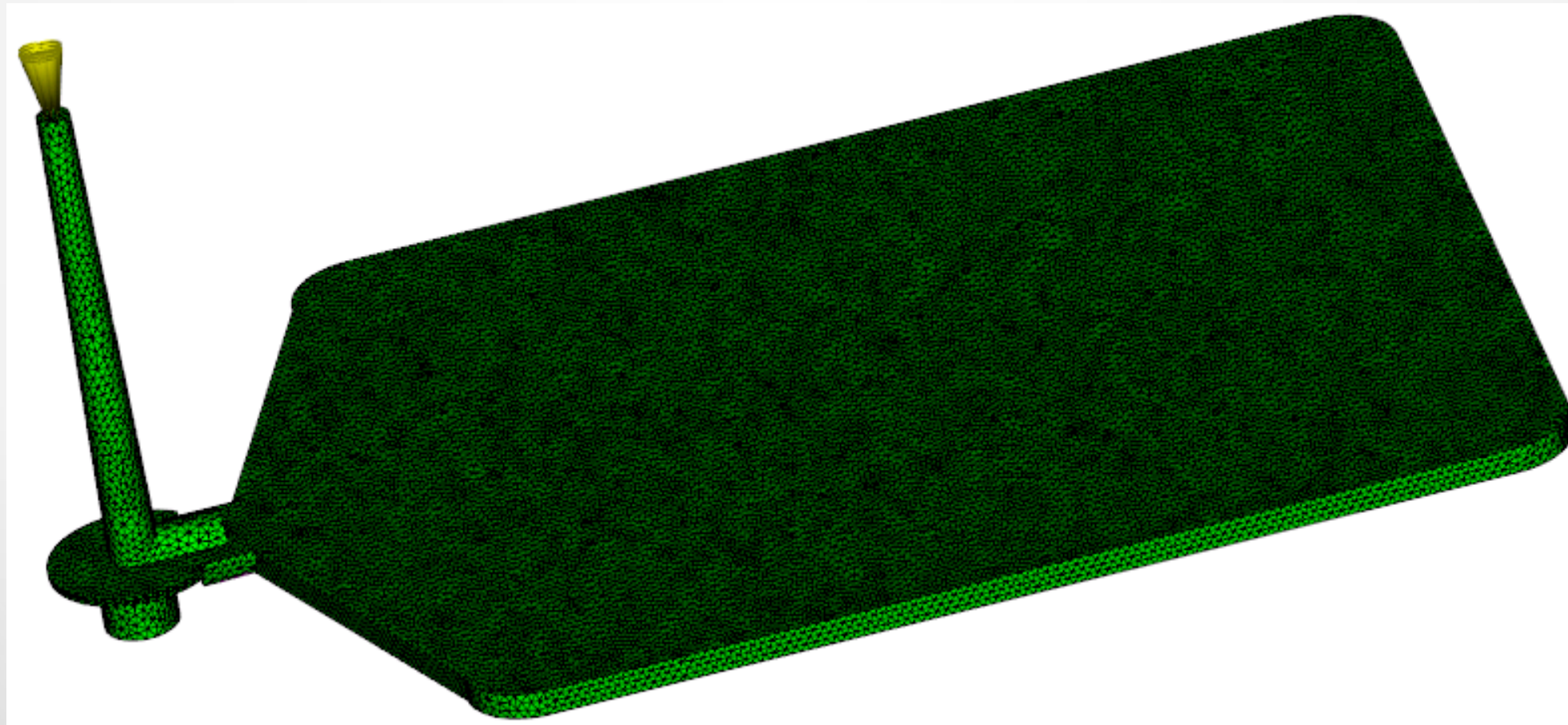
## With Core-Back



**\*Core-back feature only for 3D at present**

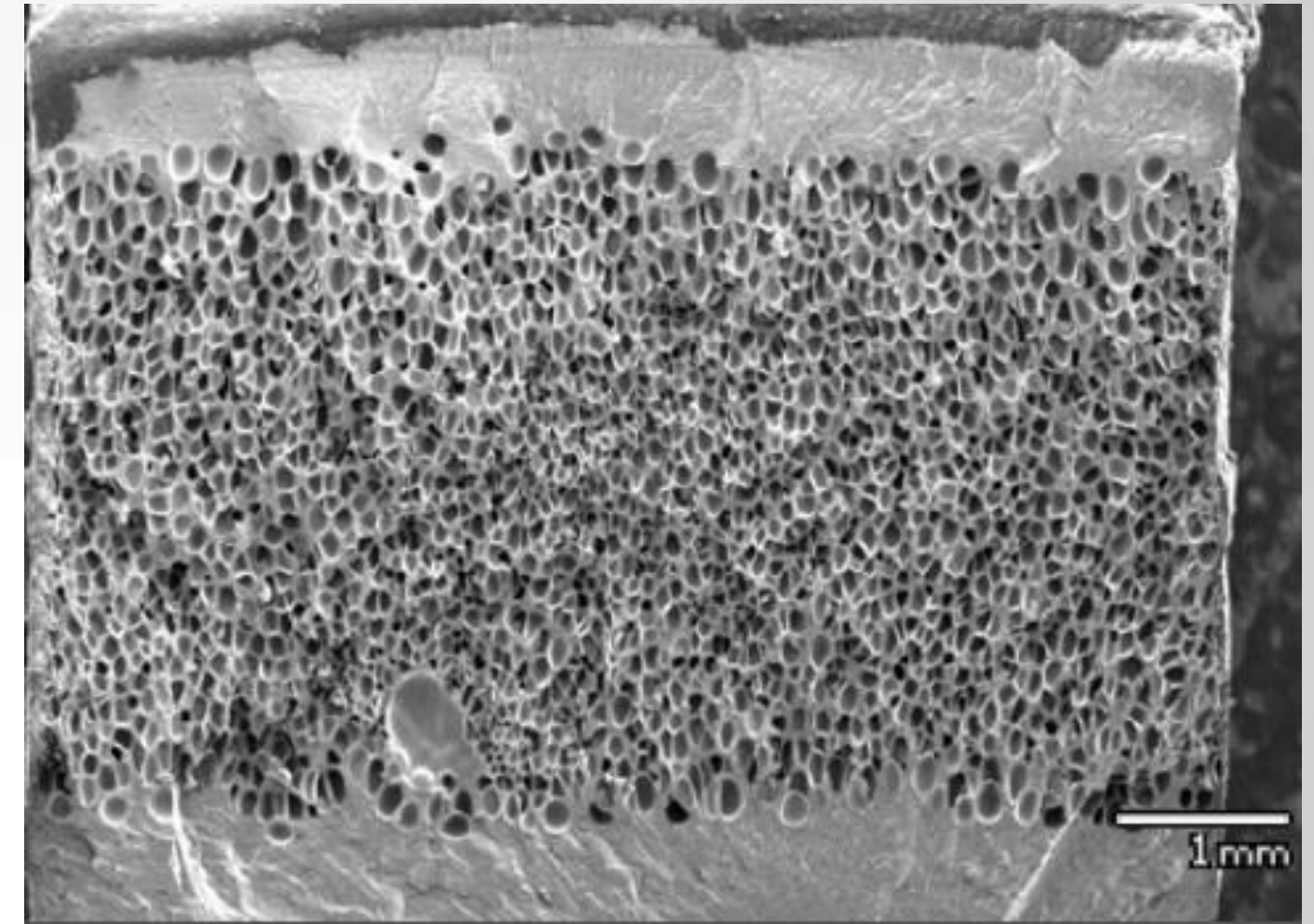
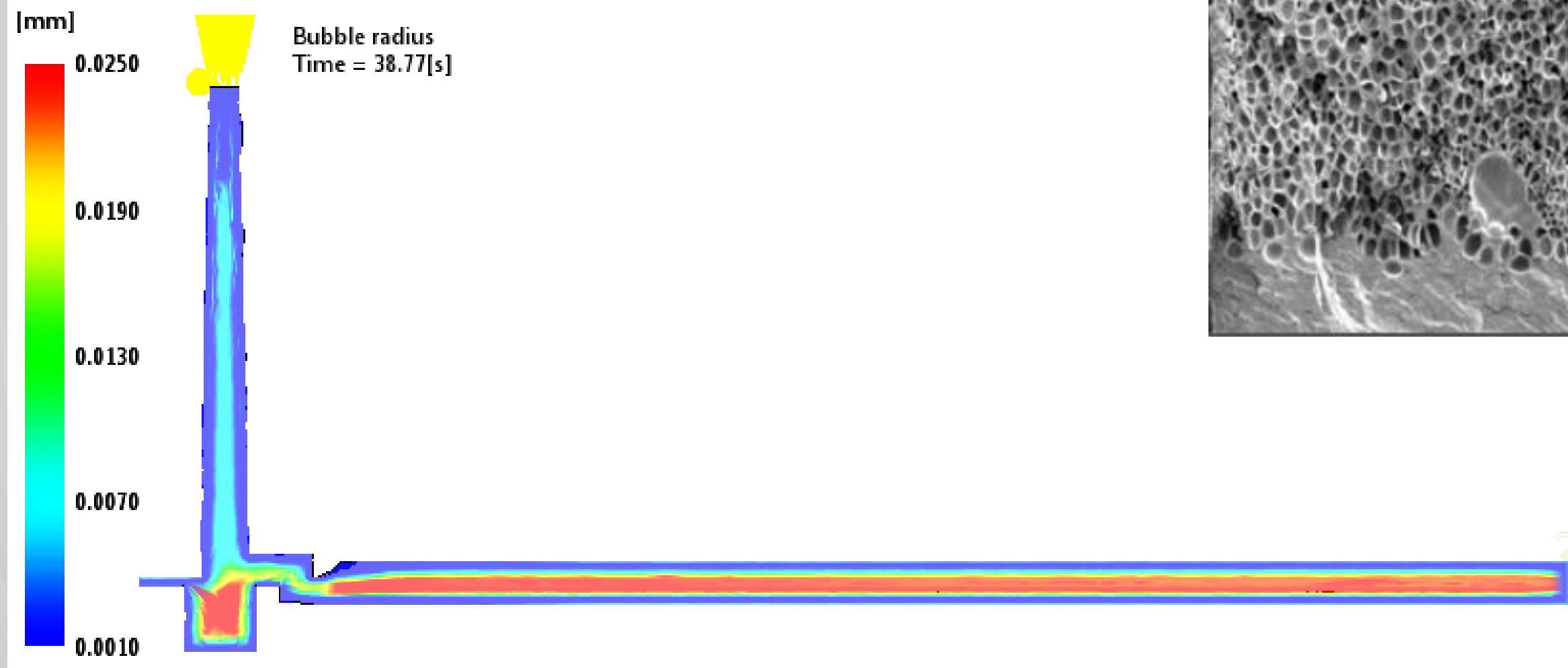
## Case 2: Plate

- Resin: PS
- Foaming gas: CO<sub>2</sub> (5% by weight)
- Plate initial thickness: 3.2 mm
- Packing: 6 or 20 MPa for 8 sec
- Open distance: 2 mm



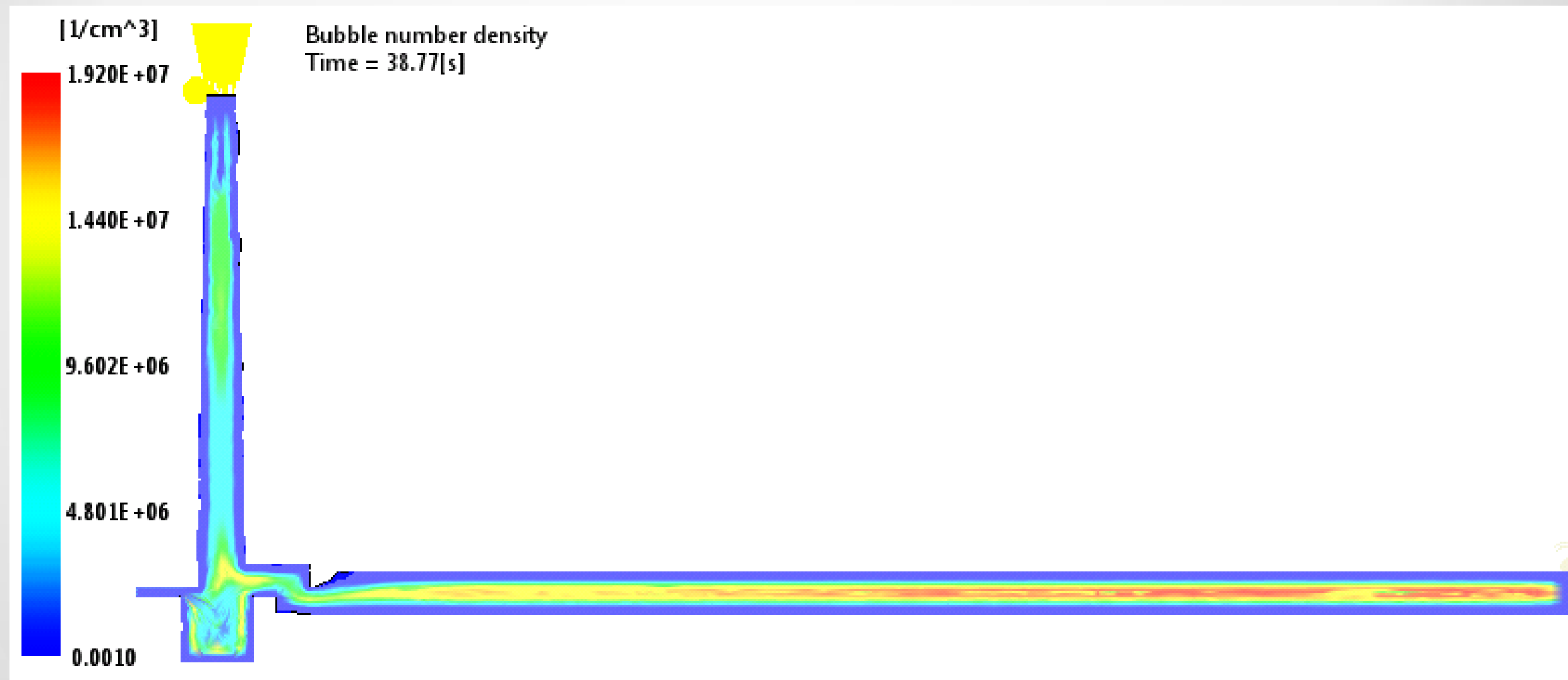
# Case 2: Calculated Bubble Radius

- Experiment: Univ. Toronto





# Case 2: Calculated Bubble Number density



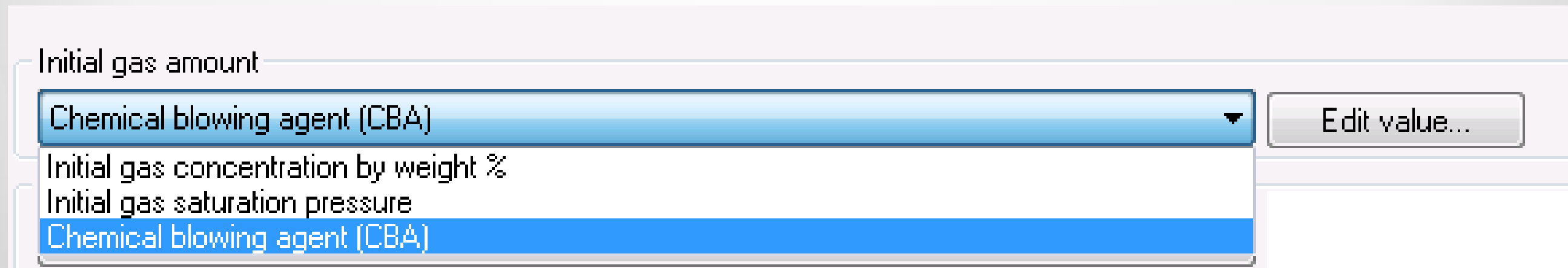
# Simulation of Microcellular Injection Molding Process

## ■ Topics

- Introduction
- Core-back microcellular injection molding
- **Microcellular injection molding using chemical blowing agent**
- Effects of gas counter pressure

# Microcellular Injection Molding by Chemical Blowing Agent

- Chemical reaction in the barrel produces foaming gas in solution
  - Assume reaction is complete in the barrel
- Choose “Chemical blowing agent” for “Initial gas amount” option



The screenshot shows a software interface for configuring parameters. The 'Initial gas amount' section is expanded, revealing a dropdown menu with the following options: 'Chemical blowing agent (CBA)', 'Initial gas concentration by weight %', 'Initial gas saturation pressure', and 'Chemical blowing agent (CBA)'. The 'Chemical blowing agent (CBA)' option is currently selected and highlighted in blue. To the right of the dropdown is a button labeled 'Edit value...'. Below the dropdown, there are two empty input fields for numerical values.



# Input Data

- **Weight % of CBA: Weight % of CBA in the resin**
- **Foaming gas conversion % of CBA by Weight: The % mass of foaming gas generated per unit mass of CBA**

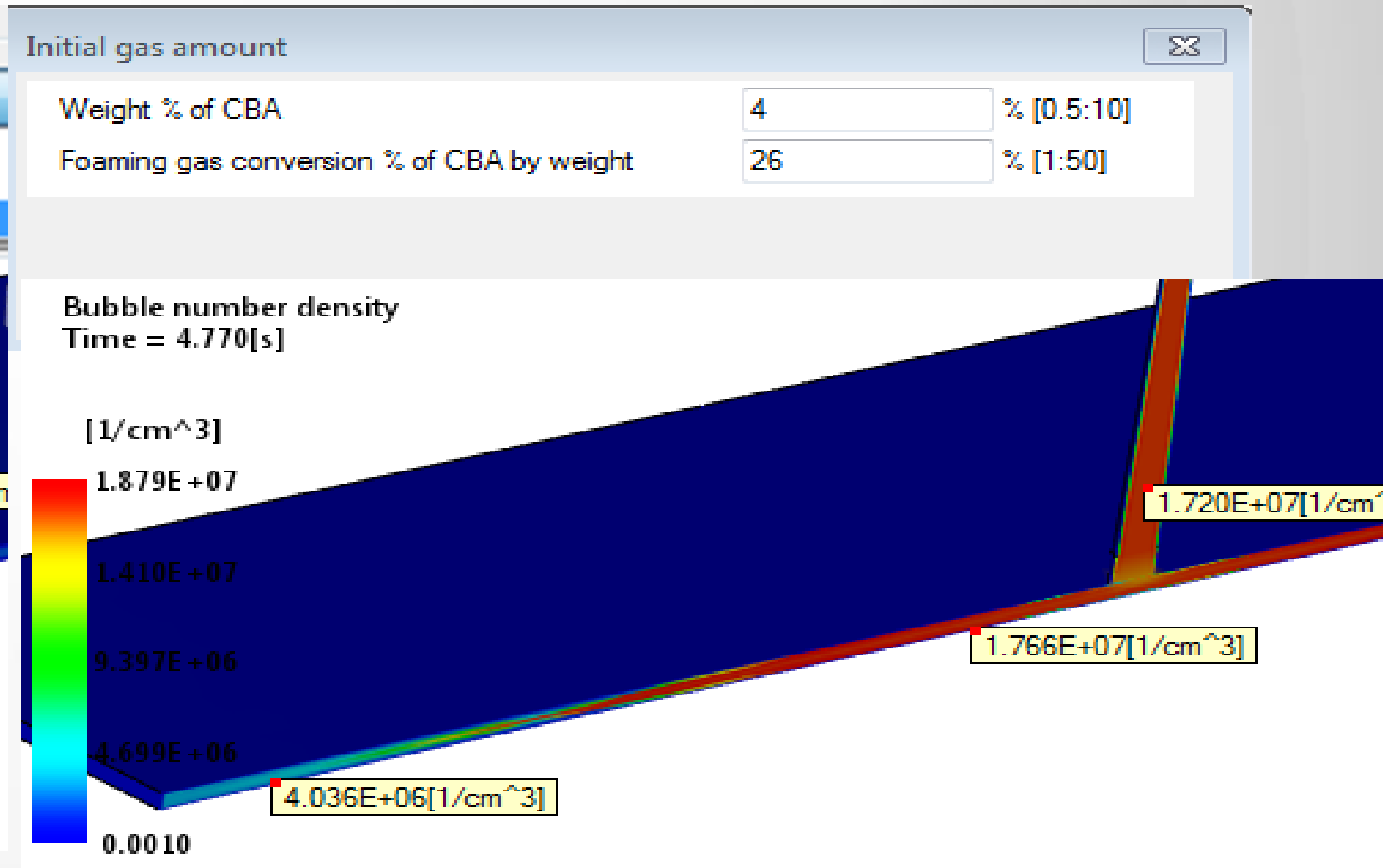
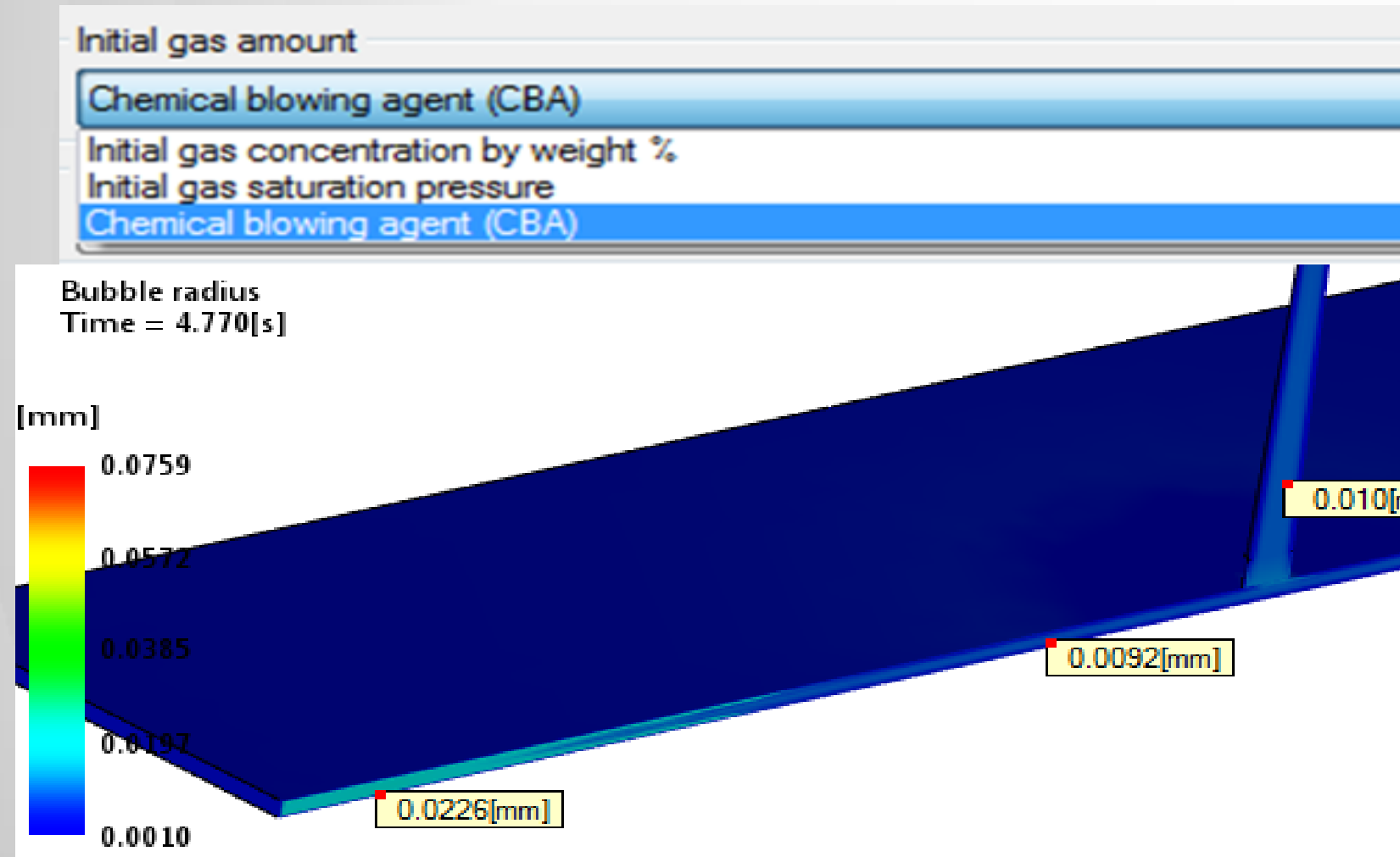
Initial gas amount		
Weight % of CBA	<input type="text" value="4"/>	% [0.5:10]
Foaming gas conversion % of CBA by weight	<input type="text" value="26.2"/>	% [1:50]

# An Example of CBA

- $\text{NaHCO}_3 \rightarrow 0.5 \text{Na}_2\text{CO}_3 + 0.5 \text{CO}_2 + 0.5 \text{H}_2\text{O}$
- Calculation of “Foaming gas conversion % of CBA by Weight”
  - Molecular weight of  $\text{NaHCO}_3 = 84$
  - Molecular weight of  $\text{CO}_2 = 44$
  - Foaming gas conversion % of CBA by Weight
    - $= 100 * (\text{Molecular weight of } 0.5 * \text{CO}_2) / (\text{Molecular weight of } \text{NaHCO}_3)$
    - $= 100 * (0.5 * 44) / 84 = 26.2\%$

# Foaming by Chemical Blowing Agent

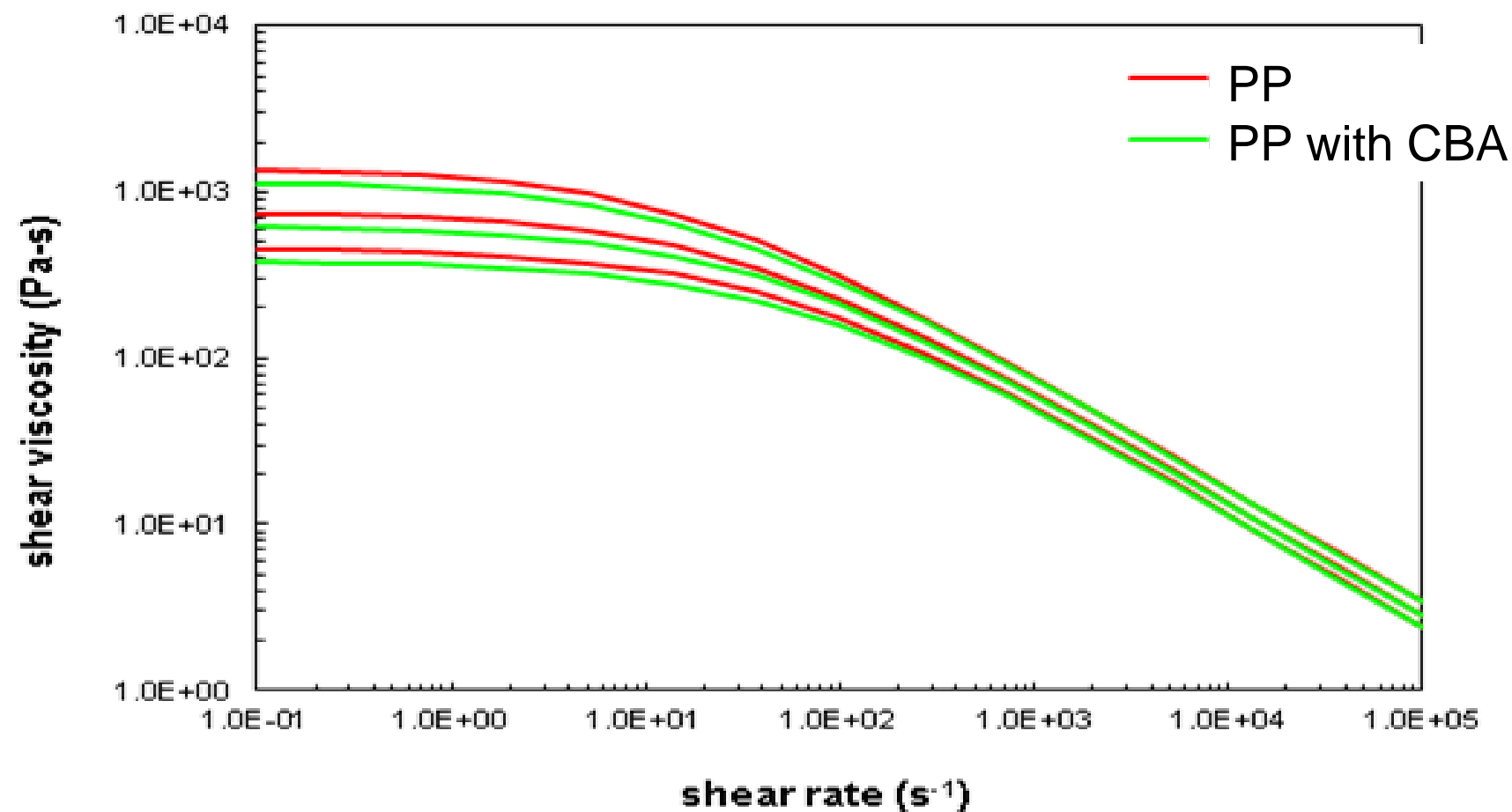
- Chemical reaction in the barrel produces  $\text{CO}_2$  in solution
  - Assume reaction is fully complete in the barrel





# Foaming by Chemical Blowing Agent

- **Research Project: Tested viscosity for a PP with 4 wt% Chemical Blowing Agent (CBA)**
  - **Injection Molding Rheometer with shutoff valve**

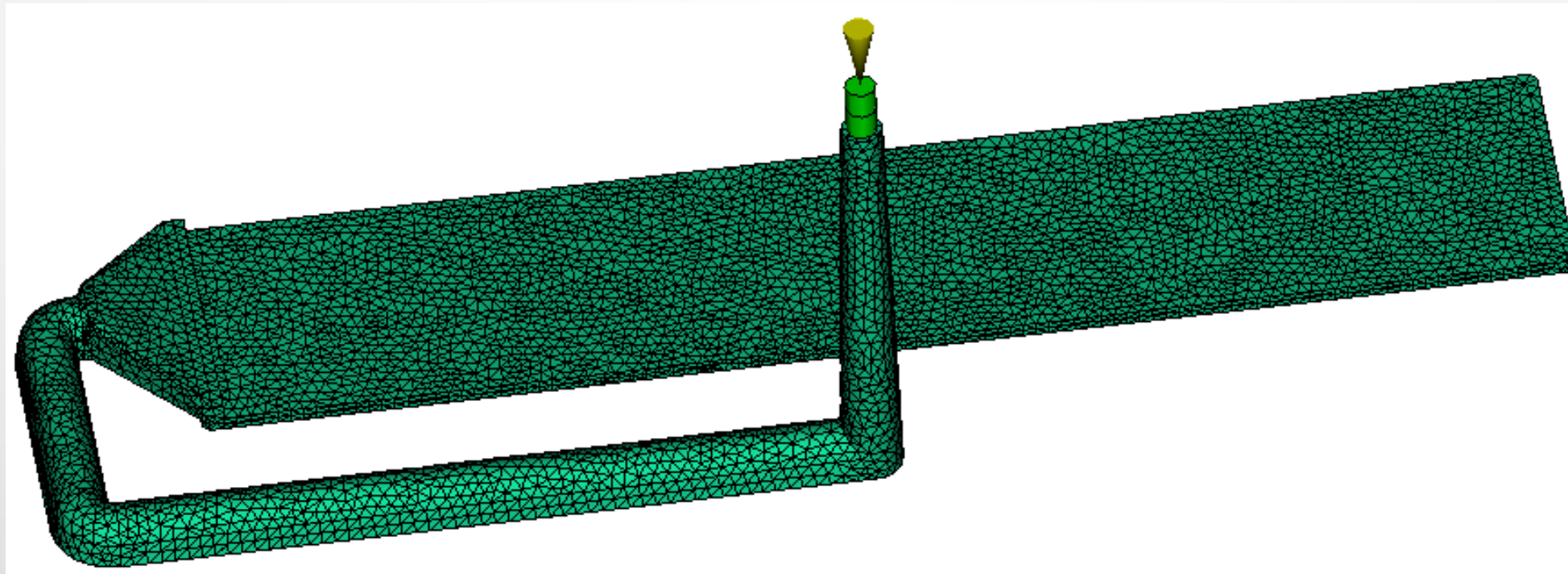


Gas content: 1wt%  
Only a small effect on shear viscosity

$$\eta = \eta_r (1 - \phi)^{v_1} \exp(v_2 c + v_3 c^2)$$

# Tag-Die Case

- Resin: PP
- CBA:  $\text{NaHCO}_3$
- CBA weight%: 4
- Initial melt temperature:  $225^\circ\text{C}$
- Mold temperature:  $50^\circ\text{C}$



# Kinetics of CBA Reaction

- Thermal decomposition of  $\text{NaHCO}_3$ :



- Degree of reaction calculation

$$d\alpha/dt = K_0 \exp(-E/R_g T)(1 - \alpha)$$

Where  $\alpha$ : degree of reaction

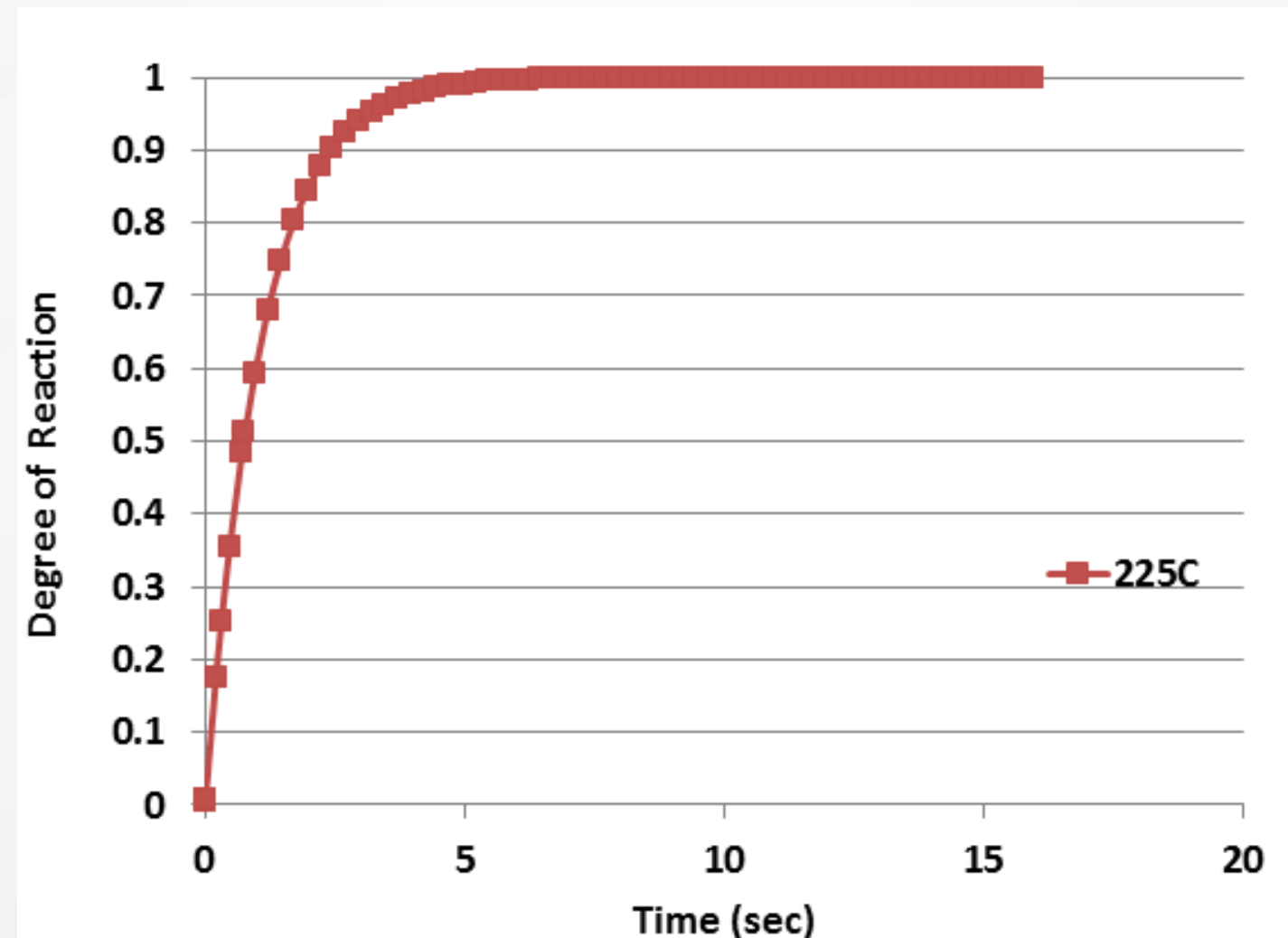
$R_g$ : Gas constant

$K_0$ ,  $E$ : Constants



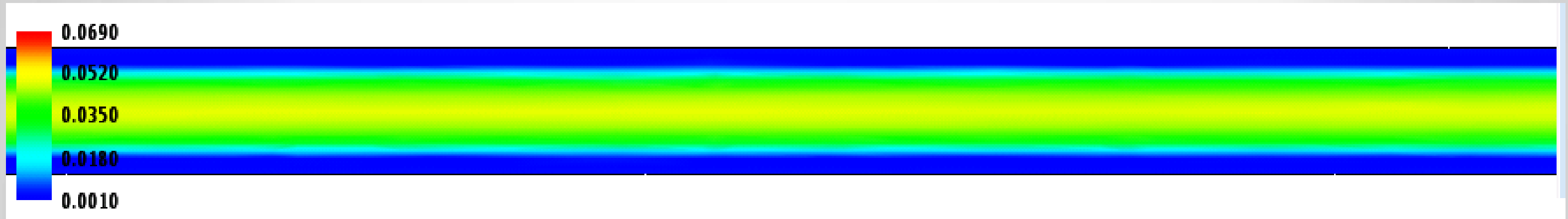
# Kinetics of CBA Reaction

- Time – degree reaction of  $\text{NaHCO}_3$  thermal decomposition at 225C
- It confirms that the reaction completes in the barrel within the residence time



# Tag-Die Case: Bubble Radius Results

- No packing



- Packing (24 MPa for 15 sec)



# Simulation of Microcellular Injection Molding Process

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- **Effects of gas counter pressure**

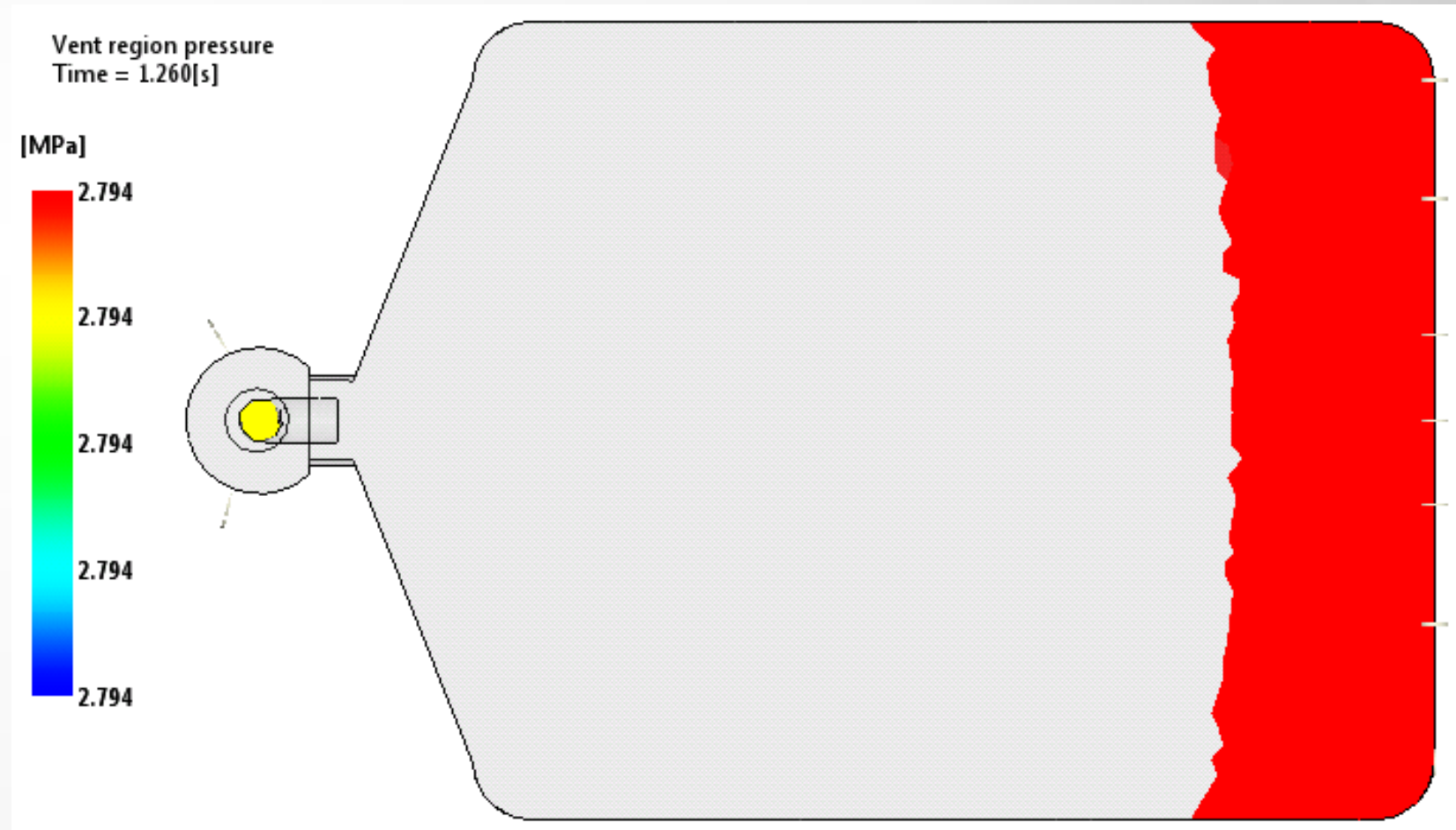
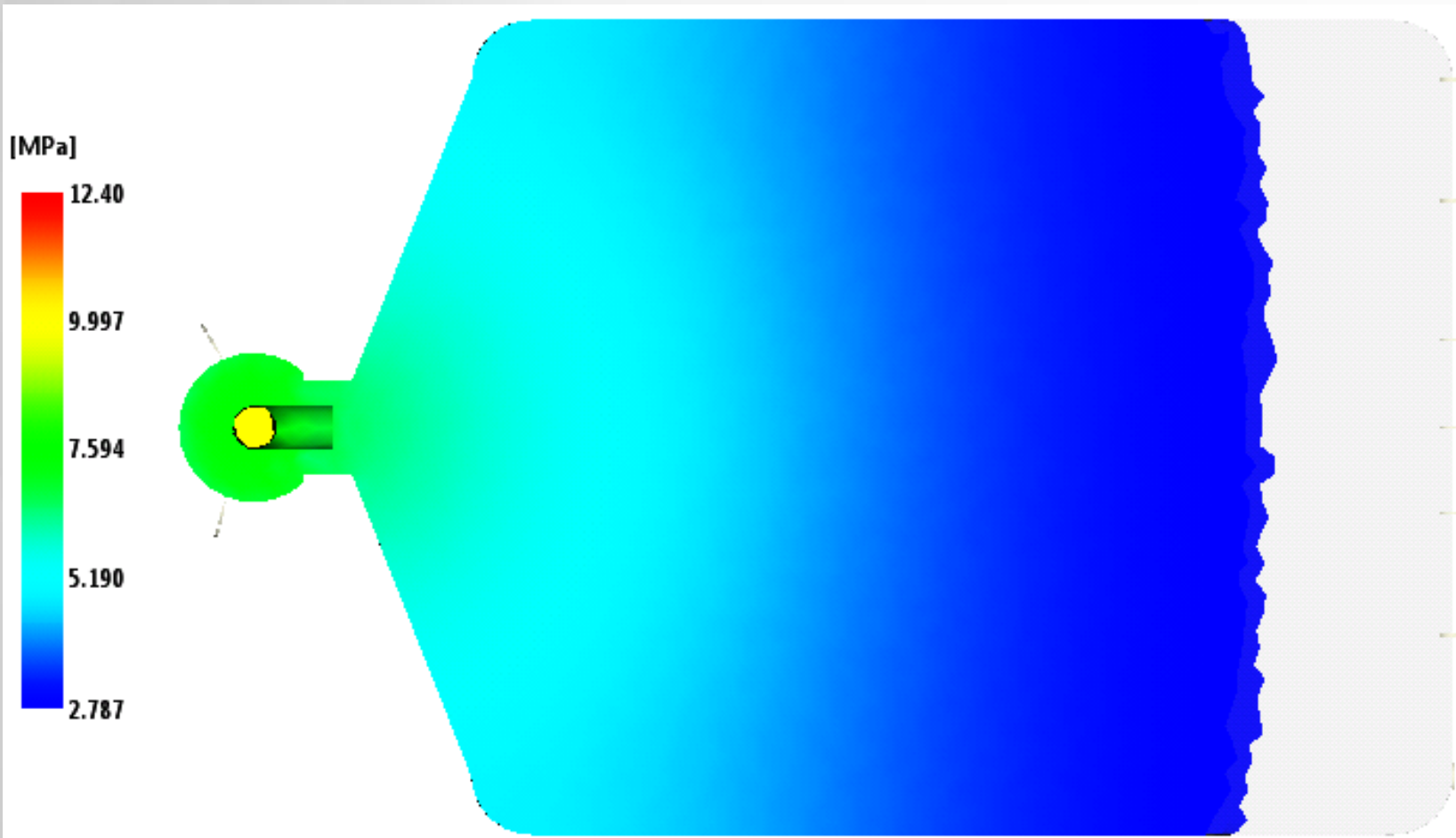
# Microcellular Injection Molding with Gas Counter Pressure

- **Use venting analysis to simulate gas counter pressure**
- **The high pressure at the melt front will suppress bubble nucleation / growth during filling**



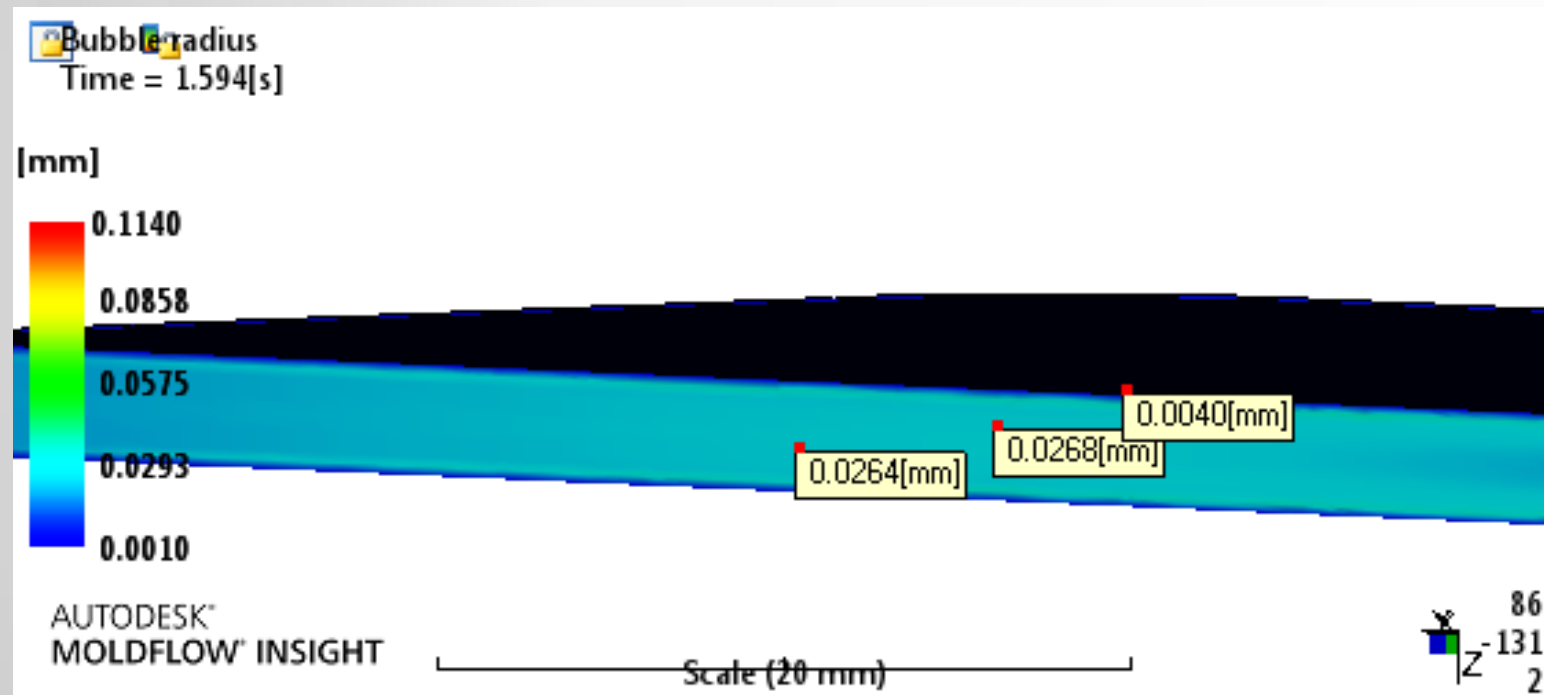
# Gas Counter Pressure: Example

- Pressure and vent region pressure plot for the case with gas counter pressure (about 2.8 MPa)

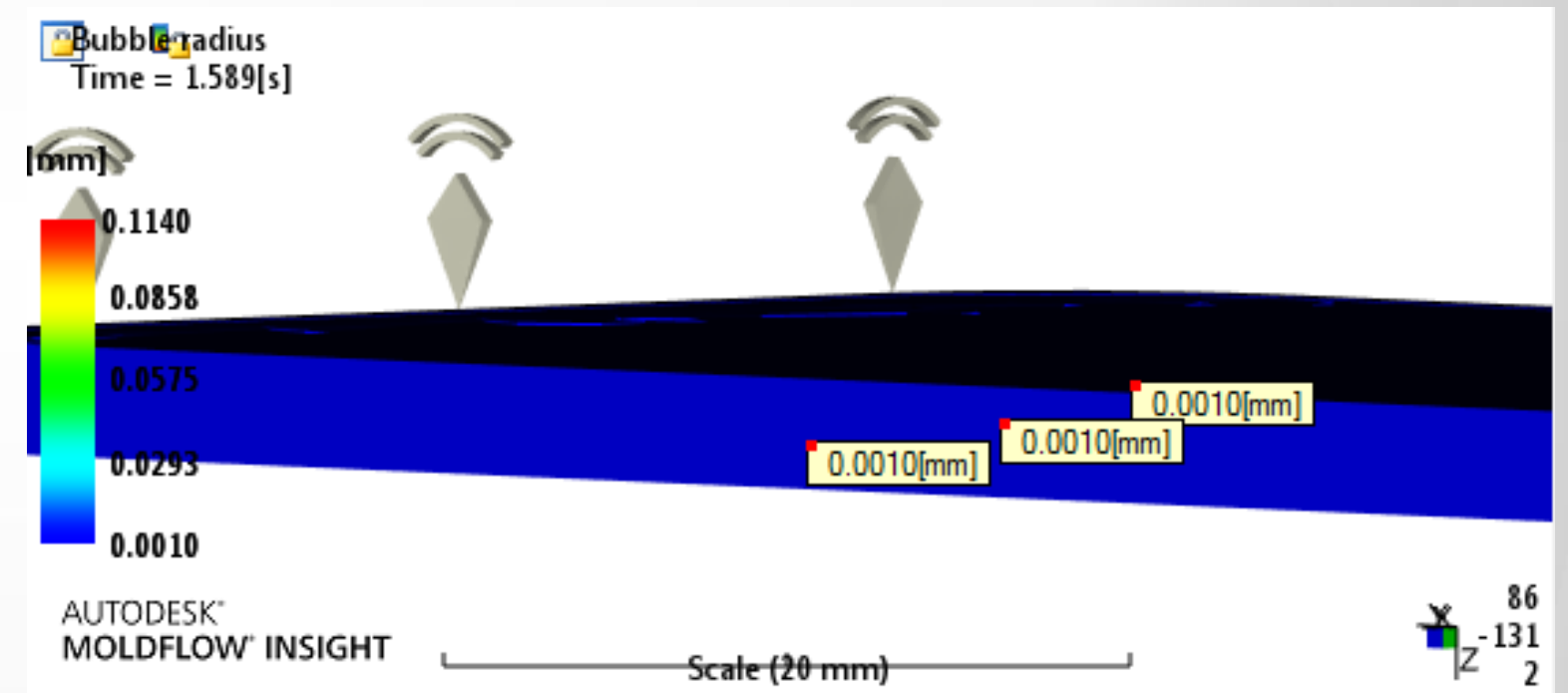


# Bubble Radius: Without and With Gas Counter Pressure

- Almost no bubble growth during filling with gas counter pressure (initial bubble radius = 0.001 mm)



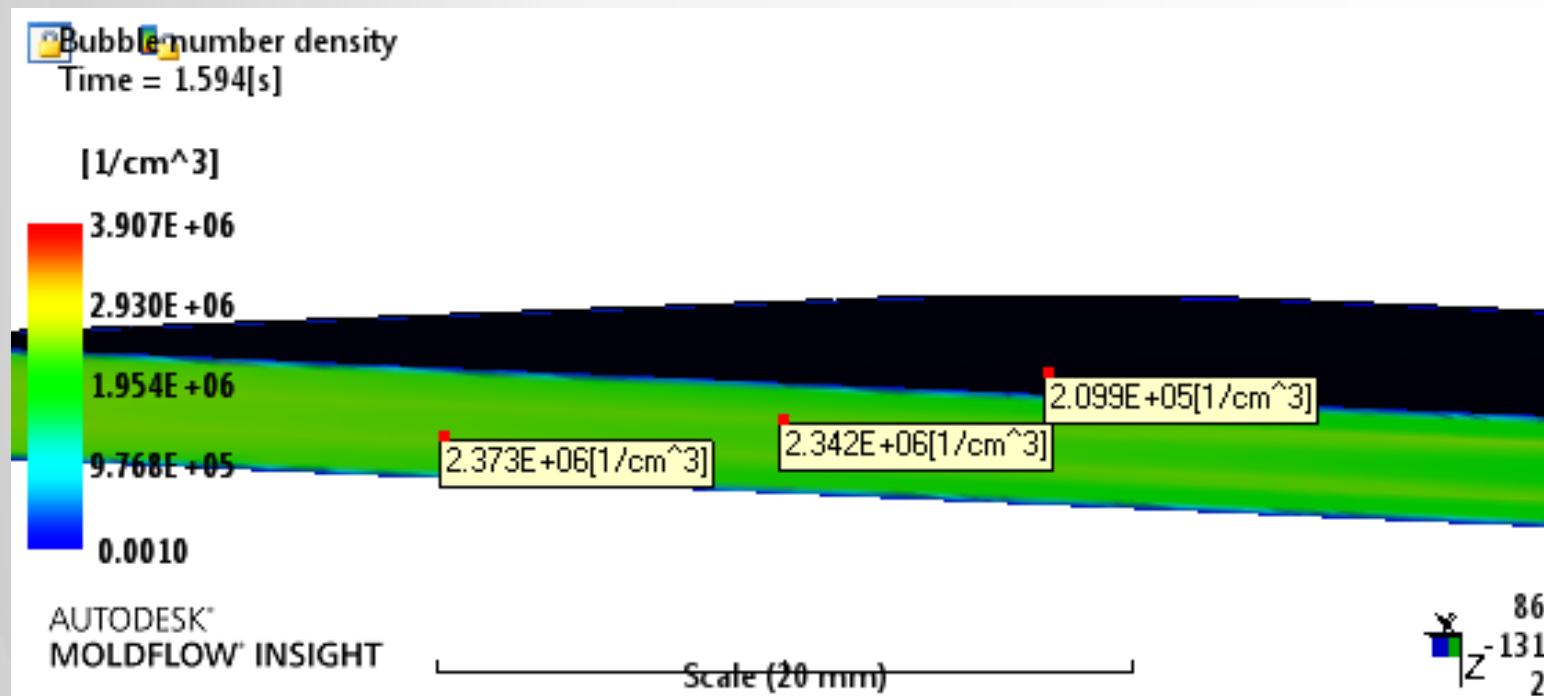
Without gas counter pressure



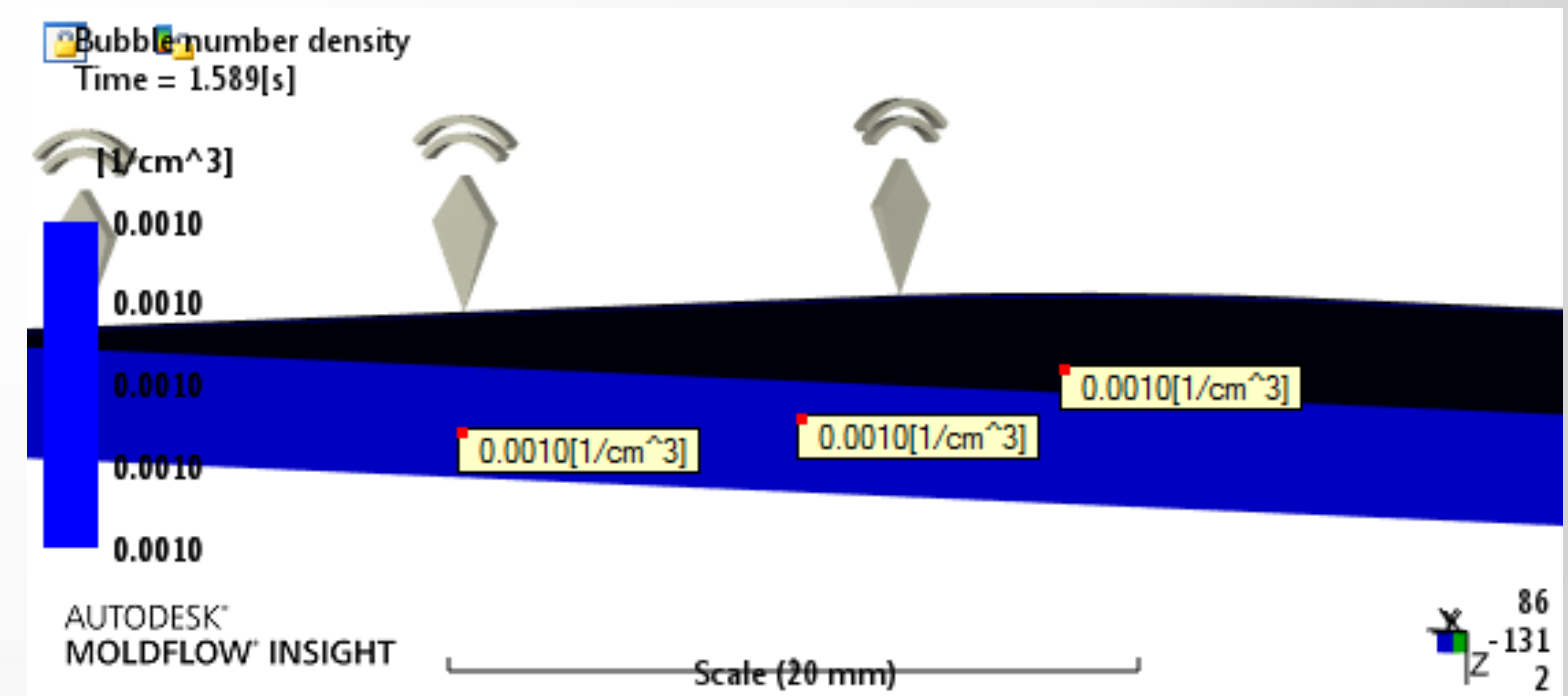
With gas counter pressure

# Bubble Number Density: Without and With Gas Counter Pressure

- Almost no bubble nucleation during filling with gas counter pressure (initial bubble number density =  $0.001 / \text{cm}^3$ )



Without gas counter pressure



With gas counter pressure



*Thank you very much !*